#### **Research Article**

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# Impact of nanoparticle shapes on the heat transfer properties of Cu and CuO nanofluids flowing over a stretching surface with slip effects: A computational study

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Abstract: This study investigates thermally radiative nanofluid flows on an elongating surface using porous media. The flow dynamics are affected by the combined impacts of exponential and thermally dependent heat sources. Additionally, magnetic effects are introduced to the flow system while it is inclined. Copper (Cu) and copper oxide (CuO) nanoparticles are mixed in water (H2O) to fabricate nanofluid flows. Different shapes of Cu and CuO nanoparticles, including column, sphere, hexahedron, tetrahedron, and lamina, were studied in this analysis. The system flow is triggered by the stretching properties of the sheet. The textured surface of the stretching sheet facilitates the exploration of the slip velocity phenomenon. The modeled equations are evaluated using the bvp4c approach in a dimensionless form. The present study is validated by comparing its findings with established datasets available in the literature. The results of this analysis show that the velocity distributions decline with increasing values of the porosity factor, velocity slip factor, and magnetic factor. The reduction in velocity profiles is quite significant in the case of Cu-water nanofluid, in contrast to the CuO-water nanofluid due to more dominance of resistive constraints in the case of the Cu-water nanofluid. The thermal distribution increases with an increase in the magnetic factor, radiation factor, Eckert number, thermal-dependent heat source, and space-based heat source, and declines with an increase in the inclination angle and thermal slip factor. The Nusselt number augments for both types of nanofluids with an increase in various emerging factors in the scenarios of thermal slip and no-slip, where an increase in the Nusselt number is maximum for the scenario where there is no thermal slip. A higher thermal distribution and heat transfer rate are determined for the lamina-shaped Cu-water and CuO-water nanofluid flows for both slip and no-slip thermal conditions. On the basis of the current findings, this study aims to design efficient cooling systems for microelectronics, improve solar thermal collectors, enhance drug delivery via heat-sensitive nanoparticles, optimize industrial heat exchangers, and advance smart textile technologies requiring controlled thermal regulation using shape-engineered Cu and CuO nanofluids.

**Keywords:** nanofluid, inclined magnetic field, porous media, heat source, slip conditions, Joule heating, numerical investigation

### **Nomenclature**

u, v

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stretching constant  $u_w(x)$ stretching velocity [m s<sup>-1</sup>] strength of the magnetic field [kg s<sup>-2</sup> A<sup>-1</sup>]  $B_0$ Ttemperature [K]  $k^*$ mean absorption coefficient [m<sup>-1</sup>]  $C_{\rm p}$ specific heat [J kg<sup>-1</sup> K<sup>-1</sup>] thermal-dependent heat source coefficient  $[W m^{-3} K^{-1}]$ space-dependent heat source coeffi- $Q_{\rho}$ cient [W m<sup>-3</sup> K<sup>-1</sup>]

thermal conductivity [W K<sup>-1</sup> m<sup>-1</sup>]

flow components [m s<sup>-1</sup>]

k

n pow	er index
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ν kinematic viscosity [m<sup>2</sup> s<sup>-1</sup>]

 $f(\eta)$  velocity profile M magnetic factor K porosity parameter Rd thermal radiation factor

Ec Eckert number

 $Q_{\rm Exp}$  exponential heat source

 $Q_I$  thermal-dependent heat source

### **Greek notation**

 $\rho$  density [kg m<sup>-3</sup>]

 $\sigma$  electrical conductivity [S m<sup>-1</sup>]

 $\theta(\eta)$  temperature profile

 $\varphi$  volume fraction of the nanoparticle

 $\sigma_1$  coefficient of velocity slip  $\sigma_2$  coefficient of thermal slip

 $\eta$  variable

 $\gamma$  acute angle  $[()^0]$ 

 $\mu$  dynamic viscosity [kg m<sup>-1</sup> s<sup>-1</sup>]

 $\lambda_1$  velocity slip factor  $\lambda_2$  thermal radiation factor

# **Subscripts**

∞ free-streamN nanoparticle

f fluid nf nanofluid

### 1 Introduction

Nanofluids are composed of a combination of nanoparticles and pure fluid, where both are mixed. The accumulation of nanoparticles alters the thermal, optical, and rheological features of the base fluid, resulting in nanofluids with enhanced heat transfer capabilities associated with conventional fluids, as observed by Choi and Eastman [1]. This enhancement arises primarily from the high surface area-to-volume ratio and unique thermal conductivities of the nanoparticles [2]. Acharya *et al.* [3] have proved that a nanolayer greatly impacts the heat transference in comparison to the nanoparticles' diameter. The Brownian motion of nanoparticles within the fluid helps distribute

heat more effectively, while the increased thermal conductivity enables faster and more efficient heat transfer [4]. Achieving stable dispersion and preventing particle agglomeration are critical challenges in nanofluid synthesis and application and are often addressed through surface modification, surfactants, or stabilizers. The applications of these fluids are there are industries, comprising heat exchangers, solar energy systems, automotive cooling, and biomedical devices, owing to their superior heat transfer performance and potential for tailored properties [5,6]. Ongoing research continues to explore new nanofluid formulations, synthesis methods, and applications to further optimize their properties and expand their utility in diverse engineering and scientific domains. With the passage of time, the dispersion of two or more distinct nanoparticles can further heighten the thermal flow behavior of a pure fluid, also termed a hybrid nanofluid [7]. Hybrid nanofluid flow represents an innovative area of research in thermal engineering, where the introduction of several kinds of nanoparticles into a pure fluid creates a composite fluid with enhanced heat transfer properties [8]. This innovative approach capitalizes on the synergistic effects of combining different nanoparticle materials, such as metallic and non-metallic particles, to tailor the fluid's thermal conductivity, viscosity, and other key characteristics for specific applications [9,10]. The occurrence of nanoparticles in pure fluid leads to effective heat dissipation and has led to the development of coolants and heat exchangers for thermal performance systems [11]. Additionally, the hybrid nature of these nanofluids allows for the optimization of other heat transfer-related properties, such as convective heat transfer coefficients. Furthermore, the unique rheological behavior of hybrid nanofluids can alter flow patterns and heat transfer mechanisms, presenting opportunities for enhancing heat transfer rates and optimizing system design [12]. Upreti et al. [13] used the heterogeneous as well as homogeneous reactions for nanofluid flow on an elongated sheet with the famous Buongiorno model and convective constraints. Adnan et al. [14] simulated numerically the thermal features for nanofluid flow using dissipative effects and convective heat constraints influences, and noticed that thermal flow is affected less by the slippery features of the surface, while growth in dissipative factor has augmented thermal profiles to the maximum level. Rahman et al. [15] studied the thermally Darcy-Forchheimer fluid flow on a medium with impressions of a magnetic field and heating source. Alharbi et al. [16] investigated the thermal management for nanofluid flow through the annular region affected by radiative and magnetized processes. Bani-Fawaz et al. [17] studied the thermal flow phenomenon for radiated nanoparticle flow influenced by the diameter of molecules

and the features of nanoparticles. Rawat et al. [18] used non-Fick and non-Fourier phenomena to investigate mixed convective magneto-hydrodynamic (MHD) fluid flows. Upreti et al. [19] assessed the thermally blood-based nanofluid flow on a permeable surface with impressions of a magnetic field and the Cattneo-Christov model and have observed dual features in flow profiles for augmentation in the magnetic factor. Upreti et al. [20] assessed convective thermal flow for Sisko fluid flow on a stretchable surface with suction and dissipative effects. Gangadhar et al. [21] discussed Stefan blowing effects on fluid flow past a spinning convective disk with effects of chemical reactivity. Ahmed et al. [22] investigated the peristaltic propulsion of thermal radiative magnetized nanofluid flow incorporating the lubrication approximation and slip boundary conditions. Their study focused on understanding how thermal radiation and magnetic fields influence the movement and heat transfer behavior of nanoparticles in a peristaltic transport system. Hayat et al. [23] studied the peristaltic hybrid nanoparticle flow through a channel with the impacts of heated asymmetric configurations. Gangadhar et al. [24] explored the nonlinear radiative heat transfer in a nanofluid flow over a permeable inclined surface, considering the effects of chemical reactivity. Their study focused on understanding the influence of radiative heat and chemical reactions on the thermal and flow characteristics of nanofluids under various conditions.

