Review Article

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Recent advances in electrocatalytic oxidation of 5-hydroxymethylfurfural to 2,5-furandicarboxylic acid: Mechanism, catalyst, coupling system

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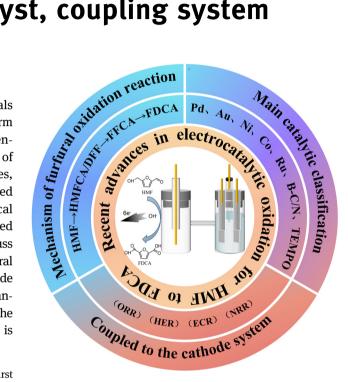
Abstract: Catalytic synthesis of value-added chemicals from sustainable biomass or biomass-derived platform chemicals is an essential strategy for reducing dependency on fossil fuels. As a precursor for the synthesis of important polymers such as polyesters, polyurethanes, and polyamides, FDCA is a monomer with high added value. Meanwhile, due to its widespread use in chemical industry, 2,5-furandicarboxylic acid (FDCA) has gained significant interest in recent years. In this review, we discuss the electrochemical oxidation of 5-hydroxymethylfurfural (HMF) and summarize the most recent advances in electrode materials from the past 5 years, including reaction mechanisms, catalyst structures, and coupling reactions. First, the effect of pH on the electrocatalytic oxidation of furfural is

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Graphical abstract

presented, followed by a systematic summary of the reaction mechanism (direct and indirect oxidation). Then, the advantages, disadvantages, and research progress of precious metal, non-precious metal, and non-metallic HMF electrooxidation catalysts are discussed. In addition, a coupled dual system that combines HMF electrooxidation with hydrogen reduction reaction, $\rm CO_2$ reduction, or $\rm N_2$ reduction for more effective energy utilization is discussed. This review can guide the electrochemical oxidation of furfural and the development of advanced electrocatalyst materials for the implementation and production of renewable resources.

Keywords: HMF, FDCA, furfural electrocatalytic oxidation, electrocatalysis, catalytic oxidation

1 Introduction

The increasing global energy demand, the depletion of non-renewable resources, and the worsening climate change

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resulting from the use of fossil fuels have prompted efforts to develop sustainable and environmentally friendly clean energy storage and conversion technologies. The only renewable and abundant carbon-containing resource that can be used to produce fuels and value-added chemicals is biomass. Since annual global production is approximately 1.7×10^{11} t, it is frequently used as an alternative to finite fossil resources [1]. Lignocellulosic biomass, the most abundant form of biomass, is a highly efficient renewable and sustainable alternative to conventional fossil fuels. Furfural acid is the most important oxidation product of the biomass molecule furfural. Furfural acid [2] is a crucial raw material in the pharmaceutical, agrochemical, flavor, and fragrance industries. As an alternative to terephthalic acid as a raw material for the synthesis of 2,5-furandicarboxylic acid (FDCA), furfural acid is also regarded as promising. In recent years, the electrooxidation process of 5-hydroxymethylfurfural (HMF) [3–5], a typical biomass-based platform compound, has been extensively investigated. FDCA, one of the products of the oxidation reaction of hydroxymethyl furfural (HMFOR), is receiving increasing attention as a monomer for the production of important polymeric materials such as polyethylene furan dicarboxylic acid ester [6]. The core literature on the electrocatalytic oxidation of HMF to FDCA has been limited in the last decade (Figure 1). Currently, FDCA can be synthesized from HMF by hydrothermal [7-11], biocatalytic, photocatalytic [12], and electrochemical oxidation [13]. During hydrothermal oxidation, HMF is initially oxidized to 2,5-diformylfuran

(DFF) or 5-hydroxymethyl-2-frantic acid (HMFCA), which is further converted to 5-formyl-2-furan carboxylic acid (FFCA) and FDCA under aerobic conditions [9]. The hydrothermal redox method usually uses tert-butyl hydroperoxide (TBHP) as the oxidant, whereas tert-butanol is also the most suitable solvent when TBHP is used as the oxidant [10]. The hydrothermal catalysis is more commonly used because of its efficient and convenient procedure. However, catalyst deactivation is usually unavoidable in the presence of strong acids or bases. In addition, thermal catalysis is usually performed at higher reaction temperatures leading to increased degradation of the substrate HMF [14]. The reaction pathway for the conversion of HMF to FDCA such as through electrochemical oxidation is similar to that of hydrothermal oxidation. Electrochemical oxidation provides favorable operating conditions, controlled selectivity and scalability, while it is a cleaner and safer method of FDCA production as it eliminates the use of high pressure oxidising atmospheres or other environmentally unfriendly chemical oxidants [15]. Driven by an external electrical potential, electrocatalysis offers significant advantages in solving thermodynamic and/or kinetic problems in thermal and photocatalysis, using inexpensive transition metals as highly active catalysts [14]. By controlling the electrode potential and circuit current, the management of electrocatalytic reaction parameters can be more accurate and easily achieved compared to thermal catalysis. At the same time, one should not overlook that electrocatalysis often requires a

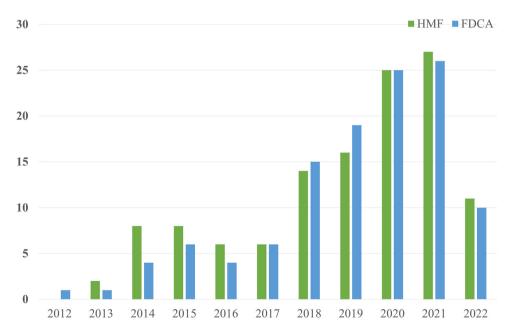


Figure 1: Number of annual core ensemble publications related to HMF and FDCA. Search engine: Web of Science. Keywords: HMF, FDCA; 19.05.2022.

PH
$$\geq$$
13

 H_2O+2e^- OH

OH

HMF

OH

H2O+2e

FFCA

FDCA

OH

OH

H2O+2e

PH \leq 13

Figure 2: Two direct oxidation pathways of HMF.

conductive electrolyte due to the poor conductivity of aqueous HMF solutions, leading to energy consumption for product separation in downstream processes compared to base-free multiphase catalysis. Depending on whether the applied potential drives the oxidation of HMF directly, the mechanism of electrochemical oxidation of HMF can be classified as either direct or indirect. There are six electron transfers in the reaction process, and both types of oxidation can occur separately or simultaneously [3].

1.1 Direct oxidation

If the applied potential drives the oxidation of the substrate directly, the valence state of the catalyst remains constant throughout the reaction; this is referred to as direct oxidation. The electrocatalytic reaction system is activated when the applied external voltage reaches the reaction's overpotential [16]. As shown in Figure 2, there are two possible direct oxidation pathways for the oxidation of HMF to FDCA: (i) the formyl group of HMF is first oxidized to give HMFCA (pH \geq 13), while the

hydroxymethyl group of HMFCA is oxidized to produce FFCA, and then the formyl group of FFCA is oxidized to form FDCA (HMF \rightarrow HMFCA \rightarrow FFCA \rightarrow FDCA); (ii) the hydroxymethyl group was first oxidized to DFF (pH < 13), then oxidized to FFCA, and finally FDCA was obtained (HMF \rightarrow DFF \rightarrow FFCA \rightarrow FDCA). The stability of the catalysts at different pH is different to the extent that different intermediates are produced, but both DFF and HMFCA are further oxidized to form 5-formyl-2-furan carboxylic acid (FFCA) and FDCA. Based on non-in situ detection, such as high-performance liquid chromatography (HPLC), the reaction pathways of HMF at different pH can be determined [17,18]. In addition, theoretical calculations can be used as a useful aid to gain insight into the oxidation process of hydroxymethyl furfural [19,20].

