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#### Research Article

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# Cross electromagnetic nanofluid flow examination with infinite shear rate viscosity and melting heat through Skan-Falkner wedge

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**Abstract:** This demonstration of study focalizes the melting transport and inclined magnetizing effect of cross fluid with infinite shear rate viscosity along the Skan-Falkner wedge. Transport of energy analysis is brought through the melting process and velocity distribution is numerically achieved under the influence of the inclined magnetic dipole effect. Moreover, this study brings out the numerical effect of the process of thermophoresis diffusion and Brownian motion. The infinite shear rate of viscosity model of cross fluid reveals the set of partial differential equations (PDEs). Similarity transformation of variables converts the PDEs system into nonlinear ordinary differential equations (ODEs). Furthermore, a numerical byp4c process is imposed on these resultant ODEs for the pursuit of a numerical solution. From the debate, it is

concluded that melting process cases boost the velocity of fluid and velocity ratio parameter. The augmentation of the minimum value of energy needed to activate or energize the molecules or atoms to activate the chemical reaction boosts the concentricity.

**Keywords:** inclined magnetized flow, infinite shear rate viscosity, Brownian motion, 2-D cross fluid, melting process of energy, thermophoresis diffusion

positive constants

#### **Nomenclature**

a, b, c, m

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notation of unsteadiness parameter  $\boldsymbol{A}$  $A_1$ first Rivlin (Erickson tensor) notation of skin friction  $C_f$ notation of specific heat of fluid  $c_p$ С concentration profile Ι notation of identity tensor k cross nanofluid thermal conductivity M notation of melting parameter notation of power law index region n notation of Nusselt number Nu exertion of pressure р Pr notation of Prandtl number notation of wall shear stress  $q_{\rm w}$ Re notation of Reynold number  $k_c$ chemical reaction parameter velocity ratio parameter S Sc notation of Schmidt number t time involved in stream function T temperature profile  $T_0$ initial temperature  $T_{\infty}$ ambient temperature of fluid temperature during melting process  $T_m$  $U_e(x, t)$ free stream velocity  $U_{w}(x,t)$ stretching velocity

u, v	velocity components
V	velocity profile
We	Weissenberg number
<i>x</i> , <i>y</i>	space coordinates
β	wedge angle parameter
τ	Cauchy stress tensor
$\mu_0$	zero viscosity in shear rate model
$\mu_{\infty}$	infinite viscosity shear rate model
Γ	notation of relaxation time constant
$\psi(x, y, t)$	Stokes stream function
μ	notation of viscosity
$ au_{rx}$	heat flux
ý	shear strain of shear rate model
η	involved in stream function dimensionless
	variable
$\sigma$	reaction rate parameter
ρ	density
$\theta_w$	temperature ratio parameter
$\alpha_m$	notation of thermal diffusivity

#### 1 Introduction

Nanotechnology is defined as the use of nanoparticles for human benefit. Nanomaterials have special properties due to their physical and chemical properties at the nanoscale. Nanotechnology has a wide range of applications and has been used to design new technologies in the manufacturing, electrical, and energy sectors. The modification of matter with at least one dimension sized between 1 and 100 nm is characterized as nanomaterials. Nanofluid and nanoscale surface morphology are two commonly utilized nanotechnologies for boiling heat transfer. The basic

process is that nano-products can alter the thermal properties of the heating surface or the base fluid, resulting in improved boiling heat transmission ability. Nanoscale coating primarily affects the wickability, wettability, and porosity of surfaces. The capillary action, which absorbs fresh liquid to dry out patches, can be delayed by modifying the surface wickability. Nanoscience gave a new dimension to heating transfer fluid. Thermal science is facing the consumption of energy, and to overcome this issue, industrial areas needed to increase the thermal conductivity of the base fluid. Nanoscience gave the way to increase the thermal conductivity of heat transfer fluid, and thus, nanoscience has been extensively engaged in industrial and engineering areas because low thermal conductivity was the main problematic issue for engineering framework. Nanoscience introduced nano liquids which are very imperative to increase thermal conductivity. Many scholars [1-4] made their studies related to fluidic models by considering several nanoparticles with base fluid. Investigation of nanoparticles of Maxwell fluid model by taking several nanoparticles distributed over the surface is discussed in detail by Asjad et al. [5]. The purpose of enhancement of thermal conductivity with cross nanofluid over wedge geometry is explained by Waqas et al. Blood behavior as a cross fluid is achieved numerically taken into consideration the influence of nanoparticles by ref. [6].

The minimum amount of energy required for the possible process of emission or reaction is called activation energy. It activates the chemical process. In engineering point of view, it has a magnificent and vital role like its usage in geothermal reservoirs, emulsion of oil, food processing, water mechanisms, *etc.* several scholars [7,8] made their efforts related to the investigation to judge the concentration of flow with activation energy. The effect of activation energy on the concentration profile

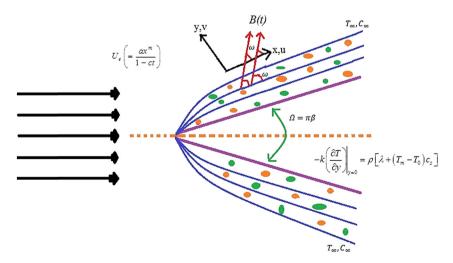


Figure 1: Geometry related to the physical flow of cross nanofluid.

