

Research Article

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Mathematical analysis of nanoparticle type and volume fraction on heat transfer efficiency of nanofluids

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Abstract: Nanofluids (NFs) have been implemented in several areas to increase heat transfer efficiency. Thus, efficiency for heat energy can be achieved. In this study, the effect of nanoparticle (NP) type, volume fraction, and Re number on the heat transfer efficiency of NFs were analyzed numerically, statistically, and theoretically. Heat transfer coefficient, number of transfer units, wall shear stress, and friction factor were selected as the heat transfer efficiency of NFs. ANSYS Fluent software was utilized to carry out computational fluid dynamics analyses. The numerical calculation scheme was implemented by employing the Taguchi L9 orthogonal array with three decisive factors. NP type, volume fraction, and Re number were assumed as decisive factors with three levels. Signal-to-noise ratio analysis was utilized to determine the direction of impact and ideal levels of each decisive factor on the heat transfer efficiency of NFs. Significance levels and contribution rates of the decisive factors on the heat transfer efficiency were calculated with Analysis of Variance. According to the mathematical responses, the most effective NPs on h and τ_w were identified as Gr, Al_2O_3 , and Cu, respectively, whereas the most effective NPs on number of transfer units are found to be Cu, Al_2O_3 , and Gr, respectively. In addition, the increase in Re number from 6,000 to 8,000 causes an increase in h and τ_w and a decrease in NTU and f . The data achieved from the mathematical research may be utilized to be a guide paper in experimental analyses.

Keywords: ANOVA, fluid dynamics, heat transfer efficiency, nanoparticle type, Taguchi approach

Nomenclature

| | |
|------------------------------|---|
| A_c | cross-sectional area of tube at inlet |
| ANOVA | analysis of variance |
| A_{sr} | tube surface area |
| $C_{1e}, C_2, C_{3e}, C_\mu$ | constants |
| $C_{p,nf}$ | specific heat of NFs |
| c_p | specific heat |
| D_{Tube} | diameter of tube |
| E | energy |
| \vec{F} | external body forces |
| f | friction factor |
| G_k | emergence of turbulence kinetic energy because of the mean velocity gradients |
| G_b | emergence of turbulence kinetic energy because of buoyancy |
| g | gravity |
| HTE | heat transfer efficiency |
| h | heat transfer coefficient |
| k_{nf} | thermal conductivity of NF |
| k_{bf} | thermal conductivity based on base fluid |
| k | turbulence kinetic energy |
| k | thermal conductivity of the fluid |
| \bar{M}_i | average HTE value at optimum levels for particle |
| \dot{m} | mass flow rate of fluid |
| NFs | nanofluids |
| NP | nanoparticle |
| NTU | number of transfer units |
| \overline{Nu}_D | Nusselt's number |
| Pr | Prandtl numbers |
| \dot{Q} | rate of heat transfer |
| \overline{Re}_i | average HTE value at optimum levels for Re number |
| Re | Reynolds number |
| \vec{r} | location vector for the field point |
| $\vec{\tau}_w$ | combination of all relevant wall boundaries |
| S_k, S_ϵ | source terms specified by the user |

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| | |
|-------------------|---|
| S/N | signal-to-noise |
| S_m | mass added to the continuous phase from the dispersed second phase |
| T_e, T_i | exit and inlet temperature of fluid |
| $T_{f,ave}$ | average fluid temperature |
| TI | turbulence intensity |
| \bar{T}_{OM} | overall mean |
| T_s | average temperature of wall surface |
| t | time |
| \overline{VF}_i | average HTE value at optimum levels for volume fraction |
| v | fluid velocity |
| Y_M | impact of the fluctuating dilatation for compressible turbulence to the mean dissipation rate |
| y | normal remoteness from the wall at cell centers |
| μ | viscosity of the fluid |
| μ_t | Eddy viscosity |
| σ_k | turbulent Prandtl numbers according to k |
| σ_e | turbulent Prandtl numbers according to e |
| ρ | fluid density |
| $\rho \vec{g}$ | gravitational body force |
| Γ | blending function |
| ϵ | rate of dissipation |
| τ_w | wall shear stress |
| ϕ | volume fraction |
| ρ_{nf} | density of NF |
| ρ_{bf} | density for base fluid |
| μ_{nf} | viscosity of NFs |
| μ_{bf} | viscosity of base fluid |
| $\bar{\mu}_{HTE}$ | optimal heat transfer efficiency |

1 Introduction

Nanofluids (NFs) obtained with nanoparticles (NPs) and base fluids were utilized to increase the heat transmission of the fluid [1,2]. NFs were produced by combining NPs with high thermal conductivity and a working liquid with low thermal conductivity [3]. NPs with high thermal conductivity increase the heat transfer coefficient of NFs [2]. NPs may be grouped under three headings such as metallic, oxide, and carbon [4]. Since each NP has various mechanical, physical, and thermal properties, it can also affect the properties of NFs. Due to these properties of NFs, it may of great potential use in various sectors [5]. Many studies have been reported about various NPs such as Al_2O_3 [6], TiO_2 [7], Cu [8], CuO [9], Cu_2O [10], MgO [11], carbon nanotubes [12], multi-wall carbon nanotubes [13], single-walled carbon