1.2 Indirect oxidation

In contrast to direct oxidation, in indirect oxidation, the applied potential does not directly drive substrate oxidation, and the valence state of the catalyst changes during

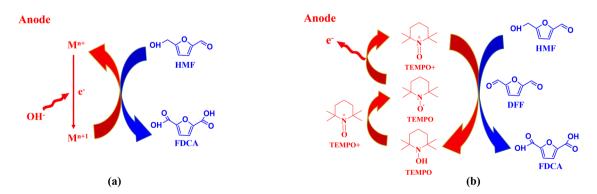


Figure 3: (a) Indirect oxidation reaction mechanism diagram of non-homogeneous oxidation medium (Mn⁺ represents the low valence state and Mn⁺¹ represents the high valence state) and (b) homogeneous oxidation medium (TEMPO-oxidation as an example).

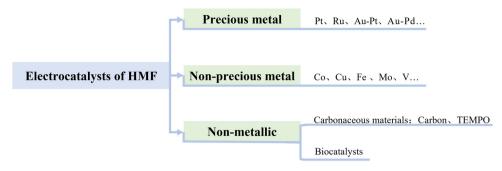


Figure 4: A brief classification of electrocatalysts for HMF conversion.

the oxidation process. The catalyst actually acts as a redox mediator to drive the oxidation of the substrate, which is a chemical process that does not require an applied potential [16]. Since this oxidation is referred to as indirect oxidation, it applies only to redox. As demonstrated in Figure 3, indirect oxidation is comprised of two sequential processes. The difference between a nonhomogeneous medium and a homogeneous medium is that the former requires OH— to participate in its oxidation. Therefore, strongly alkaline conditions (pH \geq 13) are more conducive to the oxidation of heterogeneous media.

This article provides a comprehensive review of HMF electrochemical oxidation. After proposing a pH-dependent reaction pathway and summarizing the reaction mechanism (direct and indirect oxidation), HMF electrooxidation catalyst materials are introduced, the brief classification of HMF electrocatalysts is shown in Figure 4. This paper introduces the development of precious metals, non-precious metals, and even non-metallic materials, with a focus on catalysts made of non-precious metals. In addition, a number of representative coupling reactions (e.g., HMF electrooxidation coupled with H₂ precipitation, CO₂ reduction, N₂ reduction [21], and organic reduction) for efficient energy conversion are discussed.

2 Detection method

Using linear scanning voltammetry (LSV), the electrocatalytic activity was analyzed. Chronoamperometry was used to monitor the electrochemical performance of the catalysts, and HPLC was used to analyze the electrolytes. Using the following equations, the HMF conversion, FDCA yield, and Faraday efficiency (FE) were calculated:

Conversion (%) =
$$\frac{\text{mol of HMF consumed}}{\text{mol of initial HMF}} \times 100$$
, (1)

Yield (%) =
$$\frac{\text{mol of FDCA formed}}{\text{mol of initial HMF}} \times 100$$
, (2)

FE (%) =
$$\frac{\text{mol of FDCA formed}}{\text{Total charge passed}/(F \times 6)} \times 100.$$
 (3)

3 Precious metal catalysts

Typically, noble metal catalysts are highly active in many chemical processes due to the unique electronic and orbital properties of noble metals [22]. For this reason noble metals are also used for HMF electrochemical oxidation, from single noble metals (e.g., Pd [23], Pt [13], Au [24], and Ru [25]) to noble metal alloys (e.g., PtRu and AuPd [26]). Table 1 displays the performance of HMF electrocatalytic oxidation of noble metal catalysts. As Au is combined with another precious metal to form an alloy catalyst, the catalyst will combine the benefits of both metals [27], this is because the electronic properties of Au are altered during the preparation of the alloy system, resulting in high activity, selectivity, and stability. The electronic properties of Au are altered during the preparation of the alloy system, resulting in a coordinated effect that improves the catalytic performance of the monometallic system [28]. Au and Pt are mainly present in the metallic state, with small amounts of Au⁺ and Au³⁺ or Pt²⁺ cationic states, which may be related to the surface oxidation of the metallic state or the interaction of the nanoparticles with the carrier [29,30]. Zhong's team developed an efficient and stable zeolite-supported Pt-Au alloy catalyst [11] for the selective oxidation of HMF to FDCA. The XPS results confirmed the formation of a Pt-Au alloy on the support. The binding energy of Au 4 f in the 1.5Pt₁Au₄/N-HNT bimetal is lower than that of 1.5Au/N-HNT, but higher than that in 1.5Pt/N-HNT. The shift in binding energy is attributed to the regio-electron

Table 1: Comparison of the performance of different noble metal catalysts for the oxidation of HMF

Туре	Catalyst	Electrolyte	<i>T</i> (°C)	HMF conversion (%)	FDCA yield (%)	FE (%)	Reaction time (h)	Ref.
Pt	Pt	1.0 M H ₂ SO ₄	25	88.3	_	_	_	[36]
	Pt	0.3 M NaClO ₄	25	9.0	_	9.0	_	[37]
Au	Au	1.0 M KOH	25	41.5	_	45.8	2	[13]
	Au/CeO ₂	2 equiv of Na ₂ CO ₃	140	99	91	_	15	[38]
AuPd	Au-Pd/IRA-743	2 equiv of Na ₂ CO ₃	100	100	93	_	4	[39]
	Au-Pd/nNiO	0.1 M NaBH ₄	90	100	99	_	14	[28]
Pd	Pd	1.0 M KOH	25	16	_	85.8	2	[13]
	Pd/CNT	2 equiv of K ₂ CO ₃	160	100	60	_	5	[40]
Ru	Ru(III)	0.1 M KOH	25	_	_	94	27	[41]
	Ru/C	2 equiv of NaHCO ₃	75	100	93	_	12	[25]
	Ru/HAP	H_2O	120	100	99	_	24	[42]
	Ru/MgAlO	H_2O	160	100	99	_	4	[43]

interaction between the Au and Pt atomic orbitals during the formation of the alloy [31,32]. The Fermi energy level of Pt is higher than that of Au. The higher electronegativity of Pt and the tendency of electrons to shift towards Au lead to changes in d-electron density and binding energy [33]. Verdeguer et al. demonstrated that alkalinity has a significant effect on the catalytic activity (and selectivity) of Pt/Pb-loaded catalysts [34]. On phosphorusfunctionalized carbon nanofibers (CNF) [35], Au-Pt nanoparticles were deposited and proved to be an effective catalyst for the oxidation of HMF to FDCA. The activity and selectivity to FDCA were significantly influenced by the P content of the CNF surface, with the highest P content catalyst producing the best results (98% selectivity to FDCA at 80% conversion after 1h). The authors demonstrated that Au-P interactions may have an impact on the electronic properties of the active site. Despite the fact that noble metal-based electrocatalysts have low initial potentials for HMF oxidation, they can only provide very low current densities, not even 10 mA cm⁻² in the applied potential range. In addition, complete oxidation of HMF to FDCA on a single noble metal is difficult. Due to the unique catalytic properties of Pd and Au for the competitive oxidation of hydroxyl and aldehyde groups in HMF, the Au-Pd alloy was able to generate higher yields of FDCA than single noble metal catalysts. Bonincontro et al. [28] reported an efficient and stable Au-Pd alloy catalyst containing nNiO. There is a significant synergistic effect between Au and Pd in the alloy and NiO, allowing the catalyst to achieve high conversion (95%), high activity, high FDCA yield (70%), and good stability. Using a layer-by-layer assembly technique, Park et al. fabricated a three-dimensional hybrid bimetallic electrocatalytic [13] electrode for simultaneous HMF conversion and hydrogen precipitation reaction (HER) and discovered that the thickness and structure of the LBL-assembled