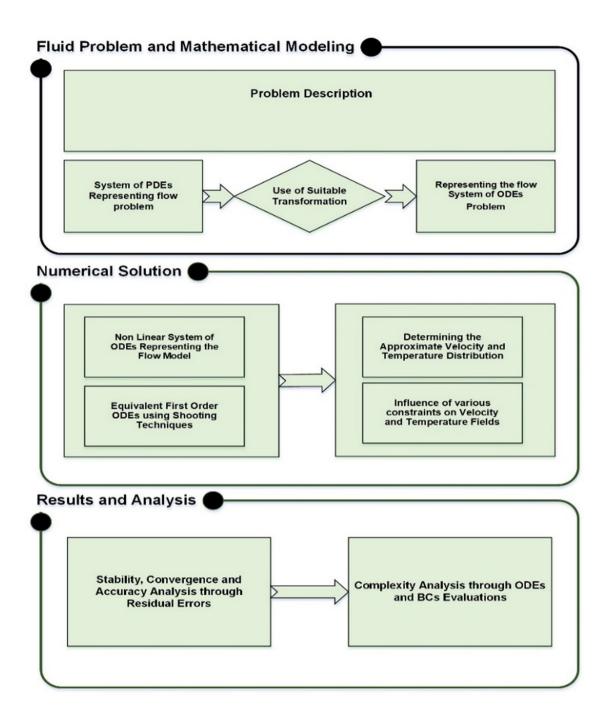


Figure 2: Description of the study.

with cross fluid over the stretching sheet is discussed by Shah et al. [9]. Mass transfer of nanoparticles of Carreau fluid with multiple features is revealed by Ayub et al. [10]. Activation role under magnetized flow, thermal radiation, buoyancy forces, etc., is countered by several investigators [11-14].

Pumping or mixing fluids in microdevices can be accomplished using an electromagnetic body force (a Lorentz force) created by the interplay of an applied

magneto force and an electrical currents that is typically provided outside. Magnetohydrodynamics (MHD) has long been the subject of considerable research due to its huge relevance in a variety of domains ranging from environmental phenomena such as geophysical and astrophysical to various technical applications such as plasma confinement, liquid metal, electromagnetic casting, and so on. Researchers in MHD natural convection completed a wide variety of research. To judge the

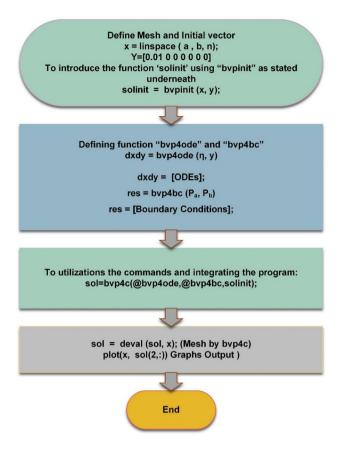


Figure 3: Description of bvp4c method.

key properties of fluid behavior under the influence of magnetic effect is called MHD flow. MHD keeps its vital application in many maladies that are dangerous to health, cancer tumor, and cure like healing wounds when bleeding is at its peak, and the most important key application is magneto resonance imaging which

0.9 0.8 M = 0.0M = 0.50.7 M = 1.00.6 0.5 0.4 0.3  $\omega = \pi/3$ 0.2 0 0.5 2 η (a)

Table 1: Verification table

β	Ali <i>et al</i> . [25]	Present study
0.0	0.469646	0.476461
0.3	0.476403	0.484032
0.6	0.997474	0.987435
1.2	1.335337	1.357343

presents an internal sketch of the brain [15-18]. The inclined magnetic effect of cross nanofluid with Brownian motion and the chemical process has been hashed out by Wahab et al. [19]. Khan et al. [20] investigated numerical solution of Carreau nanofluid keeping the orthogonal magnetic effect. The effect of perpendicular and inclined magnetic dipole combined with several effects like thermal radiation, heat sink source, and other numerous parameters are countered by different scholars [21–23] in detail.

The phenomenon of bringing the random particles into consideration and analysis of random motion is called Brownian motion. It achieves superb praise in the field of general science and the biological era of science. It is the result of continued collisions of molecules with the around medium. It has its influence in many areas of practical science like engineering and medicine [24–28]. The Brownian motion process of cross nanofluid with many features is discussed by Sabir et al. [29]. A micropolar fluid model with thermophoresis and Brownian motion under the influence of magnetic effect is revealed by ref. [30].