An inclined magnetic field is a magnetic field whose direction varies from horizontal or vertical. In such scenarios, the Lorentz force, generated from the interaction between the conducted (electrically) fluid and magnetic field, becomes a dominant factor in determining the flow dynamics [25,26]. This force exerts a deflecting influence on the fluid flow, causing deviations in the velocity profiles and shear stresses within the fluid. These changes, in turn, profoundly affect the mechanisms of convective heat transfer [27]. Forced convection, driven by external forces or pressure gradients, experiences modifications due to Lorentz force-induced alterations in the flow direction and velocity distribution. Similarly, natural convection, driven by buoyancy forces resulting from temperature gradients, undergoes significant transformations with the effect of an inclined magnetic field [28]. The Lorentz force-induced modifications in the flow dynamics disrupt the buoyancy-driven flow patterns, causing changes in the heat transfer rates and temperature distributions within the fluid. The composite phenomenon amid fluid flow, magnetic fields, and heat transfer in inclined magnetic field configurations is crucial for numerous engineering applications, such as system coolants [29,30]. Additionally, such an understanding is relevant in various natural phenomena and industrial processes, such as geophysical fluid

dynamics, metallurgical processes, and the operation of MHD systems in fusion reactors and space propulsion technologies. Saeed et al. [31] examined convective slip fluid flow with double diffusive behavior for nanofluid on an asymmetric conduit. Gangadhar et al. [32] examined the entropy optimization and impacts of electro-magnetohydrodynamics on nanofluid flow with nonlinear thermal radiations on a surface. Lone et al. [33] examined thermally MHD nanofluid flow through elongating angular spinning disks with varying porosity and the Cattaneo-Christov thermal flux model. Gangadhar et al. [34] studied Williamson fluid flow on a Riga surface with effects of nonlinear radiative flux and binary chemically reactive effects. Mahabaleshwar et al. [35] studied injection and radiation effects on Newtonian fluid flow on a permeable shrinking surface with the Brinkman model. Gangadhar et al. [36] examined computationally the heterogeneous-homogeneous chemically reactive effects on Maxwell fluid flow on a disk with effects of nonlinear thermal radiations. Mahabaleshwar et al. [37] investigated the exact solution of fluid flow over a permeable surface, considering different boundary constraints. Their study focused on analyzing how these constraints affect flow behavior, providing valuable insights into fluid dynamics. Their research enhances the understanding of boundary layer theory in engineering and scientific applications.

Porous media are materials with interrelated void spaces or pores that allow the passage or flow of fluids through them. The structure and properties of porous media play vital roles in various engineering and scientific fields. Fluid flow through porous media and its impacts on heat transfer processes are critical phenomena with wideranging implications in various engineering and scientific fields [38]. Whenever a liquid flows on a permeable medium, such as soil, sand, or a porous structure, it interacts with the solid matrix and undergoes complex flow behaviors. The porous spaces familiarize resistance to the flow, altering velocity profiles and flow patterns in a way that describes how it impacts heat transfer mechanisms [39]. The interaction between thermal transference and liquid flow on permeable media influences important processes like groundwater flow and thermal energy storage in geothermal reservoirs [40], as well as industrial applications like enhanced oil recovery, geotechnical engineering, and the design of heat exchangers and porous materials for thermal insulation [41]. These phenomena require advanced mathematical models, experimental techniques, and computational simulations to characterize the complex fluid-solid interactions and optimize the processes for efficient energy utilization and sustainable engineering practices. Habibishandiz and Saghir [42] reviewed critically the augmentation of thermal transmission for nanofluid flow on porous media using the effects of microorganisms. Verma *et al.* [43] examined fluid flow on a penetrable surface using double stratification with the surface as a nonlinearly elongating sheet.

A thermal and space-dependent heat source is a source of thermal energy that varies in both intensity and spatial distribution over time. Thermal- and space-dependent heat sources represent a complex scenario in which both the intensity and spatial distribution of heat generation vary over time. Such heat sources are encountered in numerous engineering and scientific contexts, ranging from industrial processes to environmental systems [44,45]. One common example is found in electronic devices, where the power dissipation within the device fluctuates due to varying operational conditions and computational demands. In this case, the heat generation not only changes over time but also exhibits spatial variations within the device, with certain regions experiencing higher heat fluxes than others [46]. Another example can be seen in combustion systems, where fuel combustion rates may vary due to changes in operating conditions or fuel composition, leading to fluctuations in heat release rates and spatial distributions of heat within the combustion chamber. The impacts of thermal- and space-dependent heat sources on the heat transfer processes are insightful [47]. They affect the temperature distributions, velocity profiles, and flow patterns within the surrounding medium, leading to variations in the convective heat transfer rates [48]. Additionally, these fluctuations can influence the thermal stresses, material degradation, and system performance. Accurately modeling the behavior of thermal and space-dependent heat sources is essential for optimizing heat transfer systems, designing effective cooling strategies, and ensuring the reliability and efficiency of various engineering systems, including electronic cooling systems, thermal management in buildings, and combustion processes in power generation and propulsion systems. Various theoretical analyses have been conducted to characterize the interactions between these heat sources and their surrounding environments, smoothing the progress of innovative solutions in many practical applications [49,50].

The slip conditions illustrate the performance of a fluid flow at a solid boundary, where the fluid molecules interact differently with the surface compared to the bulk fluid. The slip conditions deviate from this assumption, allowing for nonzero velocities at the borderline. Slip conditions are particularly relevant in microfluidics, nanofluidics, and other situations involving fluid flow at small length scales, where intermolecular forces become significant. Fluid flow with slip conditions, where the velocity at the solid boundary differs from that of the bulk fluid, has profound implications for

thermal transport processes [51,52]. In such scenarios, the slip alters the velocity profile near the boundary, thereby influencing the thermal transfer rate and temperature distribution within the fluid [53]. At the micro- and nanoscales, where slip effects become increasingly significant, understanding the relationship between fluid flow, slip conditions, and thermal transport is crucial for various applications. For instance, in microfluidic heat exchangers, slip-induced changes in flow behavior can impact the heat transfer efficiency and overall device performance. Similarly, in nanoscale thermal management systems, such as heat dissipation in electronic devices, slip conditions may affect the temperature gradients and heat transfer rates, thereby influencing device reliability and performance [54]. Nazeer et al. [55] inspected Hall current and slip constraints at the boundaries for nanofluid flow in a convergent conduit. Amer et al. [56] studied the slip effects of fluid flow on an extending sheet with permeable impressions and revealed that slip flow constraints significantly affect the flow phenomenon of the system. Rasool et al. [57] inspected the nanofluid unsteady flow with the impact of slip conditions. Lone et al. [58] investigated MHD blood-based nanofluid flow over a convectively heated sheet, considering variable porosity and slip conditions at the surface. Their study focused on analyzing how magnetic fields and surface constraints affect heat transfer and flow behavior in biomedical and engineering applications involving nanofluids.

#### 1.1 Novelty

This study thermally investigates radiative nanofluids flowing on an elongating sheet using a permeable sheet. The flow dynamics are affected by the combined impacts of exponential and thermal-dependent heat sources. Additionally, magnetic effects have been introduced to the flow system while it is inclined. Copper (Cu) and copper oxide (CuO) nanoparticles were mixed with water (H<sub>2</sub>O) to fabricate nanofluid flows. In this analysis, we focused on the different shapes of the Cu and CuO nanoparticles, which include column, sphere, hexahedron, tetrahedron, and lamina, to explore the thermal panels and their transmission rate. Furthermore, velocity and thermal slip conditions are executed in this analysis to investigate the nanofluid flows. The Joule heating, space-dependent heat source, and thermal-dependent heat source effects are also used in this analysis. Based on these assumptions, we focused on the following research questions:

 What are the impressions of the porosity factor and velocity slip factor on the velocity distributions of the Cu-water and CuO-water nanofluids?

- How do the velocity panels change in response to enhancing the inclination angle with respect to the magnetic field effect, and at what angles are the velocities maximized?
- · How do the thermal distribution and Nusselt number change for distinct types of nanofluids under various emerging factors, especially when comparing the thermal slip and no-slip conditions, and where is the maximum increase observed?
- What differences are observed in the thermal distribution and heat transfer rate for lamina-shaped Cu-water and CuO-water nanofluid under slip and no-slip thermal conditions?