nanotube [14], ZrO_2 [15], SiO_2 [16], Si_3N_4 [3], SiC [17], GO [18], F_3O_4 [19], Ag [20], Ni [21], SnO_2 [22], BN [23], AlN [24], ZnO [25], CB [26], CeO_2 [27]. Due to the large number of NPs, NFs have been produced for use in different areas such as nuclear power plant [28], solar energy systems [29], biomedicine [30], heat exchangers [31], jet impingement [32], lubrication machining [33], automotive application [34], electronic cooling systems [35], *etc.* In addition, different fluids such as water [36], nitride-water [37], engine oil [38], and ethylene glycol [39] have been used as base fluids. Thus, using different base fluids and NPs provide improvements in the thermophysical characteristics of the NFs. Various research works on NFs have been conducted by many scientists in the literature. Among the studies, heat exchangers are particularly prevalent. Calviño *et al.* [15] stated the heat transfer efficiency of ZrO_2 NF using heat exchangers and used four various volume fractions of NPs. Laminar and turbulent flow were chosen for flow. As a result of their study, they found that ZrO_2 can have potential effect for heat exchangers. Zhang *et al.* [40] evaluated the influence of Cu NF in heat exchangers and detected that the increase in Re number and volume fractions of NPs also increased the heat transfer coefficient. Also, they detected that the rise in Re number provides a rise on pressure difference. Fares *et al.* [41] examined that graphene nanofluids (GNF) NFs on heat exchangers stated a 29% increase in heat transfer coefficient and a 19% increase in average thermal efficiency. They also found that GNF NF has an enhancing impact on thermal characteristic. Fule *et al.* [42] improved the heat transfer coefficient of heat exchangers by employing CuO NF and observed a 37.3% improvement compared to working fluid, using 0.1% NPs. Said *et al.* [43] examined CuO NFs using a heat exchanger. They found that NF developed the average heat transfer coefficient by 7% and convective heat transfer by 11.39%. Salameh *et al.* [44] analyzed the impact of various volume fractions of NPs using NFs including CuO, Al_2O_3 , and TiO_2 in heat exchangers. They determined that NFs ensure upper heat transfer coefficient than base fluids. The authors also found that CuO NFs demonstrated the highest performance. Qi *et al.* [45] determined the impact of TiO_2 NF on thermal efficiency and pressure change in heat exchangers and stated that the increase in the volume fraction values of NPs also caused an increase in the heat transfer rate. They observed that NFs exhibited better thermal effectiveness compared to base liquids. Ajeeb *et al.* [46] stated the heat transfer efficiency using Al_2O_3 NF in heat exchangers and reached an improvement of 9.1% for Al_2O_3 in the thermal conductivity. Zheng *et al.* [47] carried out heat transfer improvement analysis utilizing various NFs in heat exchangers and stated that the most suitable concentration for thermal improvement utilizing CuO NF was 0.5% by weight. Bahiraei and Ahmadi [48] numerically carried out thermohydraulic

performance analyses in heat exchangers using alumina-water NFs. They stated that the increase in Re number and concentration play major role on the convective heat transfer and general heat transfer coefficients. In addition to these studies, many studies [49–52] involving NFs and different methods have been conducted. As can be seen from the mentioned literature summary, there are a lot of studies involving computational fluid dynamics (CFD) approaches. Some of these studies have been confirmed experimentally. However, studies containing statistical and theoretical validations are limited in number. In this study, the impacts of NP type, Volume fraction (VF), and Re number in the heat transfer coefficient, number of transfer units, wall shear stress, and friction factor of NFs were analyzed numerically, statistically, and theoretically.

2 Materials

In the numerical, theoretical, and statistical analyses, three different NPs were chosen to create NFs. Each NP has various properties. Thus, the impact of each NP property in the NFs was also determined. The water in the model was determined as base fluid. The properties such as density, specific heat, thermal conductivity, and viscosity of base fluid (water) were used as 998.2 kg/m³, 4,182 J/kg K, 0.6 W/m K, and 0.001003 kg/m s, respectively [53]. The properties for the NPs utilized are listed in Table 1 [54].

To analyze the properties of NFs, different volume fractions of NPs and base fluid were used. Volume fraction is determined as follows [55]:

$$\phi = \frac{V_{np}}{V_{bf} + V_{np}}. \quad (1)$$

Density of NFs is solved as follows [56]:

$$\rho_{nf} = \rho_{bf}(1 - \phi) + \rho_{np}\phi. \quad (2)$$

The specific heat capacities of NFs may be considered as follows [57]:

$$C_{p,nf} = \frac{(1 - \phi)\rho_{bf}C_{p,bf} + \phi\rho_{np}C_{p,np}}{\rho_{nf}}. \quad (3)$$

The thermal conductivity of NF depending on working fluid is examined as follows [58,59]:

Table 1: Properties of NPs [54]

| Properties | Symbol | Unit | Gr | Al ₂ O ₃ | Cu |
|----------------------|--------|-----------------------|-------|--------------------------------|-------|
| Density | ρ | kg m ⁻³ | 2,200 | 3,700 | 8,933 |
| Specific heat | C_p | J/kg °C ⁻¹ | 790 | 880 | 385 |
| Thermal conductivity | k | W/mK | 5,000 | 46 | 401 |

$$\frac{k_{nf}}{k_{bf}} = \frac{(k_{np} + 2k_{bf}) - 2\phi(k_{bf} - k_{np})}{(k_{np} + 2k_{bf}) + \phi(k_{bf} - k_{np})}. \quad (4)$$

The effective viscosity of NFs can be calculated as follows [60]:

$$\mu_{nf} = \mu_{bf} \frac{1}{(1 - \phi)^{2.5}}. \quad (5)$$

Properties of NFs in accordance with Eqs. (1)–(5) are defined in Table 2.