In this effort of investigation, our eye is on the melting process of energy under the influence of the inclined magnetic field of cross nanofluid over the geometry of wedge. The infinite shear rate viscosity model of

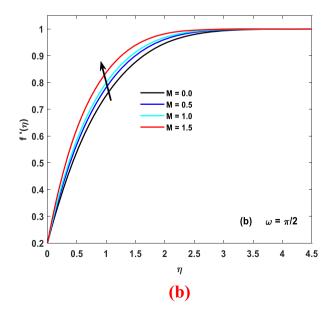
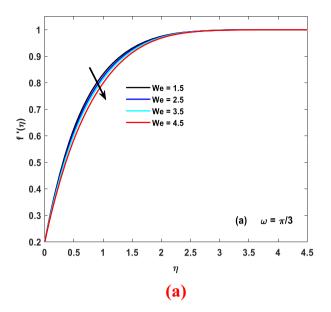


Figure 4: (a) and (b) Numerical consequences of M on the distribution of momentum of cross fluid.



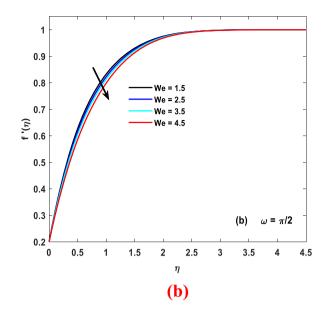


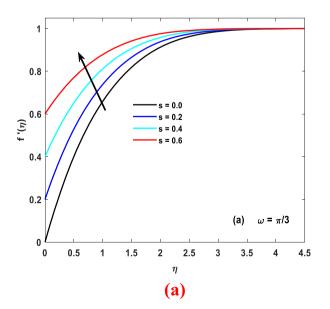
Figure 5: (a) and (b) Numerical consequences of We on the distribution of momentum of cross fluid.

the cross model is taken into consideration. A discussion of the mathematical formulation of the present article is presented in the next section.

### 2 Representation of mathematical formulation process

We assumed that there is a two-dimension (2D) fluid flowing over the Falkner-Skan wedge geometry. Characteristics of the assumed fluid flow are unsteadiness and incompressibility. There is assumed inclined magnetic field impact with infinite shear rate of viscosity model of cross fluid. The geometry look is seen in Figure 1.

When the wedge is stretching with velocity  $U_e\left(=\frac{ax^m}{1-ct}\right)$  (with ct < 1), then the fluid velocity becomes free  $U_w\left(=\frac{bx^m}{1-ct}\right)$  (with ct < 1) and it is called free stream velocity. a, b, and c involved in stretching and free stream velocity are positive constants and m is restricted by the interval [0,1]. Stretchiness and contraction of the



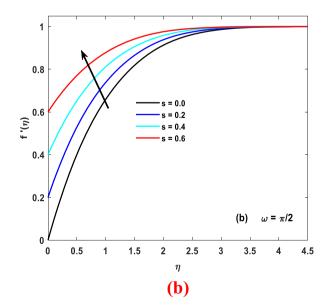
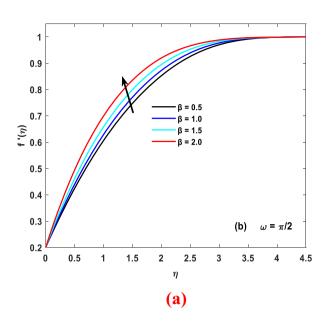
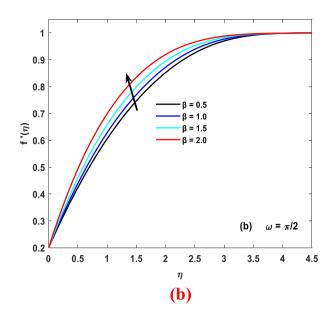


Figure 6: (a) and (b) Numerical consequences of s on the distribution of momentum of cross fluid.





**Figure 7:** (a) and (b) Numerical consequences of  $\beta$  on the distribution of momentum of cross fluid.

wedge are shown by the mathematical relation of  $U_w(x,t)>0$  and  $U_w(x,t)<0$ , respectively.  $\Omega=\beta\pi$  is the wedge angle. The mathematics of assumed flow is described through the following equations and modeling.

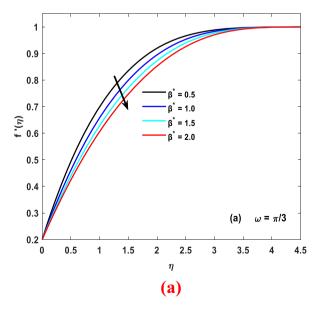
Velocity visibity = 
$$[u(x, y, t), v(x, y, t)] = V$$
,  
Tempreture visibity =  $T(x, y, t) = T$ ,  
Concentration visibity =  $C(x, y, t) = C$ .