The choice of differently shaped nanoparticles is based on their representative nature in real-world applications and their distinctive effects on thermal conductivity, flow behavior, and nanofluid performance. Spherical nanoparticles are often used in experimental studies due to their ease of fabrication and well-documented behavior in terms of flow and heat transfer properties. Column-shaped nanoparticles are relevant for applications where extended structures interact with the fluid, such as nano coatings or heat exchangers, where the elongated shape can enhance the temperature performance. Hexahedral and tetrahedral-shaped nanoparticles have been investigated in the literature due to their geometrical advantages in terms of maximizing the surface area contact with the base fluid, which can impact the heat transfer characteristics. Lamina-shaped nanoparticles are considered due to their potential application in high thermal conductivity systems, where structures can form layered flow paths in nanofluids.

### 1.2 Practical applications of the problem

Research on the impact of nanoparticle shapes on the heat transfer properties of Cu and CuO nanofluids has a wide range of practical applications. In industrial cooling systems, it can optimize the performance of heat exchangers, thereby improving the efficiency of the cooling processes in power plants, air conditioning, and refrigeration systems. For microelectronics, understanding how different nanoparticle shapes affect heat transfer is vital for thermal management in advanced devices like microchips and computer processors, which require efficient cooling to prevent overheating and enhance performance. In the biomedical field, this study has potential applications in drug delivery systems, where nanofluids can be designed to

improve the controlled release of medication by manipulating heat transfer at the targeted site. Furthermore, this research can enhance the efficiency of solar thermal collectors by utilizing nanofluids with optimized nanoparticle shapes to improve heat absorption and transfer, contributing to more effective renewable energy storage systems.

### 2 Problem formulation

Take an unsteady, laminar, and incompressible flow of nanofluids on a permeable extending surface. A two-dimensional Cartesian coordinate system is chosen for the fluid flows. The sheet expands with velocity  $u_w(x) = bx$  along the x-axis, where b(>0) is constant. A magnetic field with strength  $B_0$ acts in an inclined direction with an angle  $\gamma$  in the  $\gamma$ -direction, which acts as a transverse magnetic field when  $\gamma = 90^{\circ}$ , as shown in Figure 1. Velocity and temperature slip conditions were imposed to inspect the nanofluid flows and heat transfer rate. The surface and ambient temperatures are  $T_w$ and  $T_{\infty}$ , respectively. Joule heating, space-dependent heat source, thermal-dependent heat source, and thermal radiation impacts are also considered in this study.

Using these assumptions, we have [59]

Continuity equation:

$$u_x + v_y = 0. ag{1}$$

Momentum equation:

$$\rho_{\rm nf}(uu_{\rm x} + vu_{\rm y}) = \mu_{\rm nf}u_{\rm yy} - \mu_{\rm nf}\frac{u}{K_{\rm p}} - \sigma_{\rm nf}B_0^2u\sin^2\gamma.$$
 (2)

Energy equation:

$$(\rho C_{\rm p})_{\rm nf} (u T_{\rm x} + \nu T_{\rm y})$$

$$= \left( k_{\rm nf} + \frac{16\sigma^* T_{\infty}^3}{3k^*} \right) T_{yy} + \sigma_{\rm nf} B_0^2 u^2 \sin^2 \gamma$$

$$+ Q_t (T - T_{\infty}) + (T_w - T_{\infty}) Q_e e^{\left[ -n \sqrt{\frac{b}{\nu_f}} y \right]}.$$
(3)

The conditions at the boundary are

$$\begin{cases} u = u_w(x) + \sigma_1 \frac{\partial u}{\partial y}, & v = 0, \quad T = T_w + \sigma_2 \frac{\partial T}{\partial y}, \\ \text{at } y = 0, \\ u \to 0, \quad T \to T_\infty \quad \text{as} \quad y \to \infty. \end{cases}$$

$$(4)$$

The effective qualities of nanofluids are defined as [60-62]:

$$\mu_{\rm nf} = \frac{\mu_{\rm f}}{(1 - \varphi)^{2.5}},\tag{5}$$

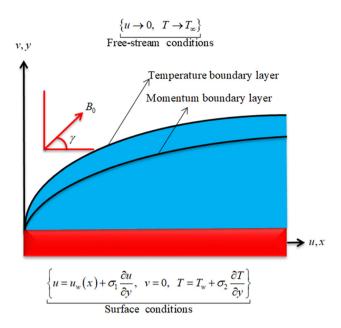


Figure 1: Graphical view of the flow phenomenon.

$$\rho_{\rm nf} = \rho_{\rm f}(1 - \varphi) + \rho_N \varphi, \tag{6}$$

$$(\rho C_{\rm p})_{\rm nf} = (1 - \varphi)(\rho C_{\rm p})_{\rm f} + \varphi(\rho C_{\rm p})_{N}, \tag{7}$$

$$\frac{k_{\rm nf}}{k_{\rm f}} = \frac{k_N + (m-1)k_{\rm f} - (m-1)\varphi(k_{\rm f} - k_N)}{k_N + (m-1)k_{\rm f} + \varphi(k_{\rm f} - k_N)},\tag{8}$$

$$\frac{\sigma_{\rm nf}}{\sigma_{\rm f}} = 1 + \frac{3\left(\frac{\sigma_N}{\sigma_{\rm f}} - 1\right)\varphi - 2(\sigma_{\rm f} - \sigma_N) + 2\sigma_{\rm f}}{\left(\frac{\sigma_N}{\sigma_{\rm f}} + 2\right) - \left(\frac{\sigma_N}{\sigma_{\rm f}} - 1\right)\varphi}.$$
 (9)

Here, N represents the nanoparticle,  $\varphi$  is the nanoparticles' volume fraction, and m represents the shape factor of the nanoparticles. The thermophysical features of Cu,

Table 1: Thermophysical features of H<sub>2</sub>O, Cu, and CuO [59,63]

Physical property	H <sub>2</sub> O	Cu	CuO
$\rho$ [kg/m <sup>3</sup> ]	997.1	8,933	6,320
C <sub>p</sub> [J/kg K]	4,179	385	531.8
k [W/m K]	0.613	401	76.5
$\sigma$ [S/m]	5.5 × 10 <sup>-6</sup>	5.96 × 10 <sup>7</sup>	$2.7 \times 10^{-8}$

CuO, and  $H_2O$  are defined in Table 1. Table 2 shows the values of the nanoparticle shape factor. Moreover, copper (Cu) and copper oxide (CuO) nanoparticles have a broad range of applications across various fields due to their excellent thermal, electrical, and chemical properties. In electronics, they are used in conductive inks, printed circuits, and semiconductors. Cu and CuO also serve as effective catalysts for chemical reactions and environmental remediation. In thermal systems, they enhance the heat transfer in nanofluids for industrial cooling and energy devices. Their antimicrobial properties make them valuable for coatings, textiles, and water purification. In biomedical applications, they have been explored for drug delivery, biosensing, and cancer therapy due to their biocompatibility and surface reactivity.

Similarity variables are given as

$$u = bxf'(\eta), \quad v = -\sqrt{bv_f} f(\eta),$$
  

$$\theta(\eta) = \frac{T - T_{\infty}}{T_{w} - T_{\infty}}, \quad \eta = y\sqrt{\frac{b}{v_f}}.$$
(10)

In Eq. (10), u, v represents the velocity components along the x- and y-directions, respectively.  $\theta(\eta)$  is the dimensionless temperature, defined as  $\frac{T-T_\infty}{T_w-T_\infty}$ , where T is the temperature,  $T_w$  is the surface temperature, and  $T_\infty$  is the free-stream temperature. Further,  $\eta$  is the similarity variable, defined as  $y\sqrt{\frac{b}{v_{\rm f}}}$ , where y is the spatial coordinate perpendicular to the flow, b is the constant, and  $v_{\rm f}$  is the kinematic viscosity. The similarity variable  $\eta$  is introduced to reduce the partial differential equations to ordinary differential equations (ODEs).