As described in Table 2, the increase in the VFs of the NPs provides an increase in the effective density, thermal conductivity, and viscosity of the NFs. However it leads to a decrease in effective specific heat.

3 Numerical analysis

ANSYS Fluent software was utilized for CFD analysis of the heat transfer efficiency of NFs. CFD approach was used for numerical calculations. A tube of 1,000 mm length and 16 mm diameter was used in modeling. The heat flux of 3,500 W/m²K was applied to the tube. In mesh analyses, MultiZone method with uniform surface mesh, Haxa mapped mesh, and free mesh types was selected. In addition, edge sizing, inflation, and face meshing were utilized to perform precise analysis. Absolute criteria for residuals base on continuity, velocity for x, y, z, energy, k, epsilon was selected as 10⁻⁶. Hybrid model was applied as solution initialization. Coupled scheme in solution methods was chosen. For precise analyses, turbulence intensity values were calculated for each Re number. Turbulence intensity may be considered [61]:

$$T.I = 0.16 \text{ Re}^{-0.125}. \quad (6)$$

Table 2: Properties of NFs

| NFs | ρ (kg m ⁻³) | C_p (J kg °C ⁻¹) | k (W m ⁻¹ °C ⁻¹) | μ (kg/m-s) |
|-------------------------------------|------------------------------|--------------------------------|---|----------------|
| 0.5% Gr | 1004.209 | 4144.844 | 0.609042 | 0.001016 |
| 1.0% Gr | 1010.218 | 4108.131 | 0.618175 | 0.001029 |
| 1.5% Gr | 1016.227 | 4071.851 | 0.627401 | 0.001042 |
| 0.5% Al ₂ O ₃ | 1011.709 | 4121.620 | 0.608699 | 0.001016 |
| 1.0% Al ₂ O ₃ | 1025.218 | 4062.831 | 0.617482 | 0.001029 |
| 1.5% Al ₂ O ₃ | 1038.727 | 4005.572 | 0.626351 | 0.001042 |
| 0.5% Cu | 1037.874 | 4018.596 | 0.609005 | 0.001016 |
| 1.0% Cu | 1077.548 | 3867.224 | 0.618100 | 0.001029 |
| 1.5% Cu | 1117.222 | 3726.603 | 0.627287 | 0.001042 |

The formulas such as continuity, momentum, stress tensor, and energy in finite element software ANSYS Fluent may be determined, respectively as follows [62]:

$$\frac{\partial \rho}{\partial t} + \nabla(\rho \vec{v}) = S_m, \quad (7)$$

$$\frac{\partial}{\partial t}(\rho \vec{v}) + \nabla(\rho \vec{v} \vec{v}) = -\nabla p + \nabla \bar{\tau} + \rho \vec{g} + \vec{F}, \quad (8)$$

$$\bar{\tau} = \mu \left[(\nabla \vec{v} + \nabla \vec{v}^T) - \frac{2}{3} \nabla \vec{v} I \right], \quad (9)$$

$$\frac{\partial(\rho E)}{\partial t} + \nabla \cdot [\vec{v}(\rho E + p)] = \nabla \cdot \left[k_{\text{eff}} \nabla T - \sum_j h_j \vec{j}_j + (\bar{\tau}_{\text{eff}} \cdot \vec{v}) \right] + S_h. \quad (10)$$

The k-epsilon realizable and near wall treatment in the viscos model was selected. The considered transport approach for k and ϵ can be described as follows [62]:

$$\frac{\partial}{\partial t}(\rho k) + \frac{\partial}{\partial x_j}(\rho k u_j) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_k} \right) \frac{\partial k}{\partial x_j} \right] + G_k + G_b - \rho \epsilon - Y_M + S_k, \quad (11)$$

$$\frac{\partial}{\partial t}(\rho \epsilon) + \frac{\partial}{\partial x_j}(\rho \epsilon u_j) = \frac{\partial}{\partial x_j} \left[\left(\mu + \frac{\mu_t}{\sigma_\epsilon} \right) \frac{\partial \epsilon}{\partial x_j} \right] + \rho C_1 S_\epsilon - \rho C_2 \frac{\epsilon^2}{k + \sqrt{\nu \epsilon}} + C_{1\epsilon} \frac{\epsilon}{k} C_{3\epsilon} G_b + S_\epsilon. \quad (12)$$

The eddy viscosity can be solved as follows [62]:

$$\mu_t = \rho C_\mu \frac{k^2}{\epsilon}. \quad (13)$$

The model constants in k-epsilon model can be solved as follows [62]:

$$C_{1\epsilon} = 1.44, \quad C_2 = 1.9, \quad \sigma_k = 1.0, \quad \sigma_\epsilon = 1.2. \quad (14)$$

Two layer model depending on the enhanced wall treatment can be defined as follows [62]:

$$\text{Re}_y \equiv \frac{\rho y \sqrt{k}}{\mu}, \quad (15)$$

$$y \equiv \min \left(\frac{\vec{r}}{\vec{r}_w \epsilon \Gamma_w}, \frac{\vec{r}}{\vec{r}_w} \right), \quad (16)$$

$$\mu_{t,2\text{layer}} = \rho C_m l_m \sqrt{k}, \quad (17)$$

$$l_m = y C_l^* (1 - e^{-\text{Re}_y / A_\mu}), \quad (18)$$

$$\mu_{t,\text{enh}} = \lambda_\epsilon \mu_t (1 - \lambda_\epsilon) \mu_{t,2\text{layer}}. \quad (19)$$