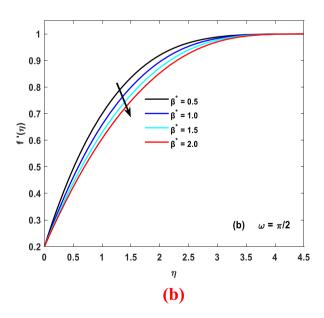
## 3 Governing equations and infinite shear rate viscosity model of cross fluid

Viscosity model of cross fluid in terms of infinite shear rate [31] is given as

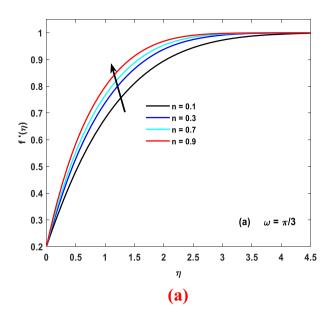
$$\mu(\dot{y}) - \mu_{\infty} - \mu_0 [1 + (\Gamma \dot{y})^n]^{-1} + [1 + (\Gamma \dot{y})^n]^{-1} \mu_{\infty} = 0, (2)$$

$$\mu(\dot{y}) - \mu_{\infty} \beta^* = [1 + (\Gamma \dot{y})^n]^{-1} - \beta^* [1 + (\Gamma \dot{y})^n]^{-1}.$$
 (3)





**Figure 8:** (a) and (b) Numerical consequences of  $\beta^*$  on the distribution of momentum of cross fluid.



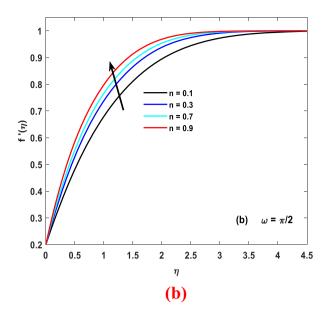


Figure 9: (a) and (b) Numerical consequences of n on the distribution of momentum of cross fluid.

Equations of motion, energy, and mass transport in the form of partial differential equations (PDEs) [32] are

$$\frac{\partial u}{\partial t} + u \left( \frac{\partial u}{\partial x} \right) + v \left( \frac{\partial u}{\partial y} \right) = \frac{\partial U_e}{\partial t} + U_e \frac{\partial U_e}{\partial x} 
+ v \left( \beta^* \left( \frac{\partial^2 u}{\partial y^2} \right) + \left( \frac{\partial^2 u}{\partial y^2} \right) [1 + (\Gamma \dot{Y})^n]^{-1} - \beta \right) 
+ v \left( \frac{\partial^2 u}{\partial y^2} \right) [1 + (\Gamma \dot{Y})^n]^{-1} \right)$$

$$- nv(1 - \beta^*) \Gamma^n \left( \frac{\partial^2 u}{\partial y^2} \right)^n \left[ \frac{1}{1 + (\Gamma u_y)^n} \right] \left( \frac{\partial u}{\partial y} \right)^n 
+ \frac{\sigma^* B^2(t)}{\rho} \sin^2(\omega) (U_e - u), 
[(\rho c)_f] \left[ \frac{\partial T}{\partial t} + u \left( \frac{\partial T}{\partial x} \right) + v \left( \frac{\partial T}{\partial x} \right) \right] 
= [(\rho c)_f] D_B \tau \left[ \frac{1}{D_B \tau \alpha^{-1}} \left( \frac{\partial^2 T}{\partial y^2} \right) + \left( \frac{\partial T}{\partial y} \frac{\partial C}{\partial y} \right) \right] 
+ \frac{1}{D_B \tau} \left[ \frac{T_{\infty}}{D_T} \right]^{-1} \left( \frac{\partial C}{\partial y} \right)^2 + \frac{Q_0}{D_B \tau} (T - T_m),$$

$$(5)$$

$$u \left( \frac{\partial C}{\partial x} \right) + v \left( \frac{\partial C}{\partial y} \right) = D_B \left( \frac{\partial^2 C}{\partial y^2} \right) - \frac{\partial C}{\partial t} + \frac{D_T}{T_{\infty}} \left( \frac{\partial^2 T}{\partial y^2} \right),$$

$$- kc^2 (C - C_{\infty}) \times (T_{\infty}^{-1} T)^m e^{\left( \frac{E_a}{kT} \right)}$$

$$U_e = \frac{ax^m}{1 - ct}, \beta^* = \frac{\mu_{\infty}}{\mu_0}, \delta = \left[ \frac{T_{\infty}}{T_m - T_{\infty}} \right]^{-1},$$

$$E = [K_{\infty} T_{\infty}]^{-1} Ea, \sigma = \left[ \frac{a}{kc^2} \right]^{-1},$$

$$u = sU_e, v = 0, T = T_m, C = C_m \text{ at } y = 0, u \to U_e, T \to T_\infty, C \to C_\infty \text{ as } y \to \infty.$$

$$(7)$$

With melting conditions [33]

$$\frac{k}{\rho}(T_y)\bigg|_{y=0} = -\lambda - (T_m - T_0)c_s; T_y = \frac{\partial T}{\partial y}.$$
 (8)

Using transformation

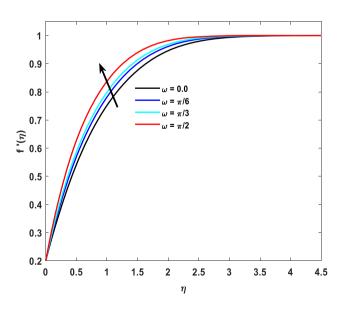


Figure 10: Numerical consequences of  $\omega$  on the distribution of momentum of cross fluid.

