

Research Article

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Study on the preparation of glycerylphosphorylcholine by transesterification under supported sodium methoxide

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Abstract: Glycerylphosphorylcholine (GPC) was prepared by transesterification using supported sodium methoxide as catalyst and natural lecithin as raw material. Sodium methoxide has been proved to be an effective catalyst for the preparation of GPC, which is easy to recover and reuse. After six repeated uses, its stability is satisfactory. The effects of agitation speed, catalyst dosage, and reaction temperature on the reaction were investigated, respectively, and the optimum conditions for preparing GPC catalyzed by supported sodium methoxide were found: the concentration of phosphorylcholine was $0.1 \text{ mol} \cdot \text{L}^{-1}$, the stirring speed was 600 rpm, the amount of catalyst was $7.5 \text{ g} \cdot \text{L}^{-1}$, the reaction temperature was 45°C , and the reaction time was 4 h; then, the conversion rate of phosphatidylcholine could reach 99%. At the same time, the reaction kinetic model was established based on the mechanism of the transesterification, and the experimental data were compared with the calculated values; it was found that the experimental data fitted the model well. Finally, the reaction activation energy obtained by the Arrhenius equation is $41.6 \text{ kJ} \cdot \text{mol}^{-1}$, which indicates that the supported sodium methoxide has good catalytic performance in this reaction system.

Keywords: supported catalyst, sodium methoxide, glycerylphosphorylcholine, kinetics

1 Introduction

Glycerylphosphorylcholine (GPC) is a water-soluble phospholipid precursor that is found in the human body, and it is very important for treating brain diseases such as acute cerebrovascular accident, Alzheimer's disease, multi-infarct dementia, and cerebral circulation decline, and it can also improve the attention, cognition, and memory of all ages [1–3]. In addition, GPC has the largest effects on protecting the liver and kidney, maintaining the normal secretion of reproductive hormones, and reducing high blood lipid. So, it is widely used in food, health products, medicine, and other industries, which has greatly improved people's quality of life [4–7]. However, the content of GPC in nature is relatively small, and the domestic research on GPC started late and developed slowly; there is a certain difference in quality scale with foreign products. Therefore, many scholars and companies have invested in the research of preparing and producing high-purity GPC, with the hope that it will bring great medicinal value and economic value [8,9].

There are several methods for preparing GPC, the biological extraction method [10,11], in which the raw material is limited, the process is complicated, and the cost is high; in the chemical synthesis method [12,13], which has many side reactions, the intermediate products are unstable and the product yield is lower, while the transesterification method has attracted widespread attention of scholars at home and abroad due to its natural and reliable raw materials in recent years [14–20]. Chadha [21] used egg yolk lecithin as raw material, added cadmium chloride in the alcoholysis process, and finally obtained a complex of GPC and cadmium chloride through recrystallization, in order to obtain pure product; it still needed further treatment. Kangyi et al. [22] hydrolyzed soybean lecithin powder using phospholipase as a catalyst to obtain GPC, and the product was separated using a chromatography column. The purity and recovery of the final GPC were 99.8% and 69.8%, respectively. Our research group has carried out a series of studies on GPC preparation under different

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Table 1: Comparison of the performance of several catalysts

Literature number	Catalyst used	Reaction conditions	Conversion of PC	Advantage and disadvantage
[23]	Low-boiling point organic amines	Catalyst content: 2.4% of the total reaction volume Lecithin concentration: $0.10 \text{ mol}\cdot\text{L}^{-1}$ Reaction temperature: 60°C Reaction time: 4 h	90%	Advantage: (1) Good activity (2) Easy to separate (3) Little deactivation Disadvantage: Low conversion rate
[24]	Propylamine	Catalyst content: 2.4% of the total reaction volume Lecithin concentration: $0.05\text{--}0.10 \text{ mol}\cdot\text{L}^{-1}$ Reaction temperature: 60°C Reaction time: 4 h	98%	Advantage: (1) Easy to separate (2) Easy to recycle Disadvantage: Short lifespan
[25]	<i>Tert</i> -butylamine	Catalyst content: 2.4% of the total reaction volume Lecithin concentration: $0.10 \text{ mol}\cdot\text{L}^{-1}$ Reaction temperature: 60°C Reaction time: 4 h	98%	Advantage: (1) High purity (2) Little deactivation (3) Long service life Disadvantage: Not easy to recycle
[15]	Calcined sodium silicate	Catalyst content: 6 wt% Lecithin concentration: $10.5 \text{ mmol}\cdot\text{L}^{-1}$ Reaction temperature: 65°C Reaction time: 2 h	99.50%	Advantage: (1) Easy to separate (2) Repeated use Still maintain high activity (3) High conversion rate