multilayer electrode largely determined its electrocatalytic activity. In HER, the structure consisting of adjacent Pd and Au(AuPd)₇ electrodes is optimal for the rapid diffusion of hydrogen from Pd NPs to Au NPs. In addition, the fullcell electrochemical system containing HMF oxidation electrodes and HER was successfully regulated utilizing an optimized electrode combination.

4 Non-precious metal catalysts

Taking cost into account, the development of efficient non-precious metal or non-metallic catalysts remains the norm. Co [44], Cu [45], Fe [46,47], Mo, W, V [48], Pb, and Mn [49,50] are examples of non-precious metals that have been studied. In particular, nickel-based [3] and Cobalt-based materials represent non-precious metal catalysts with exceptionally high catalytic activity, far exceeding other metals, including noble metal alloys. For nickel-based catalysts, the catalytic mechanism follows an "electrochemical-chemical" reaction pathway, whereby divalent nickel species are electrochemically oxidized to trivalent nickel species, followed by a spontaneous redox reaction between the trivalent nickel species and the HMF as an oxidant [51,52]. By combining the electrochemical test, in situ Raman spectroscopy test, product characterization and theoretical calculations, Deng et al. [53] explored in depth the intrinsic link between the oxidation states of surface cobalt species and the kinetics of the HMF oxidation reaction and product selectivity under electrochemical oxidation conditions, and elucidated the different intrinsic catalytic activities of the in situ generated high-valent Co3+ and Co4+ species as oxidants involved in the selective oxidation of HMF. It is shown that Co³⁺ is only able to catalyze the slow oxidation

of aldehyde groups to carboxyl groups in HMF molecules, whereas Co⁴⁺ is able to achieve the rapid oxidation of hydroxyl/aldol groups. Based on this feature, this work has achieved the first modulation of the selectivity of the HMF electrochemical oxidation products, i.e., when the applied voltage is low, Co³⁺ is the main active species and the resulting product is 5-hydroxymethyl-2-furancarboxylic acid (HMFCA); when the applied voltage is high, Co⁴⁺ is the main active species and the resulting product is FDCA. A Ni-Co-based sulfide (NiCo-S) was prepared by Zhao's group [54], and the bimetallic site and coordination effects of the layered NiCo-S catalyst on HMF electrooxidation were demonstrated at the atomic level. Electrochemical experiments and theoretical results show that Ni-Co synergistically participates in HMF oxidation, where the Co site has strong diatomic adsorption (O and C atoms) on the aldehyde group, thereby facilitating the conversion of the aldehyde group to the carboxyl group, while the Ni site accelerates the reaction rate of FDCA. Also, the ligand S species contributes to the formation of strong diatomic adsorption with the aldehyde group of HMF, and the density of states (DOS) of NiCo-S has a higher carrier transfer conductivity than NiCo-O. This confirms the effect of the Ni-Co double active site and S coordination on accelerating the reaction and lowering the energy potential barrier, thus promoting catalytic activity to achieve 98.0% selectivity and 97.1% yield.

Homogeneous catalysis is considered to be an inexpensive and effective method of converting biomass derivatives into value-added chemicals, although it has separation and reuse problems [55]. Homogeneous metal bromides are widely used as catalysts for the aerobic oxidation of hydrocarbons [56]. Manganese based catalysts are the most active of the various catalytic systems due to the different oxidation states of Mn and the high oxygen storage capacity of the metal and the faster uptake and reduction of oxygen. Mn shows significant results in terms of HMF conversion and FDCA selectivity, both directly and in combination with other metals [57]. Zuo et al. [58] investigated the rate of oxidation of FDCA by HMF in acetic acid media with a Co/Mn/Br catalyst. The transient concentration distributions of the reactants (HMF) intermediates 2,5-diformylfuran (DFF), and FFCA and final product (FDCA) were obtained by rapid on-line sampling in a stirred semi-batch reactor. They showed experimentally that spray reactors in which the liquid is dispersed as fine droplets in the oxygencontaining phase can help to alleviate the oxygen shortage in the liquid phase, thereby increasing the overall reaction rate. Chen's team [59] developed a free radical chain reaction mechanism containing primary and secondary reactions over Co/Mn/Br catalysts to describe in detail the

liquid phase air oxidation of HMF to FDCA. Parallel reactions of HMF with DFF and HMFCA intermediating during MC were demonstrated for the first time. The majority of HMF tended to convert to DFF rather than HMFCA, which can be attributed to the retarding effect of the alcohol group on the oxidation of the aldehyde group and the low C-H bond dissociation energy on the hydroxymethyl group. The high activity of hydroxymethyl groups over aldehyde groups for the oxidation of HMF is explained for the first time on the basis of the inhibitory effect of alcohols on free radical reactions and the reactivity of reactive hydrogen on both HMF substituents. The team systematically evaluated the effects of temperature, pressure, substrate solvent ratio, catalyst composition and concentration, and water concentration on the primary and secondary reactions of HMF oxidation. Under optimal conditions, at 150°C, 0.8 MPa air pressure, Co/Mn/Br molar ratio of 29/1/30, and HMF/HAc mass ratio of 1/9, the occurrence of side reactions could be reduced and the yield of FDCA maximized, resulting in a selectivity of 92% for FDCA and complete conversion of HMF with a total conversion time of less than 20 min, The purity of FDCA exceeded 99.8% [60]. The experimental results provide new ideas for the in-depth study of the oxidation process of hydroxymethyl furfural, and are of great significance for the large-scale production of FDCA. In addition, a comparison of the performance of different non-precious metal catalysts for the oxidation of hydroxymethyl furfural is shown in Table 2.