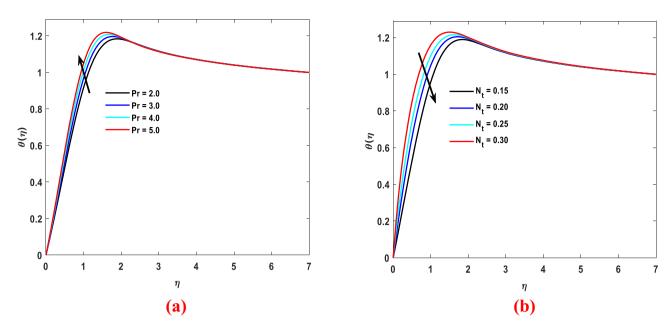


Figure 11: (a) and (b) Numerical consequences of the distribution of energy on varying the numerical values of Pr and Nt.

$$\zeta(x, y, t) = f(\eta) \sqrt{\frac{\lceil m + 1 \rceil^{-1}}{[2\nu x U_e]^{-1}}}, 
\theta(\eta) (T_{\infty} - T_m) = (T - T_m), 
\phi(\eta) \times (C_{\infty} - C_m) = (C - C_m), 
\text{with} \quad \eta \sqrt{2} = y \sqrt{\frac{U_e}{\nu \lceil m + 1 \rceil^{-1} x}}.$$
(9)

Obtained ordinary differential equations (ODEs) from the system of PDEs by using Eq. (9) in Eqs. (4–6)

$$\beta^* \lceil 1 + \lceil Wef'' \rceil^n \rceil^2 f''' - \left\{ A \left( f' + \frac{1}{2} \eta f'' - 1 \right) \lceil 1 + (Wef'')^n \rceil - ff'' \lceil 1 + (Wef'')^n \rceil \right\}$$

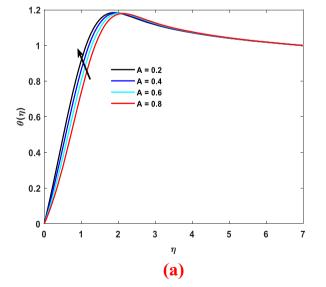
$$+ \beta (f'^2 - 1) (1 + (Wef'')^n)$$

$$+ (1 - (n - 1) (Wef'')^n) (1 - \beta^*) f'''$$

$$+ M^2 \sin^2(\omega) f' = 0,$$

$$(10)$$

$$\theta'' - Q\theta = -\Pr[N_b \phi' \theta' + f\theta' - A\eta \theta' + N_t(\theta')^2], \qquad (11)$$



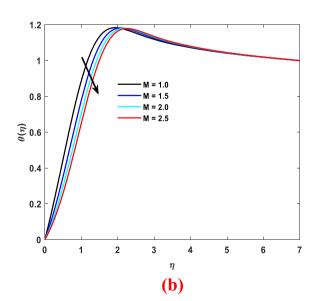
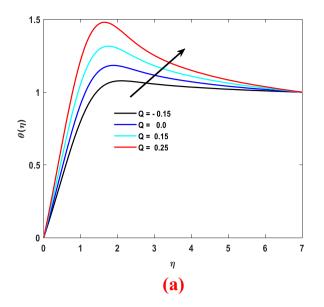


Figure 12: (a) and (b) Numerical consequences of the distribution of energy on varying the numerical values of A and M.



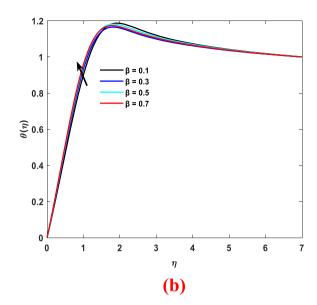


Figure 13: (a) and (b) Numerical consequences of the distribution of energy on varying the numerical values of Q and  $\beta$ .

$$\phi'' + \operatorname{Sc}\left[f \times \phi' - A\eta\phi' + \left(\frac{N_b}{N_t}\right)^{-1}\theta'' - \sigma(1 + \delta\theta)^m \phi e^{\left(-\frac{E}{1 + \delta\theta}\right)}\right] = 0,$$
(12)

subject to boundary conditions

$$N_b \phi' - N_t \theta' = 0, f' = s, \theta = 0, M\theta + \Pr f = 0, \text{ at}$$

$$\eta = 0,$$

$$f' \to 1, \theta \to 1, \phi \to 1 \quad \text{as} \quad \eta \to \infty,$$

$$(13)$$

Where

$$\begin{split} 2\nu \mathsf{W} \mathsf{e}^2 &= \tfrac{b^3(m+1)}{\nu^{-1}(\chi)^{-3m+1}}, \qquad \mathsf{Pr} &= \tfrac{\mu c_p}{k}, \, N_t = \tfrac{\tau D_T(T_m - T_\infty)}{\nu T_\infty}, \\ N_b &= \tfrac{\nu^{-1}}{[\tau D_B(C_W - C_\infty)]^{-1}}, \qquad M = [\lambda + (c_S T_m - c_S T_0)]^{-1} [c_p(T_\infty - T_m)], \\ \beta &= \tfrac{2m}{m+1}, \quad B^* &= \tfrac{\mu_\infty}{\mu_0}, \, A = \tfrac{c}{(m+1)ax^{m-1}}, \, Q = \tfrac{2Q_0(1-\mathsf{ct})}{\rho c_p(m+1)ax^{m-1}}, \quad \mathsf{Sc} = \tfrac{\nu}{D_B}. \end{split}$$