Using these similarity variables, Eqs (2)–(4) are reduced to

$$\frac{\alpha_1}{\alpha_2} f'''(\eta) - (f'(\eta))^2 + f(\eta)f''(\eta) - \frac{\alpha_3}{\alpha_2} M \sin^2(\gamma) f'(\eta) - \frac{\alpha_1}{\alpha_2} K f'(\eta) = 0,$$
(11)

$$\frac{1}{\alpha_5}(\alpha_4 + Rd)\theta''(\eta) + \frac{Pr}{\alpha_5}(f(\eta)\theta'(\eta) + \alpha_1 EcM \sin^2(\gamma)(f'(\eta))^2 + Q_{Exp}e^{(-n\eta)} + Q_I\theta(\eta)) = 0,$$
(12)

with the following conditions:

**Table 2:** Shape factor values of the nanoparticles [64,65]

Shapes	Sphere	Tetrahedron	Hexahedron	Lamina	Column
m	3	4.0613	3.7221	16.1576	6.3698

$$f(0) = 0, \quad f'(0) = 1 + \delta_1 f''(0), \quad f'(\infty) \to 0,$$
  
 $\theta(0) = 1 + \delta_2 \theta'(0), \quad \theta(\infty) \to 0.$  (13)

In the above equations, M is the magnetic factor, K is the porosity factor, Rd represents the thermal radiation factor, Pr represents the Prandtl number, Ec represents the Eckert number,  $Q_{\rm Exp}$  represents the exponential heat source,  $Q_{\rm I}$  represents the thermal-dependent heat source,  $\delta_1$  is the velocity slip factor, and  $\delta_2$  represents the temperature slip factor. These factors are defined as follows:

$$\begin{cases} \alpha_{1} = \frac{\mu_{\text{nf}}}{\mu_{\text{f}}}, \quad \alpha_{2} = \frac{\rho_{\text{nf}}}{\rho_{\text{f}}}, \quad \alpha_{3} = \frac{\sigma_{\text{nf}}}{\sigma_{\text{f}}}, \quad \alpha_{4} = \frac{k_{\text{nf}}}{k_{\text{f}}}, \\ \alpha_{5} = \frac{(\rho C_{\text{p}})_{\text{nf}}}{(\rho C_{\text{p}})_{\text{f}}}, \quad M = \frac{\sigma_{\text{f}} B_{0}^{2}}{b \rho_{\text{f}}}, \quad K = \frac{\mu_{\text{f}}}{b \rho_{\text{f}} K_{\text{p}}}, \\ Q_{\text{Exp}} = \frac{Q_{t}}{b (\rho C_{\text{p}})_{\text{f}}}, \quad \text{Ec} = \frac{u_{w}^{2}}{(C_{\text{p}})_{\text{f}} (T_{w} - T_{\infty})}, \\ \text{Pr} = \frac{v_{\text{f}} (\rho C_{\text{p}})_{\text{f}}}{k_{\text{f}}}, \quad \delta_{1} = \sigma_{1} \sqrt{\frac{b}{v_{\text{f}}}}, \quad \delta_{2} = \sigma_{2} \sqrt{\frac{b}{v_{\text{f}}}}, \\ \text{Rd} = \frac{16\sigma^{*} T_{\infty}^{3}}{3k^{*} k_{\text{f}}}, \quad Q_{I} = \frac{Q_{e}}{b (\rho C_{\text{p}})_{\text{f}}}. \end{cases}$$

$$(14)$$

The skin friction ( $C_{fx}$ ) and local Nusselt number (Nu<sub>x</sub>) are given as:

$$C_{fx} = \frac{\tau_w}{\rho_f(u_w(x))^2}, \quad \text{Nu}_x = \frac{xq_w}{k_f(T_w - T_\infty)},$$
 (15)

with

$$\tau_{w} = \mu_{\text{nf}} \frac{\partial u}{\partial y} \bigg|_{y=0},$$

$$q_{w} = -k_{\text{nf}} \left[ \frac{\partial T}{\partial y} \bigg|_{y=0} - \frac{16\sigma^{*}}{3k^{*}} \frac{\partial T^{4}}{\partial y} \bigg|_{y=0} \right].$$

Thus, Eq. (15) is reduced to

$$C_{\rm f} = \sqrt{\text{Re}_{\rm x}} C_{fx} = \alpha_1 f''(0), \quad \frac{\text{Nu}_{\rm x}}{\sqrt{\text{Re}_{\rm x}}} = -(\alpha_4 + \text{Rd})\theta'(0), \quad (17)$$

where  $\mathrm{Re}_{x} = \frac{bx^{2}}{\nu_{\mathrm{f}}}$  is the Reynolds number (local).

# 3 Numerical solution

Eqs (11) and (12) are highly nonlinear, so to solve them with the boundary conditions given in Eq. (13), the bvp4c technique is used. It is a numerical approach that is widely used to evaluate boundary value problems in the field of computational mathematics and engineering. In addition, it offers the advantage of efficiently handling complex boundary conditions and nonlinearities, making it a valuable tool in scientific computing and engineering analysis. To ensure the accuracy of the applied numerical technique, an error tolerance of  $10^{-6}$  was applied. This value is sufficiently small to minimize the numerical error and confirm the convergence and stability of the solution. To apply this technique, the given higher-order ODEs must be converted into first-order ODEs. Therefore, we assume that

$$f = \chi(1), \quad f' = \chi(2), \quad f'' = \chi(3), \quad f''' = \chi'(3),$$
  
 $\theta = \chi(4), \quad \theta' = \chi(5), \quad \theta'' = \chi'(5).$  (18)

Using Eq. (18), Eqs (11) and (12) along with Eq. (13) are transformed as  $\frac{1}{2}$ 

$$\chi'(3) = -\left\{\frac{\chi(1)\chi(3) - (\chi(2))^2 - \frac{\alpha_3}{\alpha_2}M\sin^2\gamma\chi(2) - \frac{\alpha_1}{\alpha_2}K\chi(2)}{\frac{\alpha_1}{\alpha_2}}\right\}, \quad (19)$$

$$\chi'(5) = - \begin{cases} \frac{\Pr}{a_5} (\chi(1)\chi(5) + a_1 \text{Ec} M \sin^2 \gamma (\chi(2))^2 + Q_{\text{Exp}} e^{(-n\eta)} + Q_I \chi(4)) \\ \frac{1}{a_5} (a_4 + \text{Rd}) \end{cases}, (20)$$

and

(16)

$$\begin{split} &\chi_{\text{initial}}(1)-0, \ \chi_{\text{initial}}(2)-\{1+\delta_1\chi_{\text{initial}}(3)\}, \\ &\chi_{\text{boundary}}(2)-0, \\ &\chi_{\text{initial}}(4)-\{1+\delta_2\chi_{\text{initial}}(5)\}, \ \chi_{\text{boundary}}(4)-0. \end{split}$$

## 4 Validation

To confirm the validation of the current study, a comparative analysis is carried out in Table 2 that matches current results with established works of Hamad [66], Wang [67], and Reddy Gorla and Sidawi [68]. By varying the values of the Prandtl number while keeping all the other factors at zero, a fine agreement has been noticed in this table that ensures the validation of the current study (Table 3).

### 5 Results and discussion

This study investigates thermally radiative nanofluids flowing over a porous surface. The flow dynamics are affected by the collective impacts of exponential and thermal-dependent heat sources. Additionally, an inclined

Table 3: Comparison of the current and published results when all other factors are zero