Enhanced wall functions can be determined as follows [62]:

$$u^+ = e^{\Gamma} u_{\text{lam}}^+ + e^{\frac{1}{\Gamma}} u_{\text{turb}}^+, \quad (20)$$

$$\Gamma = -\frac{0.01(y^+)^4}{1 + 5y^+}, \quad (21)$$

$$\frac{du^+}{dy^+} = e^{\Gamma} \frac{du_{\text{lam}}^+}{dy^+} + e^{\frac{1}{\Gamma}} \frac{du_{\text{turb}}^+}{dy^+}. \quad (22)$$

To calculate the heat transfer efficiency of NFs accurately, two-layer model depending on the improved wall treatment was applied. Thus, it was aimed to obtain high precision results in CFD analyses.

4 Statistical analysis

Statistical methods such as Taguchi method and variance analysis were considered to evaluate the impact of decisive factor for various levels on the heat transfer efficiency of the NFs. Nine CFD analyses were performed using different levels of decisive factors such as NP, VF, and Re number. The combination of NP, VF, and Re number according to different levels was determined in accordance with Taguchi L9 orthogonal array with three levels. Decisive factors and different levels are presented in Table 3.

As described in Table 3, the levels of NPs are determined as Gr, Al_2O_3 , and Cu, respectively. VFs of NPs were chosen as 0.5, 1.0, and 1.5%. To decide the effect of the Re number, three different values were selected and considered as 6,000, 7,000, and 8,000, respectively. Signal-to-noise (S/N) ratio analysis was utilized to explain the influence of each decisive factor on the heat transfer efficiency depending on different levels. The results obtained from the CFD data in this analysis were adapted to S/N ratios. Two different characteristics such as “the Larger is Better” and “the Smaller is Better” were utilized in the calculation of S/N ratios. Thus, it was aimed to obtain the highest h , number of transfer units (NTU), and T_w values and the lowest f values for NFs. For the maximum h , NTU, and T_w values, “the Larger is Better” characteristic was assumed and, “the Smaller is Better” characteristic was considered for the minimum f value. “The Larger is Better” and “the Smaller is Better” characteristics are explained in Eqs. (23) and (24), respectively [63]:

Table 3: Decisive factors at different levels

| Decisive factors | Symbol | Level 1 | Level 2 | Level 3 |
|------------------|--------|---------|-------------------------|---------|
| Material | M | Gr | Al_2O_3 | Cu |
| Volume fraction | VF | 0.5% | 1.0% | 1.5% |
| Re number | Re | 6,000 | 7,000 | 8,000 |

$$(S/N)_{LB} \text{ for } h, NTU, \tau_w = -10 \cdot \log \left(n^{-1} \sum_{i=1}^n (y_i^2)^{-1} \right), \quad (23)$$

$$(S/N)_{SB} \text{ for } f = -10 \cdot \log \left(n^{-1} \sum_{i=1}^n (y_i)^2 \right). \quad (24)$$

Minitab R15 program was used for statistical calculation of each characteristic and creation of graphs depending on S/N ratios.

5 Heat transfer efficiency calculation

In mathematical analyses, h , NTU , τ_w , and f were chosen as the heat transfer efficiency of NFs. The NFs were passed through a tube exposed to heat flux. The heat flux was kept constant but the levels of NP type, VF, and Re number were changed in each analysis. Thus, h , NTU , τ_w , and f values were calculated under constant heat flux.

h for tube can be defined as follows [64]:

$$h = \frac{\dot{Q}}{A_{sr}(T_s - T_{f,ave})}. \quad (25)$$

\dot{Q} obtained by using working fluid in tube may be evaluated as follows [64]:

$$\dot{Q} = \dot{m}c_p(T_e - T_i), \quad (26)$$

\dot{m} for working fluid may be defined as follows [64]:

$$\dot{m} = \rho v A_c. \quad (27)$$

NTU for tube can be calculated as follows [64]:

$$NTU = \frac{hA_{sr}}{\dot{m}c_p}. \quad (28)$$

τ_w for tube can be solved as follows [61]:

$$\tau_w = \frac{f\rho v^2}{8}. \quad (29)$$

Re number can be defined as follows [64]:

$$Re = \frac{\rho v D}{\mu}. \quad (30)$$

6 Results and discussion

The main goal of the research is to observe the impact of NP, VF, and Re number on the heat transfer efficiency of NFs numerically, statistically, and theoretically. Numerical

analyses for the heat transfer efficiency were carried out with CFD approach and the numerical data are listed in Table 4.

As can be understood from Table 4, the average values obtained for h , NTU , τ_w , and f depending on the L9 orthogonal array are 2266.9 W/m²K, 0.3146, 0.8430 Pa, and 0.0343, respectively. The S/N ratios of the CFD results in Table 4 are tabulated in Table 5.

S/N ratios for h , NTU , and τ_w were calculated according to “Larger is Better” quality characteristic and for f was solved in accordance with “Smaller is Better” quality characteristic.

6.1 Selection of optimum levels

In this study, it was aimed to obtain maximum h , NTU , and τ_w and minimum f values. The optimum levels of NP, VF, and Re number on the heat transfer efficiency of NFs were calculated utilizing average S/N ratios and CFD data corresponding to each level of each decisive factor. Overall S/N ratios and CFD results are stated in Tables 6 and 7, respectively.