Mathematics of drag real-life quantities (force and rate of heat transfer)

$$\frac{\rho U_e^2 C_{fx}}{\tau_W \mid_{V=0}} = 1, \tag{14}$$

where  $C_{fx}$  is the dimensionless aspect defined as

$$\frac{\sqrt{2} \operatorname{Re}^{\frac{1}{2}} C_{fx}}{f''(0)\sqrt{(m+1)} [\beta^* + (1-\beta^*)]} = [1 + (\operatorname{We} f''(0))^n]^{-1},$$

and

$$\frac{\mathrm{Nu}_{\mathsf{X}}(T_{\infty}-T_{m})}{\mathsf{X}}=\left(\frac{\partial T}{\partial \mathsf{y}}\right)|_{\mathsf{y}=0}.\tag{15}$$

The dimensionless version of  $Nu_x$  is

$$\operatorname{Re}_{x}^{-\frac{1}{2}}\operatorname{Nu}_{x}\sqrt{\left(\frac{m+1}{2}\right)^{-1}}=-\theta'(0),$$
 (16)

where Re =  $\frac{xU_e}{v}$  is mathematical expression of local Reynolds number. Figure 2 defines the fluid problem and mathematical modeling of the current problem.

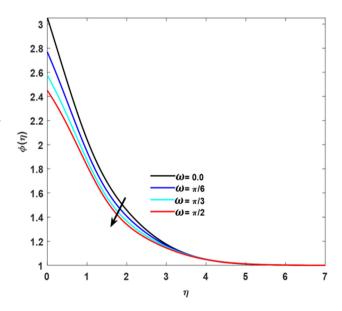
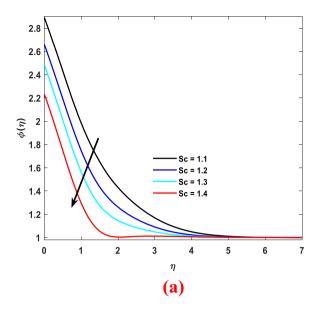


Figure 14: Numerical consequences of the distribution of energy on varying the numerical values of  $\omega$ .



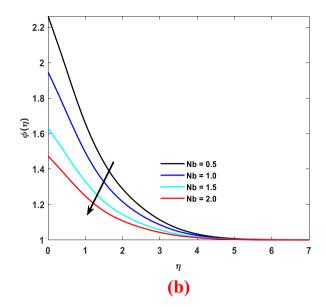


Figure 15: (a) and (b) Numerical consequences of concentration profile via Sc and Nb.

#### 4 Solution methodology

In this section, process of the numerical solution is presented. Bvp4c method [34–41] is applied to move the boundary value problem into the initial value problem. The complete procedure is given in Figure 3.

#### 5 Validation of work

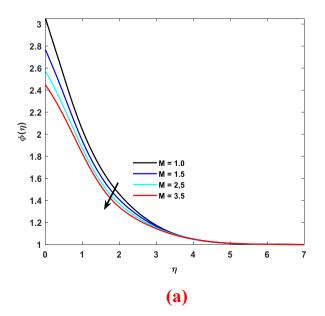
Table 1 shows the smooth agreement with old literature.

#### 6 Results and discussion

This Section presents the detailed consequences of several physical parameters on the distribution of velocity, temperature, and transport of mass.

#### **6.1** Velocity profile $f'(\eta)$

All major facts based on results concerning velocity are shown in Figures 4–10. Reports of M and We on velocity are shown in Figures 4(a) and (b) and 5(a) and (b). Behavior of



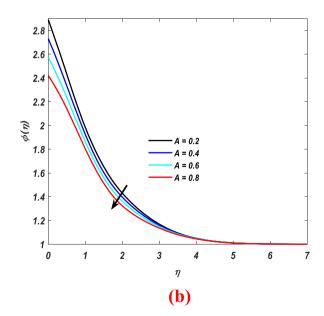


Figure 16: (a) and (b) Numerical consequences distribution of mass transport on varying the numerical values of M and A.