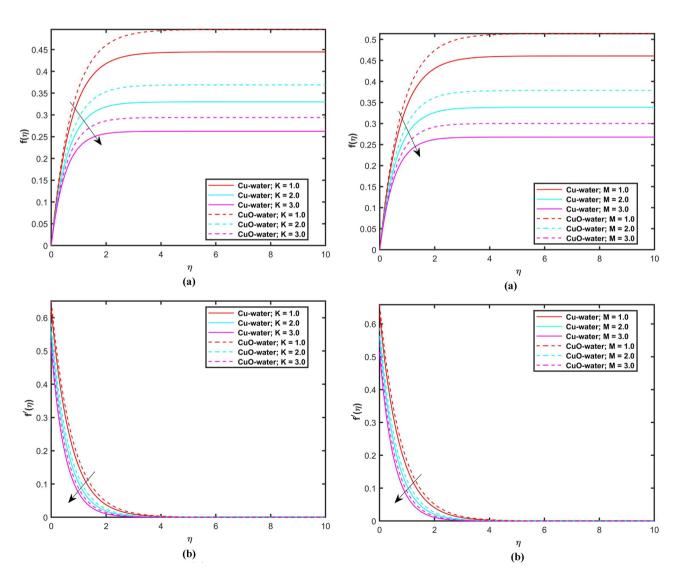
Pr	0.07	0.2	0.7	2	7	20	70
Hamad [66]	0.06556	0.16909	0.45391	0.91136	1.8954	3.3539	6.4622
Wang [67]	0.0656	0.1691	0.4539	0.9114	1.8954	3.3539	6.4622
Reddy Gorla and Sidawi [68]	0.0656	0.1691	0.4539	0.9114	1.8954	3.3539	6.4622
Present results	0.065571	0.169089	0.45391	0.911363	1.895413	3.353802	6.462193

magnetic effect is introduced to the flow system. The velocity and thermal slip conditions are imposed to investigate the nanofluid velocity and temperature distributions. The bvp4c Matlab built-in function is used to solve the modeled problem. The influences of various factors on velocity and thermal profiles are discussed in Figures 2–17 and Tables 4–15. The default values of factors are considered as  $1.0 \le K \le 3.0$ ,  $1.0 \le M \le 3.0$ ,  $30^\circ \le \gamma \le 90^\circ$ ,  $0.1 \le \delta_1 \le 10^\circ$ 

0.5,  $0.1 \le \text{Ec} \le 0.5$ ,  $0.1 \le \delta_2 \le 0.5$ ,  $0.1 \le Q_{\text{Exp}} \le 0.5$ ,  $0.1 \le Q_{\text{D}} \le 0.5$ , and  $0.1 \le \text{Rd} \le 0.5$ .

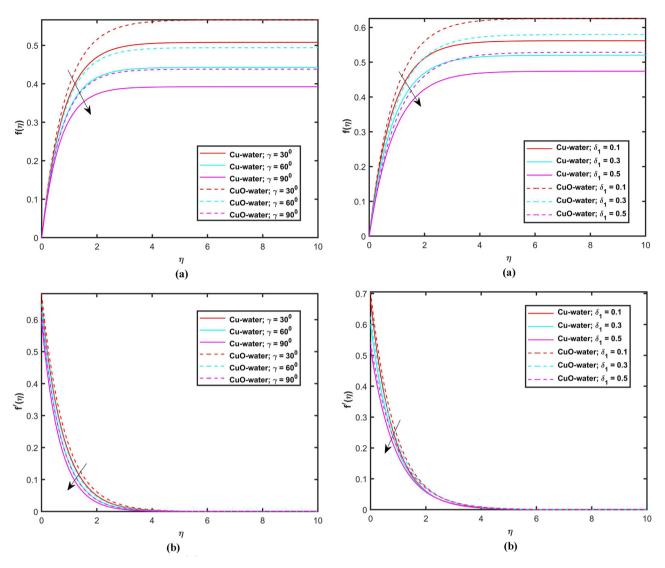
### 5.1 Velocity distributions

The impressions of diverse factors on velocity distributions  $(f(\eta), f'(\eta))$  are depicted in Figures 2–4. Figure 2(a) and (b)



**Figure 2:** (a) and (b) Behavior of  $f(\eta)$  and  $f'(\eta)$  against K.

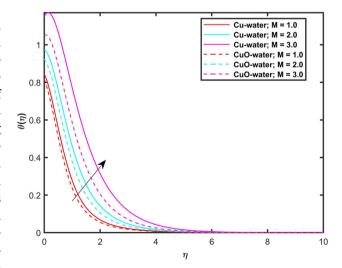
**Figure 3:** (a) and (b) Behavior of  $f(\eta)$  and  $f'(\eta)$  against M.



**Figure 4:** (a) and (b) Behavior of  $f(\eta)$  and  $f'(\eta)$  against  $\gamma$ .

**Figure 5:** (a) and (b) Behavior of  $f(\eta)$  and  $f'(\eta)$  against  $\delta_1$ .

shows the impression of the porosity factor (K) on ( $f(\eta)$ ,  $f'(\eta)$ ). Here, we observed that the greater K reduces both  $f(\eta)$  and  $f'(\eta)$ . Actually, the introduction of porous behavior on the stretching surface signifies an increase in the surface's effective permeability due to the presence of expanding pores. This augmentation in porosity facilitates the passage of fluid through the surface, thereby increasing the resistance encountered by the flowing fluid. When the resistance force increases with increasing porosity factor, the velocity profiles reduce as a result. From the obtained results in Figure 2(a) and (b), it is seen that the porous factor affects the CuO-water nanofluid flow more than the Cu-water nanofluid flow. Actually, the changes in the porous structure have a stronger impact on the flow behavior of CuO-water compared to Cu-water. This is due to the differences in physical properties like viscosity,



**Figure 6:** Behavior of  $\theta(\eta)$  against M.

10

Cu-water; Q<sub>Exp</sub> = 0.1

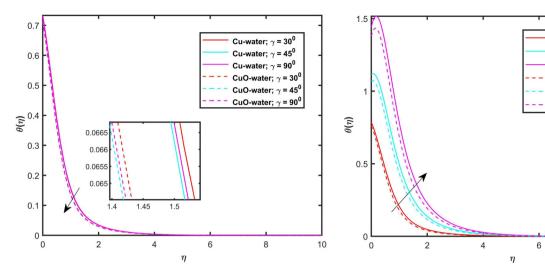
Cu-water; Q<sub>Exp</sub> = 0.3

Cu-water; Q<sub>Exp</sub> = 0.5

CuO-water; Q<sub>Exp</sub> = 0.1

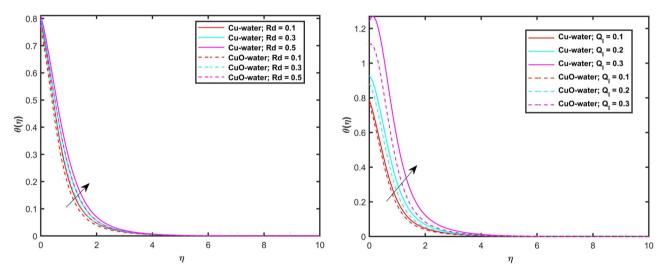
CuO-water; Q<sub>Exp</sub> = 0.3

CuO-water; Q<sub>Exp</sub>



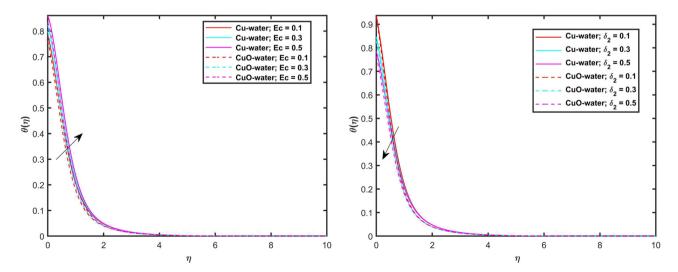
**Figure 7:** Behavior of  $\theta(\eta)$  against  $\gamma$ .

**Figure 10:** Behavior of  $\theta(\eta)$  against  $Q_{\rm Exp}$ .



**Figure 8:** Behavior of  $\theta(\eta)$  against Rd.

**Figure 11:** Behavior of  $\theta(\eta)$  against  $Q_I$ .



**Figure 9:** Behavior of  $\theta(\eta)$  against Ec.

**Figure 12:** Behavior of  $\theta(\eta)$  against  $\delta_2$ .

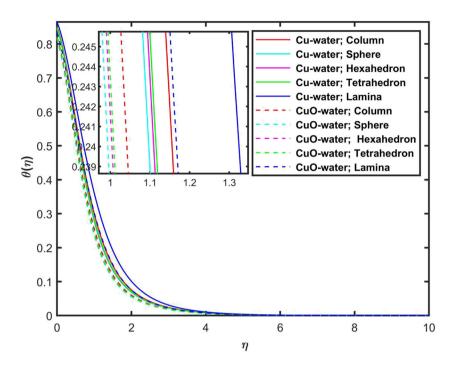
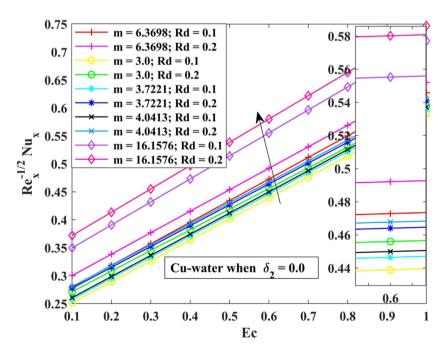
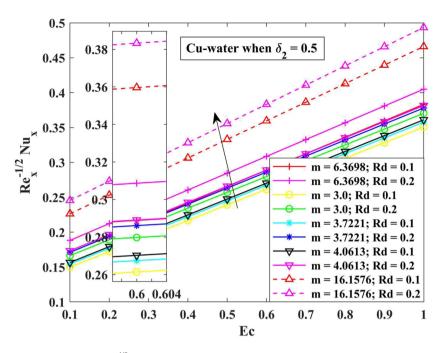


Figure 13: Variations in temperature distributions of the Cu–water and CuO–water nanofluids flows with different shapes of Cu and CuO nanoparticles.