It was demonstrated that the introduction of abundant oxygen vacancies can enhance the catalytic activity and selectivity of FDCA by increasing the electrochemical surface area and decreasing charge transfer resistance. Density flooding theory (DFT) calculations [61] show that increasing the amount of oxygen vacancy (Ov) not only improves the alcohol activity of the catalyst by reducing the generation energy of Ov, but also promotes the adsorption and activation of O_2 on the catalyst by significantly reducing the adsorption energy of O2, thus improving the oxidation activity of the catalyst towards HMF. Since the introduction of oxygen vacancies can enhance the activity of the catalyst against hydroxymethylfurfural, Han's group [62] was the first to develop highly stable metal oxides. They introduced oxygen vacancies via Se doping, and the resulting CoO/CoSe₂ with a molar ratio of 23:1 exhibited excellent performance and stability in the electrooxidation of HMF to FDCA, achieving a 99.0% yield of FDCA and a 97.9% FE at a potential of 1.43 V vs reversible hydrogen electrode potential (RHE). Huang's team [63] synthesized two-dimensional (2D) polycrystalline cobalt oxide (Co₃O₄) nanosheets without

Table 2: Comparison of performance of different non-precious metal catalysts for the oxidation of HMF

Туре	Catalyst	Electrolyte	<i>T</i> (°C)	HMF conversion (%)	FDCA yield (%)	FE (%)	Reaction time (h)	Ref.
Ni	Ni ₃ N@C	1.0 M KOH	25	100	98	_	_	[36]
	Ni _x B-modified NF	1.0 M KOH	25	100	98.5	100	0.5	[64]
	NiSe@NiO _x	1.0 M KOH	25	100	99	99	2	[65]
	NiFe LDH	1.0 M KOH	_	99	98	94.4	_	[66]
	NiCoFe LDHs	1.0 M NaOH	55	95.5	84.9	~90	1	[67]
	Ni ₂ S ₃ /NF	1.0 M KOH	_	100	98	94	2	[68]
	$Ni(OH)_2/NF$	1.0 M KOH	_	100	100	99	1.5	[69]
Co	Co-P_DES	0.5 M NaHCO3	25	99	85.3	77.3	_	[70]
	CoO-CoSe	1.0 M KOH	25	100	99	97.9	~1	[62]
	NiCo ₂ O ₄	1.0 M KOH	25	99.6	_	87.5	~1	[71]
	NiCo ₂ O ₄ /NF	1.0 M KOH	25	99.6	90.8	87.5	~1	[71]
	Co ₃ O ₄ nanowires/NF	1.0 M KOH	_	100	96.8	96.6	5.73	[72]
	NiCo-MOFs	pH = 13	_	_	99	78.8	6	[73]
Cu	Cu _x S@NiCo-LDH	1.0 M KOH	_	~100	99	100	_	[74]
	Cu(OH) ₂ NWs/CuF	0.1 M KOH	25	96.4	80.3	80.5	~3.4	[75]
	CuO NWs/CuF	0.1 M KOH	25	99.4	90.9	90.4	~1.5	[75]
	CuNi(OH) ₂ /C	1.0 M KOH	25	100	93.3	~95	5	[76]
	$CuMn_2O_4(Cu/Mn-1)$	MeCN	80	100	90.5	_	12	[77]
Mo	NF@Mo-Ni0.85Se	1.0 M KOH	25	100	95	-	2	[78]
	MoO ₂ -FeP	1.0 M KOH	25	99.4	_	97.8	2.7	[47]
Mn	MnO_2	0.6 mM NaHCO₃	100	100	91	_	24	[49]
	MnOx	1.0 M H ₂ SO ₄	25	99.9	53.8	33.8	_	[36]
	$MnFe_2O_4$	H_2O	100	_	85	_	5	[79]
٧	3D VN HNs	1.0 M KOH	25	98	_	84	~0.9	[48]
Fe	FeOOH	0.1 M KOH	25	16	~1.6	~1.6	2.3	[80]

surfactant, independent, and graded with oxygen-rich vacancies (Co₃O₄ VO) by topological transformation through rapid calcination of ultrathin cobalt oxide nanosheets synthesized by solvent heat. The nanosheets preserved the 2D structure and reduced the number of P123 surface active sites that are exposed. Furthermore, we suggest that strain-induced oxygen vacancies at the grain boundaries of Co₃O₄ nanocrystals are responsible for the enhanced electrooxidation properties. Co₃O₄-VO nanosheets exhibited significantly higher catalytic activity in oxygen evolution reaction (OER), particularly in the electrooxidation of HMF to FDCA, compared to conventionally synthesized CoOxHv nanosheets and conventionally calcined Co₃O₄ nanosheets.

In recent years, the majority of research has centered on the high performance oxidation of HMF utilizing electrocatalysts (such as 3D Ni foam [81], 3D Cu foam [82], and carbon paper [83]) deposited on high surface area 3D porous substrates. Metal foams with three-dimensional (3D) open pore structures have a high specific surface area and structural stiffness [82], making them suitable self-supporting substrates for in situ growth or coating of active materials. Pang et al. reported that CF-coated Cu (OH)2 is an effective electrocatalyst for HMF oxidation [84], enabling FDCA production with close to 100 percent

FE (yield: 98.7%). Using a polyethylene glycol template, Hu's team synthesized a 3D porous WO₃/Ni electrode [1] in a controlled manner at low temperature. The electrochemically active surface area of the electrode can reach 40 cm² if it has a high electrochemical catalytic performance. It is possible to achieve a good catalytic effect in a mild environment at room temperature and pressure. In 1.0 M KOH electrolyte, the HMF conversion was 99.4%, the FDCA yield was 88.3%, and the FE was 88.0%. Sun's team [82] reviewed the recent progress of CF-derived electrodes as low-cost and efficient electrocatalysts in combination with the advantages of 3D mesh structure of metal foams, and focused on their applications in conventional and hybrid water electrolysis. Ni-based [85] catalysts are considered as one of the best candidates as a catalyst for HMF electrooxidation due to the rich 3D electron number and unique electron orbitals that enhance the covalency of transition metal-oxygen bonds, and have been extensively studied. Liu's team [86] reported the efficient electrocatalytic oxidation of HMF to FDCA and furfural to furandicarboxylic acid using easily synthesized NiCoMn layered double hydroxide (LDH) nanosheets, rich in oxygen vacancies, loaded on nickel foam (NF). The effects of different metal ratios, reaction temperatures, and reactant

Figure 5: Schematic diagram of the electrochemical system for simultaneous HMF oxidation and hydrogen reduction over a bifunctional core-shell NiSe@NiO_x catalyst.

concentrations on FDCA yields were systematically investigated. Niu team [66] reported the vertical electrochemical growth of NiSe@NiOx core-shell nanowires on NF as a non-precious metal electrocatalyst for the preparation of FDCA by electrooxidation of HMF (Figure 5). The core-shell NiSe@NiOx catalyst achieved 100% yield and 99% FE due to the unique structure of the core-shell exposing more active sites and favoring high electron transfer capability. In addition to the efficiency and activity, the catalytic mechanism is currently an important factor. The electrochemical oxidation of HMF on nickel-based materials closely resembles the indirect oxidation process [87,88]. Even though there are numerous advanced strategies for HMF electrooxidation on Ni-based catalysts, achieving high current densities at low potentials remains a challenge. Therefore, future research should focus on enhancing the kinetics of HMF electrooxidation and decreasing the reaction time while maintaining high catalytic efficiency.