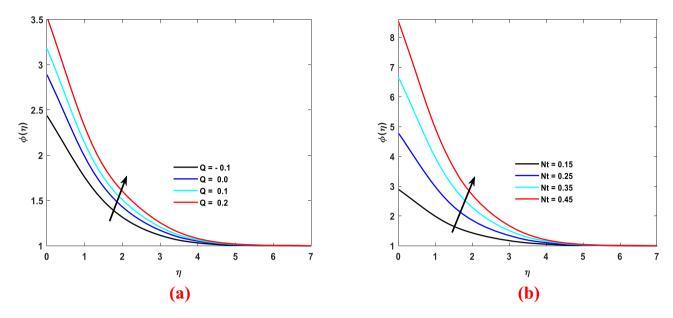


Figure 17: (a) and (b) Numerical consequences of the distribution of mass transport on varying the numerical values of Q and Nt.

nanoparticles seems depressed for the increase in We but boosts for ascending values of M. We shows relaxation time and M causes Lorentz force due to these factors, the velocity varies for M and We. An inclined angle is caused to create more Lorentz force, as the inclined angle is going orthogonal, due to the Lorentz force effect, velocity decreased. The influence of velocity ratios on the velocity is displayed in Figure 6(a) and (b). The symbol s is the velocity ratio, so greater numerical values of this parameter enhance the fluid viscosity which provides

a decrement in the fluid motion, and velocity decreases. Figures 7(a) and (b) and 8(a) and (b) disclose the influence of  $\beta$  and  $\beta^*$ , respectively. On increasing the values of  $\beta$  and  $\beta^*$ , velocity seems to be depressed due to the flow moving across the wedge. It is well established that the fluid velocity escalates due to an enhancement in wedge angle which amplifies velocity. The velocity of the fluid diminishes owing to magnification in  $\beta^*$ . It is noticed from Figure 9(a) and (b) that the velocity of fluid increases by improving the power law index n. The fluid behavior is

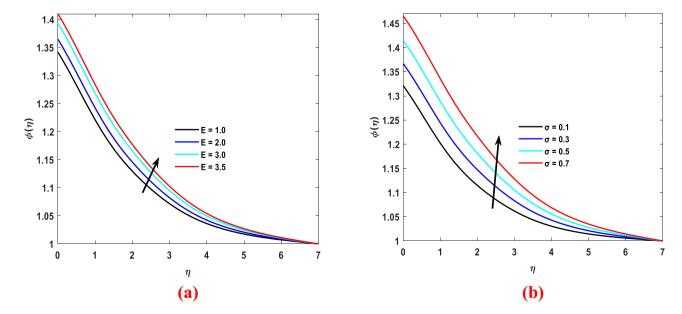
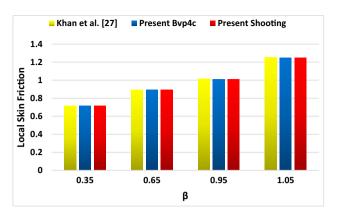


Figure 18: (a) and (b) Numerical consequences of distribution of mass transport on varying the numerical values of E and  $\sigma$ .



**Figure 19:** Numerical consequences of local skin friction coefficient with  $\beta$ .

shear thinning by the virtue of a magnification in n which diminishes the viscosity phenomenon and increases the velocity. From Figure 10 it is observed that the velocity of the fluid augments owing to magnification in wedge angle.

#### 6.2 Temperature profile $\theta(\eta)$

The results of scrutiny of  $\theta(\eta)$  distribution with the attached parameter are shown in Figures (11)–(14). Figure 11(a) and (b) reveals the effect of Prandtl and thermophoresis parameters. With the increase in Pr, the temperature profile increases, and it decreases due to a decrement in thermal conductivity of thermophoresis. Thermal diffusivity amplifies by the virtue of an amplification in Pr which amplifies the heat transfer rate and the temperature field. The molecules diffuse from the hotter surface toward the colder surface on behalf of an incremental change in

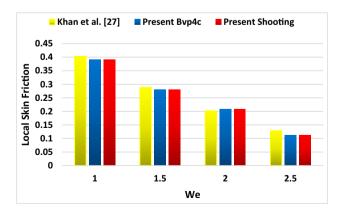


Figure 20: Numerical consequences of local skin friction coefficient with We.

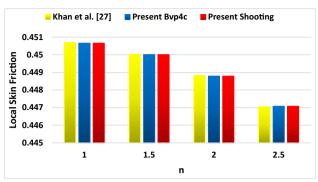
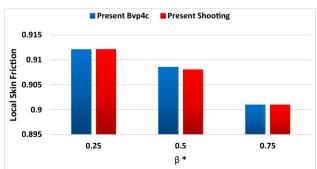


Figure 21: Numerical consequences of local skin friction coefficient with  $\boldsymbol{n}$ .

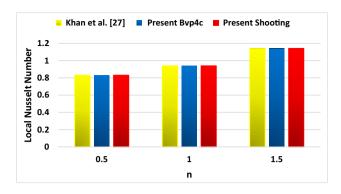
the thermophoresis parameter which diminishes the temperature inside the fluid.

Figure 12(a) and (b) launches the resultant effect of the unsteadiness parameter and melting parameter. The unsteadiness parameter boosts the temperature but the melting effect causes to lower the temperature field. It is well established that the viscosity of the fluid increases owing to an amplification in the unsteadiness parameter which amplifies the fluid viscosity. Viscosity is inversely related to temperature. That is why a positive change in the unsteadiness parameter depreciates fluid viscosity and escalates the temperature field. It is noted that a positive variation in melting parameter *M* diminishes the temperature field. The heat generation/absorption parameter has a direct relation with temperature and due to the generation of heat, temperature increases and the same result is achieved for wedge angle.