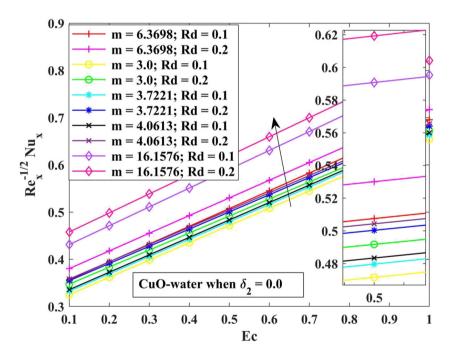
thermal conductivity, or particle concentration between the two nanofluids. As a result, the CuO-water nanofluid experiences more noticeable changes in velocity or flow pattern when the porosity factor is varied, indicating a higher sensitivity to the medium's structure. Figure 3(a) and (b) demonstrates the variation in  $f(\eta)$  and  $f'(\eta)$  via greater M. The increase in M implies a stronger impact of magnetic force on the nanofluid flow. Physically, this can be understood as the magnetic field imposing resistance on the nanofluid flow, effectively impeding its motion. As M



**Figure 14:** Variations in the Nusselt number  $(Re_x^{-1/2}Nu_x)$  *via* Rd and Ec in the case of Cu–water nanofluid flow when  $\delta_2 = 0.0$ .



**Figure 15:** Variations in the Nusselt number  $(Re_x^{-1/2}Nu_x)$  *via* Rd and Ec in the case of Cu–water nanofluid flow when  $\delta_2 = 0.5$ .



**Figure 16:** Variations in the Nusselt number ( $Re_x^{-1/2}Nu_x$ ) *via* Rd and Ec in the case of CuO-water nanofluid flow when  $\delta_2 = 0.0$ .

increases, the intensity of this resistance increases, causing a reduction in  $f(\eta)$  and  $f'(\eta)$ . This phenomenon arises from the association between the magnetic field and the fluid's magnetic susceptibility, leading to alteration in the fluid's momentum distribution and ultimately slowing down its movement. Hence, the increase in M directly correlates with a decrease in fluid velocities, reflecting

the significant impact of the magnetic force on the nanofluid flow behavior. When comparing the  $Cu-H_2O$  nanofluid to the  $CuO-H_2O$  nanofluid, the presence of CuO nanoparticles alters the fluid's magnetic susceptibility and interaction with the applied magnetic field effect. This alteration results in a less significant decrease in the velocity of the  $CuO-H_2O$  nanofluid compared to the  $Cu-H_2O$ 

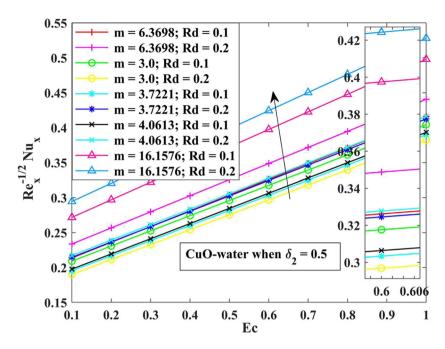


Figure 17: Variations in the Nusselt number ( $Re_v^{-1/2}Nu_v$ ) via Rd and Ec in the case of CuO-water nanofluid flow when  $\delta_2 = 0.5$ .

nanofluid. Physically, this suggests that the magnetic field exerts a more noticeable decelerating consequence on the Cu-H<sub>2</sub>O nanofluid flow because of its higher magnetic susceptibility, leading to greater resistance against the stretching motion of the surface. Conversely, the occurrence of CuO nanoparticles in the nanofluid mitigates this effect to some extent, resulting in a relatively smaller reduction in  $f(\eta)$  and  $f'(\eta)$ , as shown in Figure 4(a) and (b). These figures validate that the velocities  $f(\eta)$  increase with an increase in  $\gamma$ . The increase in  $\gamma$  corresponds to a change in the direction of the magnetic force acting on the nanofluid flow along a stretching surface. Physically, this alteration in y distresses how the magnetic field interrelates with the nanofluid, potentially enhancing the stretching and alignment of the fluid flow. As  $\nu$  increases, the magnetic field experiences a better influence by the nanofluid flow, thereby promoting more declining velocity of the nanofluid flows. From the obtained results, it was found that the magnetic field influenced the nanofluid flows more

when the angle was 90°. We call this type of applied magnetic field the transverse magnetic field. It was also found that velocity panels of the Cu-H<sub>2</sub>O nanofluid flow are greatly influenced by higher M because the electrical conductivity of the Cu nanoparticles is better than that of CuO nanoparticles. Figure 5(a) and (b) demonstrates the variation in  $f(\eta)$  and  $f'(\eta)$  via the velocity slip factor ( $\delta_1$ ). When  $\delta_1$  increases, it indicates an enhanced slip or deviation of the nanofluid velocity at the surface in comparison to the no-slip condition. This slip implies that the fluid molecules close to the surface move faster or slower than the surface itself, resulting in a reduction in  $f(\eta)$  and  $f'(\eta)$ .

### 5.2 Thermal distribution

The effects of numerous factors on the thermal distribution  $\theta(\eta)$  are shown in Figures 6–12. Figure 6 illustrates the

**Table 4:** Impact of Ec on the heat transfer rate of the Cu–water nanofluid when  $\delta_2$  = 0.0

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Ec	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.1576
0.1	0.5500258982	0.5138053375	0.5218766181	0.5256075260	0.6375105888
0.2	0.5886142049	0.5512667758	0.5595940538	0.5634423141	0.6786305709
0.3	0.6272024650	0.5887282147	0.5973114896	0.6012770126	0.7197530617

**Table 5:** Impact of Ec on the heat transfer rate of the Cu-water nanofluid when  $\delta_2$  = 0.5

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Ec	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	m = 16.1576
0.1	0.5321828479	0.4848875669	0.4952485750	0.5000721469	0.6557037633
0.2	0.5379987284	0.4902938818	0.5007457063	0.5056113427	0.6625367868
0.3	0.5438183911	0.4957002029	0.5062428434	0.5111505442	0.6693698102

**Table 6:** Impact of Rd on the heat transfer rate of the Cu–water nanofluid when  $\delta_2 = 0.0$ 

Shapes → Parameter ↓	Column	sphere	Hexahedron	Tetrahedron	Lamina
Rd	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.1576
0.1	0.6272024650	0.5887282147	0.5973114896	0.6012770126	0.7197530617
0.2	0.6456752125	0.6037442552	0.6130896798	0.6174042117	0.7468879188
0.3	0.6625485083	0.6175992852	0.6276058922	0.6322336027	0.7715460232

impact of the magnetic factor (*M*) on  $\theta(\eta)$ . This augmentation in  $\theta(\eta)$  can be understood as a result of the enhanced energy dissipation due to the increased magnetic forces acting on the fluid particles. Essentially, a higher Mimposes resistance on the nanofluid motion, causing increased frictional heating and thereby elevating the temperature gradient. For the Cu-H<sub>2</sub>O nanofluid matched with the CuO-H<sub>2</sub>O nanofluid, the occurrence of Cu nanoparticles modifies the thermal properties of the nanofluid, leading to a more significant augmentation in the temperature distribution, as depicted in Figure 6. Physically, this can be attributed to the heightened heat transfer capabilities of the nanofluid in the presence of nanoparticles, which interact with the magnetic field to facilitate more efficient heat dissipation. Figure 7 illustrates that  $\theta(\eta)$  declines with an increase in the angle of inclination (y). When yincreases, it implies a deviation of the magnetic lines of force from being perpendicular to the surface. This adjustment reduces the effective strength of the magnetic field acting parallel to surface, which, in turn, diminishes the induced Lorentz force exercised on the fluid; consequently,