As described from response table for h and NTU , the optimum h were considered as the first level for NP and the third levels for VF and Re number. For NTU , it was calculated as the third levels of NP and VF and the first level of Re number.

From response table for τ_w and f , the optimum τ_w were obtained using the first level of NP, the third level of VF, and the third level of Re number. It was determined that the third level of the Re number and all levels of NP and VF can be used to calculate the optimum f value. Main effect plots were drawn using average S/N ratios in Tables 6 and 7

Table 4: CFD data depending on L9 orthogonal array

| Test | Decisive factors | | | CFD data | | | |
|---------------------|--------------------------------|------|-------|-----------------------------------|-------------|-----------------|-----------|
| | M | VF | Re | h , (W/ m ² K) | NTU , (-) | τ_w , (Pa) | f , (-) |
| 1 | Gr | 0.5% | 6,000 | 1994.3 | 0.3158 | 0.6474 | 0.0359 |
| 2 | Gr | 1.0% | 7,000 | 2289.7 | 0.3097 | 0.8567 | 0.0342 |
| 3 | Gr | 1.5% | 8,000 | 2586.4 | 0.3049 | 1.0966 | 0.0329 |
| 4 | Al ₂ O ₃ | 0.5% | 7,000 | 2260.0 | 0.3085 | 0.8341 | 0.0342 |
| 5 | Al ₂ O ₃ | 1.0% | 8,000 | 2546.6 | 0.3047 | 1.0598 | 0.0329 |
| 6 | Al ₂ O ₃ | 1.5% | 6,000 | 2021.4 | 0.3230 | 0.6583 | 0.0359 |
| 7 | Cu | 0.5% | 8,000 | 2502.0 | 0.3065 | 1.0209 | 0.0329 |
| 8 | Cu | 1.0% | 6,000 | 1967.9 | 0.3298 | 0.6188 | 0.0359 |
| 9 | Cu | 1.5% | 7,000 | 2233.7 | 0.3288 | 0.7945 | 0.0342 |
| Overall mean values | | | | 2266.9 | 0.3146 | 0.8430 | 0.0343 |

Table 5: S/N ratios for heat transfer efficiency

| Test | Decisive factors | | | S/N ratios (η), dB | | | |
|------|--------------------------------|------|-------|---------------------------|----------------|---------------------|----------------|
| | M | VF | Re | η for h | η for NTU | η for τ_w | η for f |
| 1 | Gr | 0.5% | 6,000 | 65.9958 | -10.0110 | -3.7765 | 28.9092 |
| 2 | Gr | 1.0% | 7,000 | 67.1956 | -10.1823 | -1.3439 | 29.3215 |
| 3 | Gr | 1.5% | 8,000 | 68.2539 | -10.3167 | 0.8010 | 29.6646 |
| 4 | Al ₂ O ₃ | 0.5% | 7,000 | 67.0822 | -10.2148 | -1.5754 | 29.3214 |
| 5 | Al ₂ O ₃ | 1.0% | 8,000 | 68.1192 | -10.3222 | 0.5045 | 29.6647 |
| 6 | Al ₂ O ₃ | 1.5% | 6,000 | 66.1130 | -9.8163 | -3.6314 | 28.9092 |
| 7 | Cu | 0.5% | 8,000 | 67.9657 | -10.2712 | 0.1797 | 29.6642 |
| 8 | Cu | 1.0% | 6,000 | 65.8801 | -9.6340 | -4.1697 | 28.9089 |
| 9 | Cu | 1.5% | 7,000 | 66.9805 | -9.6607 | -1.9981 | 29.3211 |

Table 6: Response table for h and NTU

| Level | h (W/m ² K) | | | | | | NTU (-) | | | | | |
|-------|--------------------------|-------|-------|-------------|------|------|------------|---------|---------|-------------|--------|--------|
| | S/N ratios | | | Mean values | | | S/N ratios | | | Mean values | | |
| | M | VF | Re | M | VF | Re | M | VF | Re | M | VF | Re |
| 1 | 67.15 | 67.01 | 66.00 | 2290 | 2252 | 1995 | -10.170 | -10.166 | -9.820 | 0.3101 | 0.3103 | 0.3229 |
| 2 | 67.10 | 67.06 | 67.09 | 2276 | 2268 | 2261 | -10.118 | -10.046 | -10.019 | 0.3121 | 0.3147 | 0.3157 |
| 3 | 66.94 | 67.12 | 68.11 | 2235 | 2281 | 2545 | -9.855 | -9.931 | -10.303 | 0.3217 | 0.3189 | 0.3054 |
| Delta | 0.21 | 0.10 | 2.12 | 56 | 28 | 550 | 0.315 | 0.234 | 0.483 | 0.0116 | 0.0086 | 0.0175 |
| Rank | 2 | 3 | 1 | 2 | 3 | 1 | 2 | 3 | 1 | 2 | 3 | 1 |

to define the influence of each decisive factor on the h , NTU, τ_w , and f depending on the different levels. Main effect plots for h and NTU are presented in Figures 1 and 2.