Studies have demonstrated that interfacial effects can generate a large number of cationic vacancies and that cationic vacancies play a crucial role in catalyzing the electrooxidation of HMF. Lu et al. [18] successfully prepared graded nanostructured NiO-Co₃O₄ electrodes with abundant interfacial defects using a simple hydrothermal annealing technique. Due to the dissimilar crystal structures of Co₃O₄ (spinel) and NiO (face-centered cubic), the atomic arrangement at the interface is not one-to-one, resulting in an abundance of defects and vacancies (Figure 6). With a high FDCA yield of 98% and a FE of 96%, the nanosheets exhibited superior HMF oxidation activity and stability. For this reason, interfacial engineering is an effective strategy for designing high-quality and highly effective electrocatalysts. Qi's team [89] successfully prepared self-supporting cation-defect-rich NiFe-LDH (d-NiFe LDH/CP) catalysts

through a hydrothermal process and alkaline etching treatment. A series of physical characterization studies confirmed the successful removal of the zinc component and the introduction of cationic vacancies. Among them, NiFe-LDH (d-NiFe LDH/CP) is the best catalyst for the reaction of electrochemical oxidation of HMF to FDCA. The catalyst showed excellent catalytic performance at 1.48 V, obtained 97.35% conversion of HMF, 96.8% yield of FDCA, and 84.47% of FE, and the catalytic performance was maintained even after ten cycles. The introduction of a large number of cationic vacancies is the key to achieve high catalytic activity, which greatly tunes the electronic structure of NiFe LDH. This greatly increased the electrochemically active surface area and reduced the charge transfer resistance. This provides insight into the design of defect-rich catalysts and their application in the upgrading of electrochemical biomass derivatives. Due to the rich oxygen vacancy structure and high surface area of the nanosheets, Gu's team [90] successfully generated a defect-rich high-entropy oxide (HEO) nanosheet with high surface area utilizing a lowtemperature plasma method and for the first time employed it for the electrooxidation of HMF (Figure 6). In comparison to HEO made using the high-temperature method, the binary (FeCrCoNiCu)₃O₄ nanosheets demonstrated excellent electrocatalytic performance for the oxidation of HMF with lower onset potential and faster kinetics, opening up new possibilities for the synthesis of nanostructured HEO with great application potential and electrocatalytic oxidation of furfural.

It has also been demonstrated that metal-organic framework (MOF) nanosheets are effective catalysts for the electrochemical oxidation of HMF. Cai *et al.* were the first to investigate the use of nickel-based 2D MOFs (2D-MOFs) [73] as electrocatalysts for HMF oxidation.

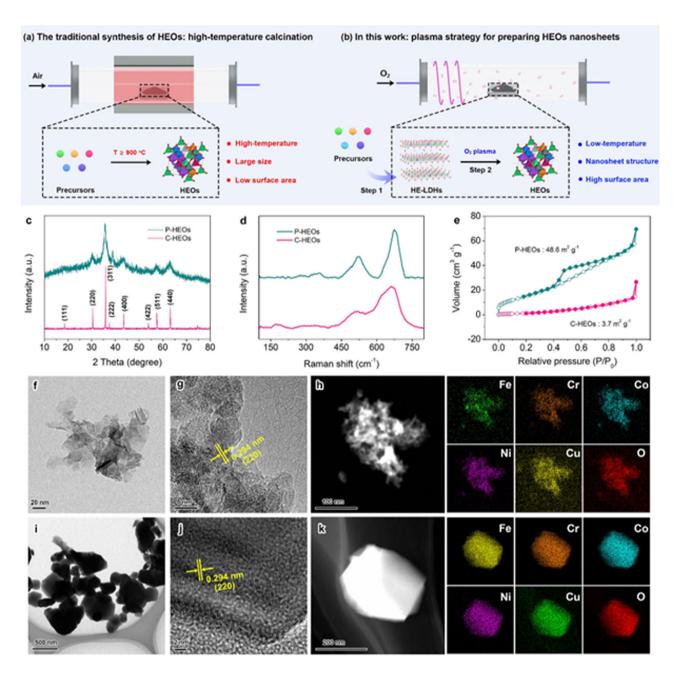


Figure 6: (a) The traditional synthesis method and (b) low-temperature plasma strategy for HEOs. (c) XRD patterns, (d) Raman spectra, and (e) N₂ adsorption—desorption isotherm of P-HEOs and C-HEOs. (f) and (i) TEM, (g) and (j) HRTEM, and (h) and (k) EDX mapping of P-HEOs and C-HEOs, respectively. Copyright © 2021 Wiley-VCH GmbH.

Their prepared co-doped 2D-MOFs-NiCoBDC (Ni²⁺, BDC = terephthalic acid) exhibited a high FDCA yield of 99% and a FE of 78.8% in an electrolyte at pH 13. Due to their abundant exposed active sites and the coupling effect between Ni and Co atoms, the 2D NiCo-MOFs exhibited high catalytic activity and strong electrochemical stability. Chamberlain's team [91] discovered that the oxidation-active MIL-100(Fe) MOF synthesized in water is an effective, stable, and recoverable MOF catalyst. Within

24 h, HMF was completely converted as a result of the synergistic effect of the MOF and the co-catalyst TEMPO. Under optimal reaction conditions, the maximum yields of FDCA and FFCA, respectively, were 57 and 17%, with an overall selectivity of 74%. Compared to other HMF oxidation catalysts using TEMPO as a co-catalyst, this is the only example of using water as a solvent. The porosity and abundance of active sites in 2D MOF make it a promising catalyst.

Table 3: HMF electrooxidation performance of non-metallic catalysts

Type	Catalyst	Electrolyte	<i>T</i> (°C)	HMF conversion (%)	FDCA yield (%)	FE (%)	Reaction time (h)	Ref.
Carbon	Carbon B-N co-doped porous carbons (BNC-2)	0.1 M NaOH	25	71	57	I	9	[96]
TEMPO	TEMPO	0.5 M sodium borate buffer	25	6.66	93.8	93.8	I	[67]
	BiVO4/CoPi-30	5.0 mM TEMPO	ı	95	88	ı	2.7	[86]
	Hub-TEMPO	0.5 mM LiClO4	25	66	78	ı	20	[66]

5 Non-metallic catalysts

Non-metallic catalysts can circumvent metallic catalysts' disadvantages, such as high cost and product contamination. Two types of non-metallic catalysts have been studied for the electrochemical oxidation of HMF: non-homogeneous carbon-based materials [92,93] and homogeneous N-oxyl materials (i.e., TEMPO [94] and its derivatives). 4-acetamido-TEMPO [95] (ACT TEMPO = 2,2,6,6-tetramethylpiperidin-1-yloxy) has been identified as a highly promising homogeneous electrocatalyst for alcohol oxidation; TEMPO derivatives offer superior activity at a lower price. It permits the indirect electrochemical oxidation of HMF to FDCA [17] with close to 100% FE. The properties of the non-metallic HMF electrooxidation catalysts are listed in Table 3.

6 Coupling with cathode system

In recent years, more and more people have turned their attention from uncoupled 5-HMF oxidation catalytic system to its coupling system. This is because the coupled system can first improve the energy utilization efficiency of the whole system. Second, the coupling system is promising to upgrade biomass derivatives into value-added products at the same time. Finally, the coupling system can further promote the industrialization of electrocatalytic furfural oxidation. The OER is a common anodic half-reaction that acts as a counter electrode in a range of electrocatalytic conversion technologies, such as electrocatalytic water separation, carbon dioxide reduction reaction (CO2RR), nitrogen reduction reaction (NRR), and nitrate reduction reaction (NO₃-RR). However, the slow kinetics of the anode OER leads to a significant overpotential, which largely restricts the rate of the entire electrocatalytic reaction. For example, hydrogen generation in water splitting is limited due to the four-electron transfer of the anode OER, requiring a high cell voltage to drive the overall water electrolysis. Therefore, the replacement of OER with thermodynamically more favorable organic oxidation reactions has attracted great interest.