the decrease in the frictional heating and thermal transfer within the nanofluid causes a reduction in  $\theta(\eta)$ . Physically, this can be interpreted as a smaller (M) influence on fluid dynamics, resulting in a less pronounced impact on temperature gradients and decrease in  $\theta(\eta)$ . Figure 8 shows that  $\theta(\eta)$  augments with an increase in the radiation factor (Rd). When Rd increases, it indicates a better rate of energy transmission from the surface to the surrounding fluid. This enhanced radiation results in amplified thermal transfer from the surface, which subsequently increases  $\theta(\eta)$ . Physically, the augmentation in  $\theta(\eta)$  can be understood as a result of greater thermal energy loss from the system, leading to a more rapid depletion of the heat available to the nanofluid. For the Cu-H<sub>2</sub>O nanofluid matched with the CuO-H2O nanofluid, the presence of Cu nanoparticles modifies the thermal properties of the fluid, causing augmentation in the temperature profile, as shown in Figure 8. Figure 9 shows that  $\theta(\eta)$  augments with an increase in the Eckert number (Ec). When Ec increase, it implies a higher ratio of kinetic energy to enthalpy change in the nanofluid flow. This signifies that more of the energy

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**Table 7:** Impact of Rd on the heat transfer rate of the Cu–water nanofluid when  $\delta_2$  = 0.5

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Rd	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.1576
0.1	0.4479725362	0.4097581918	0.4181507221	0.4445721225	0.5467894505
0.2	0.4739733867	0.4331093030	0.4420774964	0.4703341655	0.5799366421
0.3	0.4985422898	0.4551437556	0.4646645597	0.4946750448	0.6113375818

**Table 8:** Impact of M on the heat transfer rate of the Cu–water nanofluid when  $\delta_2 = 0.0$ 

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
$\overline{M}$	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.15760
0.1	0.6879867431	0.6456006690	0.6550379169	0.6594016178	0.7910766290
0.2	0.7196352530	0.6752505076	0.6851251604	0.6896926205	0.8280855561
0.3	0.7522465074	0.7058272617	0.7161476742	0.7209226719	0.8661410723

provided to the system is transformed into kinetic energy rather than being absorbed as heat. Consequently, with the higher Ec, the flow carries more kinetic energy, which leads to increased heat transfer. This augmentation in  $\theta(\eta)$  is a result of enhanced energy dissipation, where a better portion of flow energy is altered to thermal energy due to heightened fluid motion. In the case of the Cu-water nanofluid compared to the CuO-water nanofluid, the presence of Cu nanoparticles modifies the thermal properties of the fluid, leading to a more significant augmentation in temperature distribution, as depicted in Figure 9. Figure 10 shows that  $\theta(\eta)$  augments with an increase in the exponential heat source factor ( $Q_{\rm Exp}$ ). When the exponential heat source factor increases, it implies a higher rate of heat generation within the fluid due to an exponential increase in the heat source. This additional heat input contributes to an augmentation in  $\theta(\eta)$ . Physically, the increase in  $Q_{\text{Eyn}}$ results in more energy being released into the fluid, causing heightened thermal energy dissipation and subsequently higher temperatures within the nanofluid flow domain. In the case of Cu-water nanofluid compared to

the CuO-water nanofluid, the presence of Cu nanoparticles modifies the thermal properties of the fluid, causing better augmentation in  $\theta(\eta)$ , as depicted in Figure 10. Figure 11 shows that  $\theta(\eta)$  increase with an increase in  $(O_t)$ . When  $O_t$ increases, then heat generation within the nanofluid is directly influenced by its temperature. As the temperature of the nanofluid increases, the heat source factor also increases, leading to a higher temperature distribution. This increase in  $Q_I$  leads to an increase in  $\theta(\eta)$ . In the case of Cu-water nanofluid compared to the CuO-water nanofluid, the presence of Cu nanoparticles modifies the thermal properties of the fluid, causing a more substantial augmentation in temperature distribution, as depicted in Figure 11. Figure 12 shows that  $\theta(\eta)$  declines with an increase in the thermal slip factor ( $\delta_2$ ). When  $\delta_2$  increases, it indicates an enhanced ability of the fluid molecules to exchange heat with the surface. This means that the fluid molecules can more effectively transfer thermal energy across the boundary layer, resulting in a reduction in  $\theta(\eta)$ . Physically, an increase in  $\delta_2$  promotes more efficient heat transfer, allowing the nanofluid to carry away heat

**Table 9:** Impact of M on the heat transfer rate of the Cu–water nanofluid when  $\delta_2$  = 0.5

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
M	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	m = 16.15760
0.1	0.5024227430	0.4583517342	0.4680202806	0.4725188871	0.6166583180
0.2	0.5229628390	0.4768784077	0.4869819136	0.4916842033	0.6428619407
0.3	0.5438183911	0.4957002029	0.5062428434	0.5111505442	0.6693698102

**Table 10:** Impact of Ec on the heat transfer rate of the CuO–water nanofluid when  $\delta_2$  = 0.0

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Ec	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	m = 16.1576
0.1	0.8902787300	0.8263632989	0.8407061367	0.8473165342	1.040542310
0.2	0.8989690336	0.8345874477	0.8490357722	0.8556944761	1.050252470
0.3	0.9076531895	0.8428115964	0.8573654077	0.8640723984	1.059962631

**Table 11:** Impact of Ec on the heat transfer rate of the CuO-water nanofluid when  $\delta_2 = 0.5$ 

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Ec	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	m = 16.1576
0.1	0.5687866175	0.5202281081	0.5310228273	0.5360177574	0.6875476919
0.2	0.5743359023	0.5254064073	0.5362841482	0.5413177023	0.6939637512
0.3	0.5798860422	0.5305829422	0.541545469	0.5466176383	0.7003798104

more efficiently and, consequently, the temperature gradient along the stretching surface decreases. Figure 13 depicts that the temperature distribution has different behaviors against the different shapes of nanoparticles. There is maximum growth in  $\theta(\eta)$  for the lamina-shaped nanoparticles. In the case of lamina-shaped nanoparticles, there tends to be a maximum increase in thermal flow. This is because lamina-shaped nanoparticles typically have a larger surface area compared to other shapes for the same volume, which promotes greater interaction with the surrounding nanofluid. As a result, lamina-shaped nanoparticles can effectively enhance heat transfer by increasing the contact area between the fluid and the nanoparticles. This increased surface area facilitates more efficient heat exchange, leading to a higher rate of thermal energy transfer and consequently a greater augmentation in temperature distribution within the nanofluid flow. Therefore, in systems where effective heat transfer is desired, the presence of lamina-shaped nanoparticles can significantly influence and maximize the thermal flow behavior. Again in the case of Cu-water nanofluid compared to the CuO-water nanofluid, the presence of Cu nanoparticles modifies the thermal properties of the fluid, leading to a more significant augmentation in  $\theta(\eta)$ , as depicted in Figure 13.

(Ec) when  $\delta_2$  = 0.0 and  $\delta_2$  = 0.5 for the Cu–water nanofluid. As Rd increases, it indicates that radiative heat transfer becomes more significant in contributing to the overall heat transfer process. This augmentation in Re<sub>v</sub><sup>-1/2</sup>Nu<sub>v</sub> suggests that the convective heat transfer is enhanced due to the additional heat transfer mechanism introduced by radiation. Furthermore, the higher heat transfer rate is found for lamina-shaped nanoparticles in the presence and absence of thermal slip conditions. Figures 16 and 17 depict that Re<sub>x</sub> -1/2 Nu<sub>x</sub> augments with an increase in Rd and Ec when  $\delta_2$  = 0.0 and  $\delta_2$  = 0.5 for the CuO–water nanofluid. This trend suggests that increasing Rd enhances the radiative heat transfer contribution, while increasing Ec augments the convective heat transfer. In the case of  $\delta_2$  = 0.5, where there is a relative slip between the fluid and surface, the Nusselt number further increases due to enhanced fluid mixing and increased convective heat transfer. Under no-slip conditions,  $Re_x^{-1/2}Nu_x$  still increases with Ec, indicating that convective heat transfer dominates despite the absence of slip. These trends highlight the combined influence of radiation and convective heat transfer mechanisms on heat transfer enhancement in the CuOwater nanofluid. Furthermore, the higher heat transfer rate is found for lamina-shaped nanoparticles in the presence and absence of thermal slip conditions.