catalysts [23–25], and the properties of several catalysts are shown in Table 1. In the preparation of GPC, the catalyst used affects the difficulty of separation and purity of product directly, and the solid catalyst can be recycled many times and has long service life [26–28], so the choice of catalyst and its preparation process are very important for the preparation of GPC by transesterification.

In this work, GPC is prepared by transesterification using lecithin as raw material, catalyzed by the supported sodium methoxide. The optimal conditions for the reaction were obtained, and the reaction kinetics was discussed in order to provide theoretical basis for its practical application.

2 Experimental sections

2.1 Materials and chemicals

Lecithin was purchased from Tianjin Heowns Biochemical Technology Co., Ltd. All the chemicals such as sodium methoxide, methanol, and chloroform are of analytical grade, and water used is deionized water.

2.2 Preparation of catalyst

A certain amount of activated silica was added to a round-bottomed flask, and the sodium methoxide solution ($2.2 \text{ mol}\cdot\text{L}^{-1}$) in methanol was poured into it at the ratio of $0.25 \text{ g}\cdot\text{mL}^{-1}$, then stirred, and refluxed at 60°C for 4 h, and filtered after cooling. Finally, the supported sodium methoxide catalyst was obtained after dried.

2.3 Transesterification reaction

The transesterification was performed in a 100 mL three-necked flask equipped with a reflux condenser and magnetic stirrer. When the methanol solution of lecithin was heated to the setting temperature, the supported sodium methoxide catalyst was added and the stirrer was started, and liquid samples about 0.5 mL were withdrawn by a syringe in predefined time intervals; the sample solutions were collected in small vials for further analysis.

2.4 Analysis method

Thin-layer chromatography (TLC) was used to analyze the sampling and calculate the conversion of phosphatidylcholine

(PC). Each sample with equal volume was spotted on the TLC plate, which was prepared from our laboratory by silica gel GF254. After drying for several minutes, the plate was developed in the solvent of chloroform:methanol:water = 13:5:0.8 (volume ratio), the developed plate was dried in an oven for about 10 min and detected in the iodine chamber, and then yellow spots with white background appeared after several minutes. The spots were quantified by densitometric scanning at 450 nm using a Shimadzu dual-wavelength chromatographic scanner CS-930.

3 Results and discussion

3.1 Effect of stirring speed

For heterogeneous reaction processes, the stirring speed affects the mixing, diffusing, and contacting with catalyst of the reactants. Increasing the speed of the stirrer can reduce the effect of external diffusion on the reaction. The concentration of PC is $0.1 \text{ mol}\cdot\text{L}^{-1}$, the catalyst dosage is $10 \text{ g}\cdot\text{L}^{-1}$, the reaction temperature is 40°C , and the reaction time is 4 h; the effect of stirring speed on the transesterification was examined at 200, 400, 600, and 800 rpm, respectively, and the results are shown in Figure 1.

It was found that with increasing stirring speed, the conversion of PC increased, but when the stirring speed was greater than 600 rpm, the stirring speed had little effect on the conversion of PC, indicating that the catalyst was distributed satisfactory in the reactor at the high

stirring speed, and this was considered to be the minimum stirring speed required to eliminate the effect of external diffusion, so the 600 rpm was selected at the subsequent experiments.