In recent years, oxidation reaction (OER) is a common anodic half-reaction, similar to electrocatalytic decomposition of water, and electroreduction of organic small molecules such as CO_2 and N_2 for energy or fine chemicals is gradually becoming a hot topic [100–102]. Furthermore, this series of electrocatalytic conversion technologies frequently acts as counter electrodes. Numerous studies have combined the commonly employed hydrogen precipitation reactions, CO_2RRs , NRRs [96], and NO_3 -RR with anodic oxidation reactions, and the design of electrochemically

coupled systems is emerging as a promising area of research. However, the slow kinetics of the anodic OER leads to a high overpotential, which largely limits the overall electrocatalytic reaction rate, consequently, substituting the OER with a thermodynamically more favorable organic oxidation reaction, which has drawn great interest. Theoretically, this coupled reaction system is twice as efficient (200%) as a conventional reaction system, but consumes the same amount of energy. The anodic oxidation kinetics of HMF is better than OER, so the starting voltage for HMF oxidation is lower than OER. By replacing OER with HMF oxidation at the anode, organic substrate reduction, H₂ production, CO₂RR, and NRR can be achieved simultaneously at a lower voltage [16]. The bifunctional linked system consisting of furfural oxidation and reduction reactions can not only maximize the return on energy investment but also provide value-added products for both parties. Table 4 shows the properties of different catalysts in the coupled system for the HMF electrooxidation catalyst.

6.1 Coupling with CO₂RRs

In CO₂ reduction reactions (CO₂RRs), typical CO₂RR electrolyzers tend to use slow kinetic and high overpotential anodic OER, resulting in low anodic product values and wasteful operating costs. To address the problems of low space utilization and low energy utilization of the currently commonly used monopole CO₂ electroreduction reaction process (cathode CO₂ reduction and anode water

oxidation to oxygen), it is crucial to construct a paired electrochemical reaction system with cathode CO₂ reduction coupled with anode organic oxidation. It was discovered that partial oxidation of furfural coupled with H₂ precipitation or other reduction reactions (such as CO₂ [109]) in an electrochemical cell permits electrolysis at lower voltages while yielding a more valuable product than O2. The introduction of biomass oxidation as an alternative anode reaction in an electrolyte saturated with CO2 and near neutral allows for an efficient CO2 electrolysis system. The Nam team [107] designed and synthesized nickel oxide nanoparticles (NPs) 3D transition metal-based catalysts NiO, Mn₃O₄, and Co₃O₄ NPs using a thermal injection method in order to establish an efficient HMF-CO₂ double electrolysis system. Native electrolysis in 0.5 M KHCO3 saturated with CO2 was performed at 2 mA cm⁻² for 3 h. The cell voltage was 2.5 V. The FE from biomass conversion was 36% and the FE from formate (HCOO-) production was 81%. They successfully demonstrated a formate production system combined with biomass oxidation for the simultaneous production of liquid fuels and synthesis of valuable polymer feedstocks. Han's team [110] used PdOx/ZIF-8 as the cathode catalyst and PdO as the anode catalyst to efficiently catalyse the reduction of CO2 to CO at the cathode and the oxidation of HMF to organic acids at the anode. Figure 7a-d shows that the CO2RR-HMFOR system has higher current density and efficiency at the same tank voltage. Furthermore, the paired CO₂RR-HMFOR system only requires a starting tank voltage of 1.06 V, which is much lower than the CO₂RR-OER system (1.77 V) (Figure 7e). The tank voltage could be reduced by

Table 4: Comparison of performance of different catalysts for the oxidation of HMF in coupled systems

Туре	Catalyst	Electrolyte	<i>T</i> (°C)	HMF conversion (%)	FDCA yield (%)	FE (%)	Reaction time (h)	Ref.
Ru	Ru(III)-PEI@MWCNT	1.0 M KOH	_	_	_	94	27	[41]
	Ru/MgO	Aqueous conditions	160	100	90	_	4	[43]
Co	Cu _x S@NiCo-LDH	1.0 M KOH	_	87	~99	~99	20	[74]
	NiCo ₂ O ₄	1.0 M KOH	_	>99	>99	>99	2	[44]
	CoNiP-NIE	1.0 M KOH	_	_	87.2	87.2	_	[103]
	Co ₃ O ₄ /CF	1.0 M KOH	_	100	93.2	92.9	1.67	[104]
BNC	BNC-2	0.1 M NaOH	25	71	57	_	6	[96]
Ti	Ti-MOF	0.7 M MEA electrolyte (pH 11.0)	_	35	30	_	6	[105]
Ni	NiB _x @NF	1.0 M KOH	_	99	99	99	1.67	[19]
	NiMoP/NF	1.0 M KOH	30	91.9	99.7	107.1	2	[106]
	NiO NPs	0.5 M KHCO ₃ (pH 7.2)	_	90	30	35	_	[107]
	CoOOH/Ni	1.0 M KOH	_	_	90.2	92.3	_	[108]
	NiCo-S	1.0 M KOH	_	99.1	97.1	96.4	0.67	[54]
	CoFe@NiFe	1.0 M KOH	_	100	100	99.8	1	[83]
	Co _{o.4} NiS@NF	1.0 m KOH	_	98.8-100	96.3-99.9	100	_	[87]

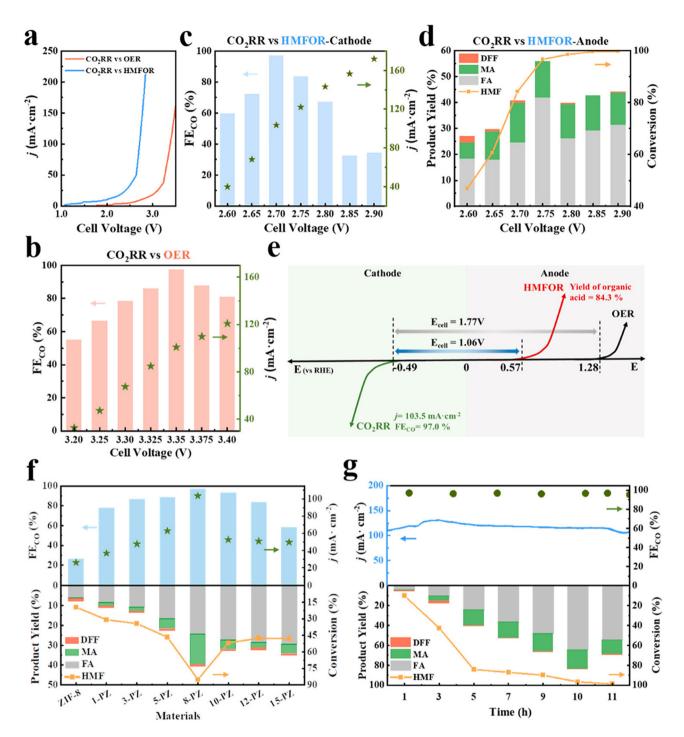


Figure 7: Performance of $CO_2RR-OER$ and $CO_2RR-HMFOR$. (a) Current density vs cell voltage curves of CO_2RR with OER or HMFOR over 8-PZ cathode and 8-PdO anode (scan rate: 20 mV s⁻¹); (b) CO_2RR vs OER: FE of CO and current density at different cell voltages for 8-PZ; (c) CO_2RR vs HMFOR cathode: FE of CO and current density at different cell voltages for 8-PZ; (d) CO_2RR vs HMFOR anode: the conversion of HMF and the yield of products at different cell voltages for 8-PdO (electrolysis time: 5 h; temperature: 40°C); (e) the comparison between a traditional single reaction and paired electrolysis system; (f) current density, FECO, the conversion of HMF, and the yield of anodic products on various catalysts (cell voltage: 2.70 V; electrolysis time: 5 h; temperature: 40°C); (g) long-term electrolysis results of CO_2RR and HMFOR over 8-PZ cathode and 8-PdO anode (cell voltage: 2.70 V; temperature: 40°C). Copyright © 2022 American Chemical Society.