Figure 1 shows that the most influential NPs on h were identified as Gr, Al₂O₃, and Cu, respectively. Increase in the VF of NPs from 0.5 to 1.5% causes an increase in h . This finding was identified by a study by Garud and Lee [65]. In addition, increasing the Re number from 6,000 to 8,000 provides an increase in h . This finding is supported by a previous study [65] and it is stated that increasing Re number also increases h value. As seen in Figure 2, the

most effective NPs on NTU were evaluated as Cu, Al₂O₃, Gr, respectively. An increase in the VF values of NPs from 0.5 to 1.5% causes an increase in NTU, whereas the increase in Re number from 6,000 to 8,000 causes a decrease for NTU. Main effect plots for τ_w and f are displayed in Figures 3 and 4.

As described from Figure 3, the most dominant NPs on τ_w were determined as Gr, Al₂O₃, and Cu, respectively. Increase in the VF of NPs from 0.5 to 1.5% and Re number from 6,000 to 8,000 causes an increase in τ_w . As explained from Figure 4, it was found that NP and VFs did not have

Table 7: Response table for τ_w and f

| Level | τ_w (Pa) | | | | | | f (-) | | | | | |
|-------|---------------|--------|--------|-------------|--------|--------|------------|------|-------|-------------|--------|--------|
| | S/N ratios | | | Mean values | | | S/N ratios | | | Mean values | | |
| | M | VF | Re | M | VF | Re | M | VF | Re | M | VF | Re |
| 1 | -1.440 | -1.724 | -3.859 | 0.8669 | 0.8341 | 0.6415 | 29.3 | 29.3 | 28.91 | 0.0343 | 0.0343 | 0.0359 |
| 2 | -1.567 | -1.670 | -1.639 | 0.8507 | 0.8451 | 0.8284 | 29.3 | 29.3 | 29.32 | 0.0343 | 0.0343 | 0.0342 |
| 3 | -1.996 | -1.610 | 0.495 | 0.8114 | 0.8498 | 1.0591 | 29.3 | 29.3 | 29.66 | 0.0343 | 0.0343 | 0.0329 |
| Delta | 0.556 | 0.115 | 4.354 | 0.0555 | 0.0157 | 0.4176 | 0 | 0 | 0.76 | 0 | 0 | 0.0030 |
| Rank | 2 | 3 | 1 | 2 | 3 | 1 | 2.5 | 2.5 | 1 | 2.5 | 2.5 | 1 |

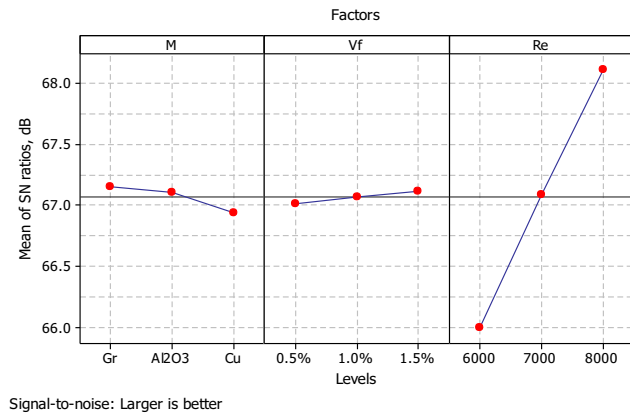


Figure 1: Effects of M, VF, and Re on h .

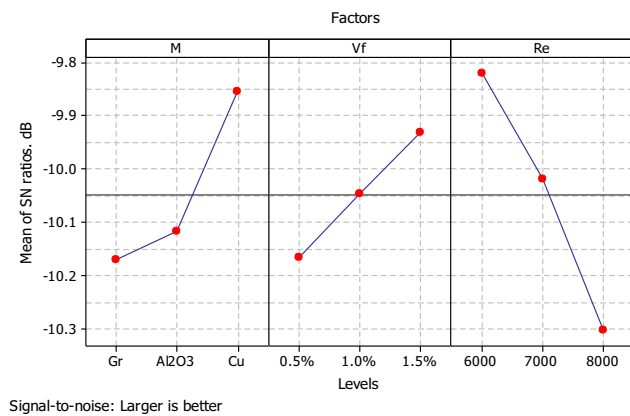


Figure 2: Effects of M, VF, and Re on NTU.

any effect on f . This finding can be explained by Eq. (35). According to the Colebrook equation [64], f depends on the relative roughness and Re number. However, increasing the Re number from 6,000 to 8,000 provides a decrease in the f value. A finding is supported by a study and it is

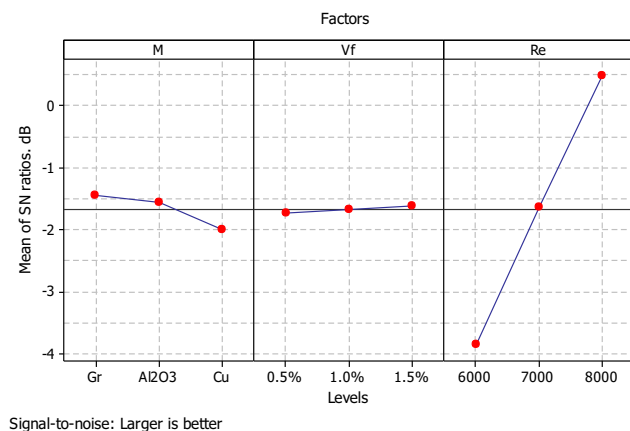


Figure 3: Effects of M, VF, and Re on τ_w .

stated that an increase in the Re number from 6,000 to 8,000 decreases the f value [65].

6.2 Analysis of variance

ANOVA was implemented according to general approach at 95% confidence interval to decide the percentage contributions and importance levels of NP, VF, and Re number on the h , NTU, τ_w , and f . ANOVA data depending on h and NTU are presented in Table 8.