3.2 Effect of catalyst amount

As an important factor affecting the chemical reaction, the catalyst not only affects the speed of the reaction and the yield of the product, but also affects the difficulty of purification and separation of subsequent products seriously. Under the conditions of PC concentration of $0.1 \text{ mol}\cdot\text{L}^{-1}$, stirring speed of 600 rpm, reaction temperature of 40°C , and reaction time of 4 h, the catalyst amount was investigated at 5, 7.5, 10, and $12.5 \text{ g}\cdot\text{L}^{-1}$, and the results are shown in Figure 2.

It can be seen that the conversion of PC increased with the increase in catalyst amount. When the amount of catalyst exceeded $7.5 \text{ g}\cdot\text{L}^{-1}$, the amount of catalyst had no significant effect on the conversion of PC. At the end of the reaction, the conversion of PC under catalyst amount of $12.5 \text{ g}\cdot\text{L}^{-1}$ was only 4% higher than that at $7.5 \text{ g}\cdot\text{L}^{-1}$. Therefore, the appropriate amount of catalyst used in the subsequent experiments was $7.5 \text{ g}\cdot\text{L}^{-1}$.

3.3 Effect of reaction temperature

The reaction temperature was examined at 30°C , 35°C , 40°C , 45°C , and 50°C , respectively, to discuss its effect on the transesterification process, under the conditions of a

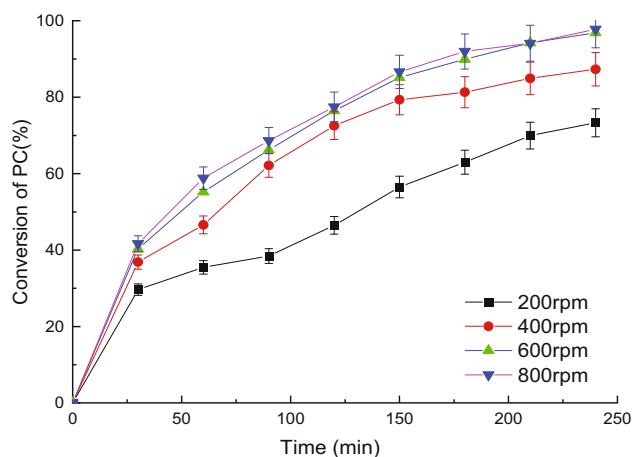


Figure 1: Effect of stirring speed on the conversion of PC. Reaction conditions: the concentration of PC was $0.1 \text{ mol}\cdot\text{L}^{-1}$, the catalyst dosage was $10 \text{ g}\cdot\text{L}^{-1}$, the reaction temperature was 40°C , and the reaction time was 4 h.

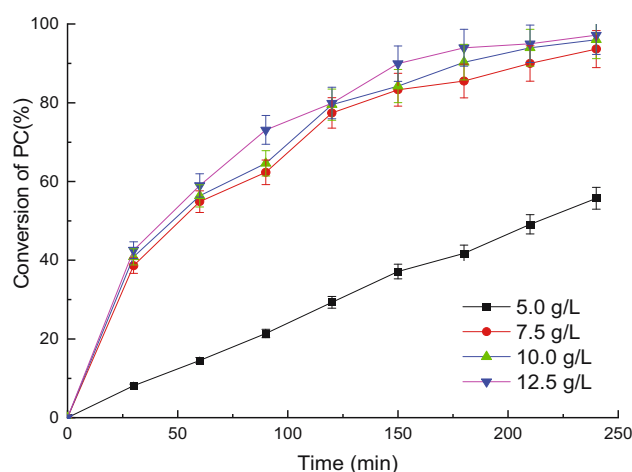


Figure 2: Effect of catalyst amount on the conversion of PC. Reaction conditions: concentration of PC was $0.1 \text{ mol}\cdot\text{L}^{-1}$, stirring speed was 600 rpm, reaction temperature was 40°C , and reaction time was 4 h.