#### 5.3 Nusselt number

Figures 14 and 15 depict that  $Re_x^{-1/2}Nu_x$  increases with an increase in the radiation factor (Rd) and Eckert number

#### 5.4 Table discussion

The impacts of various factors on  $Re_x^{-1/2}Nu_x$  regarding Cu–water and CuO–water nanofluids are depicted in

**Table 12:** Impact of Rd on the heat transfer rate of the CuO–water nanofluid when  $\delta_2$  = 0.0

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Rd	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.1576
0.1	0.8133207011	0.7650727653	0.7759434836	0.7809461591	0.9250412488
0.2	0.8389160014	0.7858160329	0.7977718794	0.8032740654	0.9621856566
0.3	0.8631182582	0.8057018763	0.8186166398	0.8245627745	0.9968976138

**Table 13:** Impact of Rd on the heat transfer rate of the CuO-water nanofluid when  $\delta_2$  = 0.5

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
Rd	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.1576
0.1	0.4750996874	0.4362669660	0.4449196398	0.4489195558	0.5692057223
0.2	0.5032848123	0.4616647800	0.4709328806	0.4752183306	0.6043920095
0.3	0.5300707465	0.4857794328	0.4956366174	0.5001956787	0.6379036944

**Table 14:** Impact of M on the heat transfer rate of the CuO-water nanofluid when  $\delta_2 = 0.0$ 

Shapes → Parameter ↓	Column	sphere	Hexahedron	Tetrahedron	Lamina
M	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	<i>m</i> = 16.15760
0.1	0.8387346180	0.7791929008	0.7925697591	0.7987317128	0.977951303
0.2	0.8726977989	0.8105372556	0.8244957637	0.8309273315	1.018400033
0.3	0.9076531895	0.8428115964	0.8573654077	0.8640723984	1.059962631

**Table 15:** Impact of M on the heat transfer rate of the CuO-water nanofluid when  $\delta_2$  = 0.5

Shapes → Parameter ↓	Column	Sphere	Hexahedron	Tetrahedron	Lamina
M	m = 6.3698	m = 3.0	m = 3.7221	m = 4.0613	m = 16.15760
0.1	0.5423729946	0.4965025902	0.5067094298	0.5114305183	0.6540461149
0.2	0.5609563373	0.5133812346	0.5239635359	0.5288587981	0.6770193930
0.3	0.5798860422	0.5305829422	0.5415454690	0.5466176383	0.7003798104

Tables 4–15 for both  $\delta_2$  = 0.0 and  $\delta_2$  = 0.5 conditions. Tables 4 and 5 show the impacts of the Eckert number (Ec)numerically on  $\operatorname{Re}_{x}^{-1/2}\operatorname{Nu}_{x}$  by keeping  $\delta_{2}=0.0$  and  $\delta_{2}=0.5$  while all other factors as fixed. It was observed from these tables that when  $\delta_2 = 0.0$ , the values of  $\text{Re}_x^{-1/2} \text{Nu}_x$  increase more quickly for lamina-shaped nanoparticles with variation in Ec. Tables 6 and 7 show the impacts of the radiation factor Rd numerically on  $Re_x^{-1/2}Nu_x$  by keeping  $\delta_2 = 0.0$  and  $\delta_2$  = 0.5, while all other factors are fixed. It was observed from these tables that when  $\delta_2 = 0.0$ , the values of  $Re_x^{-1/2}Nu_x$  increase more quickly for lamina-shaped nanoparticles with variation in Rd. Tables 8 and 9 show the impacts of the magnetic factor (M)numerically on  $\text{Re}_x^{-1/2}\text{Nu}_x$  when  $\delta_2 = 0.0$  and  $\delta_2 = 0.5$  while all other factors are fixed. It was observed from these tables that when  $\delta_2 = 0.0$ , the values of  $Re_x^{-1/2}Nu_x$  increase more quickly for lamina-shaped nanoparticles with variation in M. Tables 10 and 11 show the impacts of the Eckert number (Ec) numerically on  $\text{Re}_x^{-1/2}\text{Nu}_x$  when  $\delta_2 = 0.0$  and  $\delta_2 = 0.5$  while all other factors are fixed and considering the CuO-water nanofluid. It was observed from these tables that when

 $\delta_2=0.0$ , the values of  $\mathrm{Re}_x^{-1/2}\mathrm{Nu}_x$  increase more quickly for lamina-shaped nanoparticles with variation in Ec. Tables 12 and 13 show the impacts of the radiation factor (Rd) numerically on  $\mathrm{Re}_x^{-1/2}\mathrm{Nu}_x$  when  $\delta_2=0.0$  and  $\delta_2=0.5$  while all other factors are fixed and considering the CuO—water nanofluid. It was noticed from these tables that when  $\delta_2=0.0$  the values of  $\mathrm{Re}_x^{-1/2}\mathrm{Nu}_x$  increase more quickly for Lamina-shaped nanoparticles with variation in Rd. Tables 14 and 15 show the impact of the magnetic factor M numerically on  $\mathrm{Re}_x^{-1/2}\mathrm{Nu}_x$  when  $\delta_2=0.0$  and  $\delta_2=0.5$  while all other factors are fixed, and considering the CuO—water nanofluid. It was observed from these tables that when  $\delta_2=0.0$ , the values of  $\mathrm{Re}_x^{-1/2}\mathrm{Nu}_x$  increase more quickly for lamina-shaped nanoparticles with variation in M.

### 6 Conclusion

This study investigates thermally radiative nanofluid flows over a surface using porous media. The flow dynamics are affected by the combined impacts of exponential and temperature-dependent heat sources. Additionally, the inclined magnetic effect was introduced to the flow system. The flow in the system is induced by the stretching nature of the sheet. The textured surface of the stretching sheet facilitates the exploration of velocity and thermal slip conditions. The impacts of different factors on the velocity, thermal skin friction, and heat transfer rate is discussed in detail. Based on the above analysis, the following conclusions are drawn.

- As the porosity factor, velocity slip factor, and magnetic factor increase, they impose greater resistance on the fluid flow, leading to a decline in the velocity distributions. The reduction is more pronounced in Cu-water nanofluid due to the stronger resistive effects, such as higher density and stronger magnetic interaction, which impede the flow.
- CuO—water nanofluids experience relatively less resistance because of the lower density and better stability of CuO nanoparticles, allowing them to maintain higher velocities with an increase in the porosity factor, velocity slip factor, and magnetic factor.
- Both velocity distributions decline with increasing values of inclination angle with respect to the magnetic field effects. Moreover, these velocities are maximum when the angle of inclination is 90°. This occurs because the magnetic field's impact on the fluid is minimized in this configuration, allowing the fluid to flow more freely.
- Thermal distribution increases with an increase in the magnetic factor, radiation factor, Eckert number, exponential heat source, space-based heat source, and decreases with an increase in the inclination angle and thermal slip factor.
- The Nusselt number increases for both types of nanofluids with increases in various emerging factors in the scenarios of thermal slip and no-slip, where the increase in the Nusselt number is maximum for the scenario where there is no thermal slip.
- The higher thermal distribution and heat transfer rate are determined for the lamina-shaped Cu-water and CuO-water nanofluid flows under both slip and no-slip thermal conditions.
- This study aids industrial cooling by optimizing nanofluid-based heat exchangers, improving thermal performance in microchips, turbines, and reactors. In biomedical applications, enhanced heat transfer supports targeted drug delivery, thermal therapies, and precise temperature regulation in medical devices, where nanoparticle shape control enables more efficient and safer thermal management under complex flow conditions.

### 7 Future research directions

In future work, some other nanoparticle materials like rod, cube, disk, wire, star-shaped, prism, and ellipsoid will be tested to check their impacts on the heat transfer rate. By expanding the range of particle shapes, the study will aim to identify optimal geometries that maximize heat transfer efficiency under varying flow conditions. This will contribute to the development of more efficient nanofluid-based thermal management systems for industrial and technological applications.

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**Data availability statement:** The datasets generated and/ or analyzed during the current study are available from the corresponding author on reasonable request.

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