0.71 V compared to the conventional paired OER reaction, and at a tank voltage of 2.70 V, a current density of 103.5 mA cm⁻² was achieved at a cathodic CO FE of 97.0% using 8-PZ as the catalytic material; meanwhile, 84.3% organic acid yields were achieved on the anode, including 20.0% maleic acid (MA) and 64.3% formic acid (FA) (Figure 7f and g).

6.2 Coupling with NRRs

Since the thermodynamics of HMF oxidation are more favorable than OER, the first attempt to combine ammonia production with biomass upgrading was made by Xu et al. [41] who investigated a straightforward and effective technique for the production of Ru(III)-PEI@MWCNT catalysts for the electrocatalytic oxidation of NRR and HMF in alkaline environments. During 27 h of stable electrolysis, the current density was 0.50 mA cm⁻² and the cell voltage dropped from 1.56 to 1.34 V compared to the OER. And the yields and FEs of NH₃ and FDCA were high, and the oxidation products obtained, FDCA, were more valuable than the HMF and O₂ obtained by water cracking. The team of Oschatz [96] reported the synthesis of nitrogen and boron co-doped porous carbons, which has a unique structure with porosity, a high amount of heteroatom doping, and a high oxidation potential. As the created B-N motif combined a large number of unpaired electrons and frustrated Lewis pairs (FLPs), the B-N motif was extremely reactive. In the absence of metal auxiliaries, they performed well in both the electrochemical oxidation and NRR of HMF. The yield of NH₃ was steady at 21.3 µg h⁻¹ mg⁻¹, and the FE reached 15.2%. Additionally, FDCA was generated for the first time utilizing a non-metal electrocatalyst with a 71% conversion and a 57% yield. Gas adsorption investigations clarified the link between the structure of the catalyst and its ability to

activate substrate molecules. They shed light on the logical design of non-metal-based catalysts for prospective electrocatalytic applications and the increase in their activity through the introduction of FLP and grain boundary point defects (Figure 8).

6.3 Coupling with hydrogen evolution reaction

Electrochemical hydrogen production is considered to be an efficient and forward-looking sustainable technology, but its anodic oxygen precipitation reaction OER kinetics are slow and the value added to the product is low. Although the overpotential of OER can be reduced by developing advanced electrocatalysts, a qualitative breakthrough in overall reaction efficiency is yet to be achieved. Systems using biomass-derived chemicals such as glucose, furfural, and HMF as substrates for oxidation reactions are particularly attractive because the electricity and organic feedstock used are renewable and the hydrogen generation process is fully sustainable [54]. The use of new anodic oxidation reactions with good thermodynamics and kinetics in combination with cathodic hydrogen precipitation reactions (HER) can reduce the voltage required for electrolytic systems. Deng et al. developed and produced low-energy Cu_xS@NiCo-LDH core-shell nanoarray electrocatalysts [74] for HMF oxidation and water reduction, while simultaneously producing FDCA and hydrogen fuel with additional value. Zhou et al. produced and fabricated a variety of Ni_xCo_{3-x}O₄ electrodes using a simple hydrothermal technique [44]. At 1.45 V (relative to RHE), a highly selective conversion of HMF to FDCA was accomplished with >99% conversion and FE efficiency, as well as

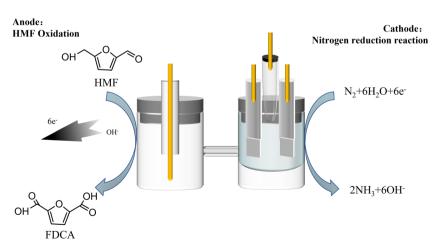


Figure 8: Schematic diagram of the electrochemical system used for electrocatalytic NRR with HMF oxidation and the whole cell reaction.

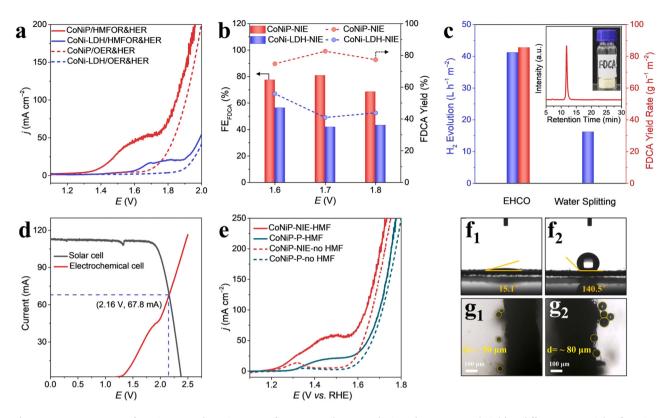


Figure 9: (a) LSV curves of CoNiP-NIE and CoNi-LDH-NIE for EHCO and water splitting. (b) FEFDCA and yield at different potentials of CoNiP-NIE and CoNi-LDH-NIE for EHCO. (c) H₂ evolution rate and FDCA yield rate of CoNiP-NIE for EHCO system and water splitting system (the inset shows HPLC chromatogram and digital photograph of FDCA powders). (d) I–V curve of commercial Si solar cell under illumination together with polarization curve of the catalytic cell. (e) LSV curves of CoNiP-NIE and CoNiP-P in 1 M KOH in the presence and absence of 10 mM HMF. The connect angles of (f1) CoNiP-NIE and (f2) CoNiP-P. Microscope photographs of H₂ bubbles on the surface of (g1) CoNiP-NIE and (g2) CoNiP-P. © 2022 Published by Elsevier.

a considerable increase in hydrogen production of 8.16 times that of pure water oxidation. Song et al. [103] reported a bifunctional nickel-titanium alloy nanosheet integrated electrode (CoNiP-NIE) to enhance HER and replace OER by 5-hydroxymethylfurfural oxidation reaction (HMFOR) to obtain high-value FDCA. As can be seen from Figure 9, FE_{FDCA} on CoNiP-NIE could reach 87.2% at 1.50 VRHE and FE_{FDCA} exceeded 82% over a wide potential range from 1.40 VRHE to 1.70 VRHE. CoNiP-NIE also showed good HER activity with overpotentials as low as 107.56 mV at -10 mA cm⁻² current density. Furthermore, the CoNiP-NIE-based bifunctional EHCO system exhibited an ultra-low cell potential (1.46 V) and a higher H₂ precipitation rate (41.2 L h⁻¹ m⁻²) compared to the hydrolysis system (1.76 V, 16.1 L h⁻¹ m⁻²). This ECHO system achieved a high FDCA yield (85.5 g h⁻¹ m⁻²), further improving the economic efficiency of hydrogen production. The bilayer hydroxide (CoFe@NiFe) [83], synthesized by the electrodeposition method of Zhao's team, can selectively react with six electrons of HMF to produce FDCA via an anodic half-reaction in a two-chamber system with cathodic HER. The overall reaction reaches $38\,\text{mA}\,\text{cm}^{-2}$ at $1.40\,\text{V}$ and exhibits 100% selectivity, producing FDCA and almost 100% FE with a hydrogen yield of $901\,\mu\text{mol}\,\text{cm}^{-2}$. Sun's team [87] developed a convenient route based on *in situ* heteroatom doping to prepare co-doped Ni₃S₂ electrocatalysts on NF substrates. The optimized electrocatalyst (Co_{0.4}NiS@NF) electrode requires only a very low starting potential and achieves high current density at a lower potential. Very high production rates of cathodic H₂ and anodic value-added chemicals were achieved in the HMFOR-assisted conventional HER cathodic reaction process, providing a reference for the development of industrial-scale electrocatalytic production of H₂.