This fact is shown in Figure 13(a). More heat enters inside the fluid as a result of magnification in the heat generation parameter which amplifies the heat inside the fluid and temperature field as well. The passage of the fluid flow diminishes owing to an increment in wedge angle and molecules collide more randomly which



**Figure 22:** Numerical consequences of local skin friction coefficient with  $\beta^*$ .

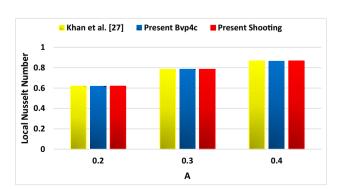


**Figure 23:** Numerical consequences of local Nusselt coefficient with n.

enhances the thermal conductivity of the fluid and temperature field as well, as shown in Figure 13(b). It is noticed from Figure 14 that the temperature, as well as heat transfer rate, diminishes when there is a positive change in an inclined angle.

#### 6.3 Concentration of nanoparticle $\phi(\eta)$

The results of scrutiny of  $\phi(\eta)$  distribution with the attached parameter are shown in Figures 15–18. Figure 15(a and b) reveals the effect of Schmidt number Sc and Brownian parameter Nb, as a result the profile of  $\phi(\eta)$  is seen depressed for both the mentioned parameters. Due to mass diffusivity and increment in the collusion between molecules, Schmidt diffusivity is inversely related to mass diffusivity. A positive variation in mass diffusivity diminishes the concentration profile which diminishes the concentration field. Molecules collide more randomly as a result of magnification in Nb which amplifies temperature and molecules from a region of lower concentration to the higher which



**Figure 24:** Numerical consequences of local Nusselt coefficient with  $\boldsymbol{A}$ .

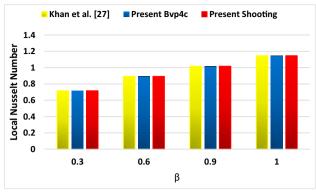


Figure 25: Numerical consequences of local skin Nusselt coefficient with  $\beta$ .

creates abatement in the concentration field. The melting process reduces the concentration and as a result temperature declines and also, the unsteadiness parameter is decreasing the temperature. Effects of M and A are shown in Figure 16(a) and (b). From Figure 17(a) and (b), it can be seen that the concentration profile *via Q* and Nt is increasing due to heat generation effect. It is noticed that the heat transfer rate amplifies due to the change in Q which amplifies the mass diffusion phenomenon and concentration of the fluid as well. The molecules diffuse from a region of lower concentration to a higher one as a result of a magnification in Nt which brings about an amplification in the concentration field. Activation energy and  $\sigma$  effect on mass transfer field is presented in Figure 18(a) and (b). Increment in E increases the concentration because activation energy provides the energy to activate the chemical reaction. The concentration profile enlarges as a result of a magnification in E which provides substantial energy to process the reaction and strengthen the concentration field. Amplification in reaction rate parameter  $\sigma$  amplifies the overall activation energy phenomenon and concentration of the fluid.

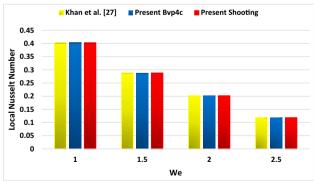


Figure 26: Numerical consequences of local skin Nusselt coefficient with  $\it We$ .

#### 6.4 Local skin friction and Nusselt number

In this section, the numerical aspect of physical quantities is presented via statistical graphs. Statistical Figures 19-22 are presented with attached numerical physical parameters. Figures 19-22 represent the comparison analysis of the obtained results with those obtained by Ali et al. [25], byp4c, and shooting for the case of surface drag coefficient due to variation in various dimensionless parameters like  $\beta$ , We, n, and  $\beta^*$ . From the figures, it is noticed that the incremental change in surface drag is observed in the case of  $\beta$  but decremented change is noticed in the case of the remaining parameters.

From Figures 23-26, it is observed that the obtained results are quite reliable in comparison to that in the already available literature, bvp4c, and shooting technique. The change in heat rate escalates owing to magnification in n, A, and  $\beta$  but diminishes in the case of an increment in We.

#### 7 Conclusion

The primary goal of this research is to acquire the numerical and tabular results of infinite shearing rate viscid of a cross rheological model including Brownian diffusion, thermophoretic, activation energy, and heat production under melting heat conditions. The gist of the current study is presented with sum-up points.

- 1) Activation energy promotes mass transport.
- 2) Due to imposed inclined magnetic field, Lorentz force is generated, hence the velocity of cross nanofluid is decreased.
- 3) Inclined magnetic effect causes decrease in the velocity of cross nanofluid.
- 4) For greater infinite shear rate viscosity parameter  $\beta^*$ , magnitude of velocity profile decreases.
- 5) Concentration profile *via Q* and *Nt* increases due to the heat generation effect.
- 6) Increment in *E* increases concentration because activation energy provides the energy to activate the chemical reaction.

The bvp4c technique could be applied to a variety of physical and technical challenges in the future [42–52]. Some recent developments exploring the significance of the considered research domain are reported in the studies [53-68].

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