According to the F test results for 95% confidence interval in ANOVA, although Re number on h and NTU were determined as significant decisive factors, NP and VF were determined as insignificant parameters. The most effective decisive factors on h were obtained as Re number with 98.58% impact, NP with 1.09% impact, and VF with 0.26% impact, respectively. For NTU, the most powerful decisive factors were decided as Re number with 56.30% impact, NP with 28.04% impact, and VF with 13.54% impact, respectively. ANOVA data for τ_w and f are given in Table 9.

According to ANOVA data for τ_w and f , although the most significant decisive factor on τ_w was selected as Re number due to 95% confidence level, NP and VF were determined as insignificant decisive factors. The most dominant decisive factors on τ_w were obtained as Re number with 97.88% impact, NP with 1.82% impact, and VF with 0.14% impact, respectively.

7 Statistical validation

The average values obtained from the CFD results corresponding to each level of each decisive factor were used to

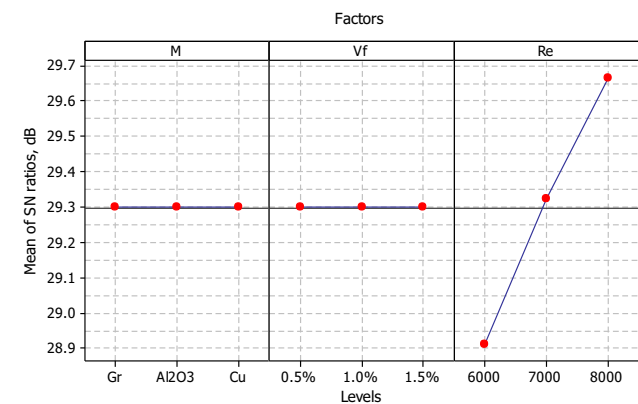


Figure 4: Effects of M, VF, and Re on f .

Table 8: ANOVA results for h and NTU

| Source | h | | | | | | NTU | | | | | |
|--------------------------------------|-----|---------|---------|---------|-------|----------|--------------------------------------|---------|-------|-------|----------|--|
| | DF | Seq SS | Adj MS | F | P | % Impact | Seq SS | Adj MS | F | P | % Impact | |
| M | 2 | 5,011 | 2,505 | 14.74 | 0.064 | 1.09 | 0.000231 | 0.00012 | 13.15 | 0.071 | 28.04 | |
| VF | 2 | 1,216 | 608 | 3.58 | 0.218 | 0.26 | 0.000112 | 0.00006 | 6.35 | 0.136 | 13.54 | |
| Re | 2 | 454,669 | 227,335 | 1337.36 | 0.001 | 98.58 | 0.000465 | 0.00023 | 26.4 | 0.036 | 56.30 | |
| Error | 2 | 340 | 170 | | | 0.07 | 0.000018 | 0.00001 | | | 2.13 | |
| Total | 8 | 461,236 | | | | 100 | 0.000825 | | | | 100 | |
| R-Sq = 99.93% and R-Sq(adj) = 99.71% | | | | | | | R-Sq = 97.87% and R-Sq(adj) = 91.47% | | | | | |

Table 9: ANOVA results for τ_w and f

| Source | τ_w | | | | | | f | | | | | |
|--------------------------------------|----------|----------|----------|--------|-------|----------|--|-----------|-----|-----|----------|--|
| | DF | Seq SS | Adj MS | F | P | % Impact | Seq SS | Adj MS | F | P | % Impact | |
| M | 2 | 0.00489 | 0.002445 | 12.11 | 0.076 | 1.82 | 0 | 0 | ** | ** | 0 | |
| VF | 2 | 0.000387 | 0.000194 | 0.96 | 0.511 | 0.14 | 0 | 0 | ** | ** | 0 | |
| Re | 2 | 0.262558 | 0.131279 | 650.23 | 0.002 | 97.88 | 0.0000134 | 0.0000067 | ** | ** | 100 | |
| Error | 2 | 0.000404 | 0.000202 | | | 0.15 | 0 | 0 | | | 0 | |
| Total | 8 | 0.268239 | | | | 100 | 0.0000134 | | | | 100 | |
| R-Sq = 99.85% and R-Sq(adj) = 99.40% | | | | | | | R-Sq = 100.00% and R-Sq(adj) = 100.00% | | | | | |

perform statistical verification of the heat transfer efficiency. These values are given in Tables 6 and 7. The optimum values of h , NTU, and τ_w was calculated by employing the optimum levels of important decisive factors. The estimated mean of h , NTU, and τ_w can be evaluated as follows [63]:

$$\bar{\mu}_{\text{HTE}} = \bar{M}_i + \bar{VF}_i + \bar{Re}_i - 2\bar{T}_{\text{OM}}. \quad (31)$$

\bar{T}_{OM} represents the overall mean of nine CFD analyses based on the L9 orthogonal array. \bar{T}_{OM} for h , NTU, τ_w , and f were calculated as 2266.9 W/m²K, 0.3146, 0.8430 Pa, and