6.4 Coupling with other reactions

In electrocatalytic processes, metal sulfides [111] (sulfides and selenides) have also been widely explored. They can

exhibit an extensive range of crystalline phases and oxidation states, and can be used to catalyze UOR and HMF-EOR reactions by constructing multiphase structures and doping non-homogeneous atoms to generate new active centers that enhance intrinsic activity and accelerate electron transfer. Zhang et al. [19] prepared NiB_x catalysts to oxygenate HMF to FDCA while hydrogenating p-nitrophenol to p-aminophenol in a 1 M KOH electrolyte, achieving 99% conversion efficiency and selectivity. This paired electrosynthetic cell was also coupled to a solar cell as a stand-alone reactor to cope with sunlight. The Liang team [106] demonstrated the use of paired electrolysis of acrylonitrile (AN) and HMF for the simultaneous production of acetonitrile (ADN) and FDCA. Their paired electrolysis reaction system, using electrodeposited NiMoP amorphous film-covered NF as the anode, effectively increased HMFOR activity and expanded ECSA by in situ selective removal of surface Mo and P. By adding DMF to the cathode chamber, the solubility of ADN was increased and the resulting single-phase solution provided better mass transfer for the hydrolysis of AN. DMF as co-solvent increased the solubility of ADN and the resulting single-phase solution provided better mass transfer for the hydrolysis of AN. The ANEHD-HMFOR pairing system allowed the production of FDCA and ADN at high currents (160 mA) as the cathode and anode simultaneously increased the conversion of the substrate molecules, achieving 83.7% FDCA yield for the anode and 62.3% ADN yield, with a FE of 107.1% for the whole cell. Román et al. [112] optimized FA production by limiting the coupling to the Pt electrode surface, thereby prevented decarbonylation/decarboxylation (and the associated complete oxidation of furan groups) and induced aggregate effects of modifiers such as Bi or Pb (which adsorb irreversibly to Pt under electrooxidation conditions) or self-assembled monolayers [113]. The selectivity of MA and HFN is optimized by doping the Pt surface with an oxygen-loving metal (such as Ru), thereby increasing the concentration of active OH* species at the surface. These "bifunctional" Pt alloys or composites can increase CO oxidation at lower potentials and can release the metallic Pt surface at steady state, producing C4 products (via the decarbonization pathway). A paired photoelectrochemical cell (PEC) was successfully constructed by Bharath et al. [114]. They employed Au/α-Fe₂O₃/RGO as the photoelectric cathode and Ru/RGO-modified Pt as the anode, reducing CO₂ at the cathode to CH₃OH and oxidizing furfural at the anode to 2-FA and 5-HFA. Both PEC CO2 reduction and furfural oxidation at various anode solution concentrations produced high CH₃OH vield (63 µmol L⁻¹ cm⁻²), 82% FF conversion, 63% yield of 2-FA, and 19% yield of 5-HFA with good stability. Electrocatalytic reductive amination and simultaneous oxidation (ERAO) was proposed to convert biomassderived HMF to valuable 2-hydroxymethyl-5-(ethanolamine methyl) furan (HEMF) and FDCA at the cathode and anode, respectively. Zhang's team [105] suggested an ERAO approach to convert biomass-derived HMF to useful HEMF at the cathode and FDCA at the anode. They devised and produced titanium-based MOF (Ti-MOF) cubes and NiCoF-LDH nanosheets as cathode and anode materials, respectively. ERAO showed very good performance overall, with 67.8% conversion of HMF in ERAO, 99% selectivity for HEMF (cathode), and 35% selectivity for FDCA after 6 h of reaction (anode), which is closely related to the additional internal site access provided by the Ti-MOF exposed N-Ti-O active center and the porous structure.

6.5 Coupling with photovoltaic electrolysis

In addition, the coupling reaction of hydroxymethyl furfural oxidation with photovoltaic electrolysis has also become a hot topic of interest. Chen's [104] team used in situ electrochemical modulation to prepare a highly efficient multifunctional hydrangea-like CoO electrocatalyst. The defective structure and abundance of electroactive sites enabled the catalyst to achieve photovoltaic electrocatalysis for the simultaneous production of FDCA and H₂. The team constructed the first solar-driven integrated reaction using photovoltaic electrocatalysis (PVEC) of 2,5-Bis(hydroxymethyl)furan (BHMF), effectively improving the overall sustainability. Takanabe's [108] team believes that efficient electrochemical devices can convert electrical energy from intermittent renewable energy sources into chemical form. The different targets and the choice of combinations provide different thermodynamics and kinetics for redox reactions. They demonstrate a promising approach for the production of H₂ using an intermediate redox medium in combination with sulfide remediation. For the first time, Zhang's team used the more stable furan molecule BHMF as the reaction substrate for the coupling system and prepared vertical CoOOH nanosheet electrocatalysts [108] by simple electrodeposition and subsequent oxidative activation, achieving complete conversion of BHMF with 90.2% FDCA yield and 100% current efficiency for H2 evolution, providing a green coupling electrolysis for industrial applications.

7 Summary and outlook

FDCA is a viable biomass-derived feedstock, and its most attractive application is as a substitute for terephthalic acid derived from petroleum for the synthesis of valuable biobased polymers, polyethylene-2,5-furandicarboxylate. In recent years, the electrocatalytic synthesis of FDCA from bio-based HMF has garnered increased interest due to its substantial economic and sustainable benefits. Meanwhile coupling furfural oxidation with numerous reduction reactions can be used for a variety of energy-related applications, with remarkable achievements in the catalytic synthesis of FDCA and its derivatives by different methods. The selective catalytic oxidation of HMF to FDCA is therefore seen as a promising process that can effectively reduce energy consumption and environmental pollution issues. However, there are still some practical problems:

- In the oxidation of HMF to FDCA, most of the current methods are carried out in water in the presence of excess alkali, which is an environmentally unfriendly and expensive process, and various by-products such as furan compounds are formed, so there is a need to develop greener catalytic systems and find milder conditions to achieve high FDCA selectivity.
- 2) From a practical application point of view, it is vital to produce more efficient, active, and stable transition metal catalysts for the aerobic oxidation of HMF to FDCA compared to expensive precious metal materials.
- 3) The design of electrochemically coupled systems is becoming a promising area of research. Bifunctional coupled systems consisting of furfural oxidation reactions not only maximize the return on energy investment, but also provide value-added products for both parties. But few research has integrated the anodic furfural oxidation and reduction reactions to produce a double-coupled system, so the creation of an efficient double-coupled electrocatalytic system is important for energy consumption. Finally, further developments are still needed to accomplish industrial large-scale and economic production of FDCA and its derivatives.

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