0.0343, respectively. \bar{M}_i denotes the overall data of heat transfer efficiency at the optimum level of NPs. \bar{M}_i for h , NTU, τ_w , and f were found as 2,290, 0.3217, 0.8669, and 0.0343, respectively. \bar{VF}_i expresses the overall data of heat transfer efficiency at the optimum level of VF. \bar{VF}_i for h , NTU, τ_w , and f were evaluated as 2,281, 0.3189, 0.8498, and 0.0343, respectively. \bar{Re}_i means the overall data of heat transfer efficiency depending on the optimum level of Re number. \bar{Re}_i for h , NTU, τ_w , and f were evaluated as 2,545, 0.3229, 1.0591, and 0.0329, respectively. Substituting the data of different terms in Eq. (31), estimated heat transfer

Table 10: Comparison of CFD and predict Taguchi data

| Results | h for $M_1VF_3Re_3$ | NTU for $M_3VF_3Re_1$ | τ_w for $M_1VF_3Re_3$ | f for $M_{\text{all}}VF_{\text{all}}Re_3$ |
|----------------|---------------------------|-----------------------|----------------------------|---|
| CFD result | 2586.4 W/m ² K | 0.3377 | 1.0966 Pa | 0.0329 |
| Taguchi result | 2582.2 W/m ² K | 0.3343 | 1.0898 Pa | 0.0329 |
| Difference | 0.2% | 1% | 0.6% | 0% |

Table 11: Comparison of CFD and theoretical results

| Results | h for $M_1VF_3Re_3$ | NTU for $M_3VF_3Re_1$ | τ_w for $M_1VF_3Re_3$ | f for $M_{\text{all}}VF_{\text{all}}Re_3$ |
|--------------------|---------------------------|-----------------------|----------------------------|---|
| CFD result | 2586.4 W/m ² K | 0.3377 | 1.0966 Pa | 0.0329 |
| Theoretical result | 2568.1 W/m ² K | 0.3381 | 1.0943 Pa | 0.0328 |
| % Difference | 0.7% | 0.1% | 0.2% | 0.3% |

efficiency was obtained. The comparison of the CFD and predict Taguchi results obtained is presented in Table 10.

Table 10 displays that the differences for h , NTU, τ_w , and f are 0.2, 1, 0.6, and 0%, respectively. This finding shows that the low difference between the results increases the accuracy of the analysis.

8 Theoretical validation

Theoretical approach was utilized to define the accuracy of CFD results. Heat transfer efficiency of NFs such as h , NTU, τ_w , and f were calculated theoretically. Eqs. (32)–(35) were used to calculate h , NTU, and f , whereas Eq. (29) was utilized for τ_w .

Nu number depending on the Pr number and heat flux can be described as follows [64]:

$$\overline{Nu}_D = 0.023Re^{0.8}Pr^{0.4}. \quad (32)$$

Pr number can be solved as follows [64]:

$$Pr = \frac{\mu C_p}{k}. \quad (33)$$

h obtained by considering the Nu number can be explained as follows [64]:

$$h = \frac{k\overline{Nu}_D}{D}, \quad (34)$$

f can be calculated as follows [64]:

$$\frac{1}{\sqrt{f}} = -2 \log \left(\frac{e/D_{Tube}}{3.7} + \frac{2.51}{Re\sqrt{f}} \right). \quad (35)$$

The results calculated with the theoretical approach are compared with the results obtained depending on CFD analysis and are presented in Table 11.

Table 11 shows that the differences for h , NTU, τ_w , and f are 0.7, 0.1, 0.2, and 0.3%, respectively. Thus, it was determined that the CFD analysis was performed with high accuracy.

9 Conclusion

In this numerical, theoretical, and statistical research, the impact of NP type, VF, and Re number in the heat transfer efficiency of NFs were analyzed. Heat transfer coefficient, NTU, wall shear stress, and friction factor were considered as the heat transfer efficiency of NFs. ANSYS Fluent software was employed to perform computational fluid dynamics analyses. The test sequences of the analyses were designed

according to the Taguchi method and the L9 orthogonal array was utilized. NP type, VF, and Re number were considered as decisive factors. S/N ratio analysis was applied to determine the optimal levels of decisive factors on the heat transfer efficiency of NFs. Significance levels and contribution rates of the decisive factors on the heat transfer efficiency were evaluated utilizing Analysis of Variance. The important findings obtained from the numerical, statistical, and theoretical study are summarized. The most effective NPs on h and τ_w were identified as Gr, Al_2O_3 , and Cu, respectively. For NTU, the most effective NPs are found to be Cu, Al_2O_3 , Gr, respectively. However, no effect of NPs on f could be detected. The increasing Re number from 6,000 to 8,000 causes an increase in h and τ_w and a decrease in NTU and f . The increasing volume fractions of NPs from 0.5 to 1.5% causes an increase in h , NTU, and τ_w , but no effect was observed on f . The optimum h and τ_w data were obtained using 1.5%Gr NFs, and Re number of 8,000. However, the optimum NTU was achieved utilizing 1.5%Cu NFs and Re number of 6,000. According to ANOVA, Re number on h , NTU, and τ_w was detected as a significant decisive factor. The most effective decisive factors on h were achieved to be Re number with 98.58% impact, NP with 1.09% impact, and volume fraction with 0.26% impact, respectively. The most powerful decisive factors for NTU were obtained as Re number with 56.30% impact, NP with 28.04% impact, and volume fraction with 13.54% impact, respectively. The most dominant decisive factors on τ_w were considered as Re number with 97.88% impact, NP with 1.82% impact, and volume fraction with 0.14% impact, respectively. The differences for h , NTU, τ_w , and f were found to be 0.2, 1, 0.6, and 0% in statistical verification, whereas these differences were detected as 0.7, 0.1, 0.2, and 0.3% in theoretical verification.

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