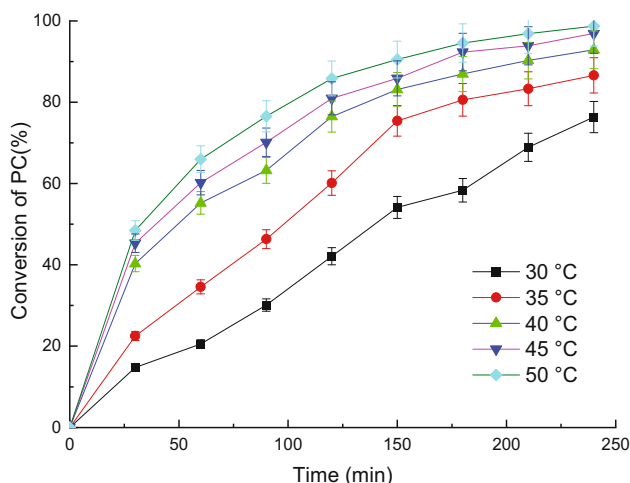


Figure 3: Effect of temperature on the conversion of PC. Reaction conditions: concentration of PC was $0.1 \text{ mol}\cdot\text{L}^{-1}$, stirring speed was 600 rpm, catalyst amount was $7.5 \text{ g}\cdot\text{L}^{-1}$, and reaction time was 4 h.

concentration of PC of $0.1 \text{ mol}\cdot\text{L}^{-1}$, a stirring speed of 600 rpm, a catalyst amount of $7.5 \text{ g}\cdot\text{L}^{-1}$, and a reaction time of 4 h. The results are shown in Figure 3.

As can be seen, the conversion of PC increased with increasing temperature. When the temperature rose above 40°C , the increase in the conversion of PC gradually decreased. When the reaction temperatures were 45°C and 50°C , the conversion of PC was basically the same at the end of the reaction. Therefore, 45°C was selected as the most suitable experimental temperature.

3.4 Stability of catalyst

When the transesterification completed under the suitable conditions, the catalyst was filtered off and reused after washing with anhydrous methanol (Figure 4). It was found that only 9% decrease in PC conversion was observed after recycling six times under the same conditions, and the catalyst stability was satisfactory during the experiment.

3.5 Reaction kinetic analysis

The mechanism of the transesterification can be interpreted as shown in Scheme 1. First, sodium methylate dissociates the methoxy ion. In the second step, the nucleophilic methoxy group attacks the carbonyl carbon atom on the PC molecule and forms an intermediate with a tetrahedral structure. In the third step, this intermediate undergoes electron transfer and rearranges to produce lysophospholipid (LPC) negative ions, which combine with

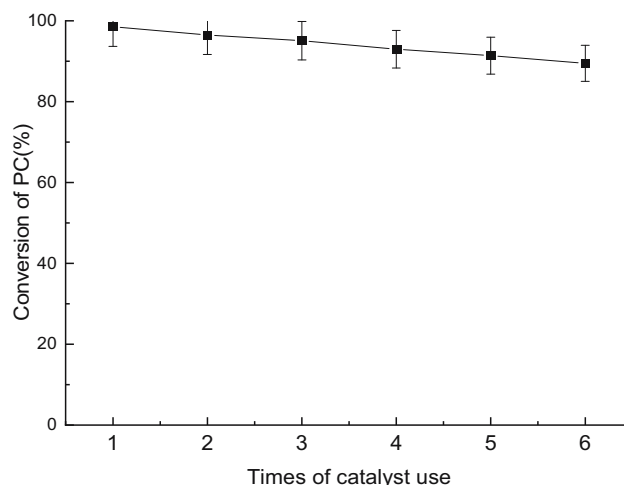
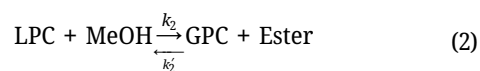
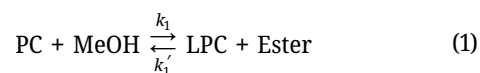


Figure 4: Stability of the catalyst.

protons provided by methanol to form the intermediate LPC. Finally, the methoxy group continues to attack the acyl carbon atoms on the lecithin molecule, and the process is repeated to produce GPC.

The entire transesterification can be expressed as follows:



The first step is assumed to be much faster than the second step, so the intermediate LPC is in equilibrium with the reactants PC and MeOH at any time. Using the steady-state approximation, the concentration of LPC can be expressed as:

$$\frac{dC_L}{dt} = k_1 C_P C_M - k_1' C_L C_E = 0 \quad (3)$$

so,

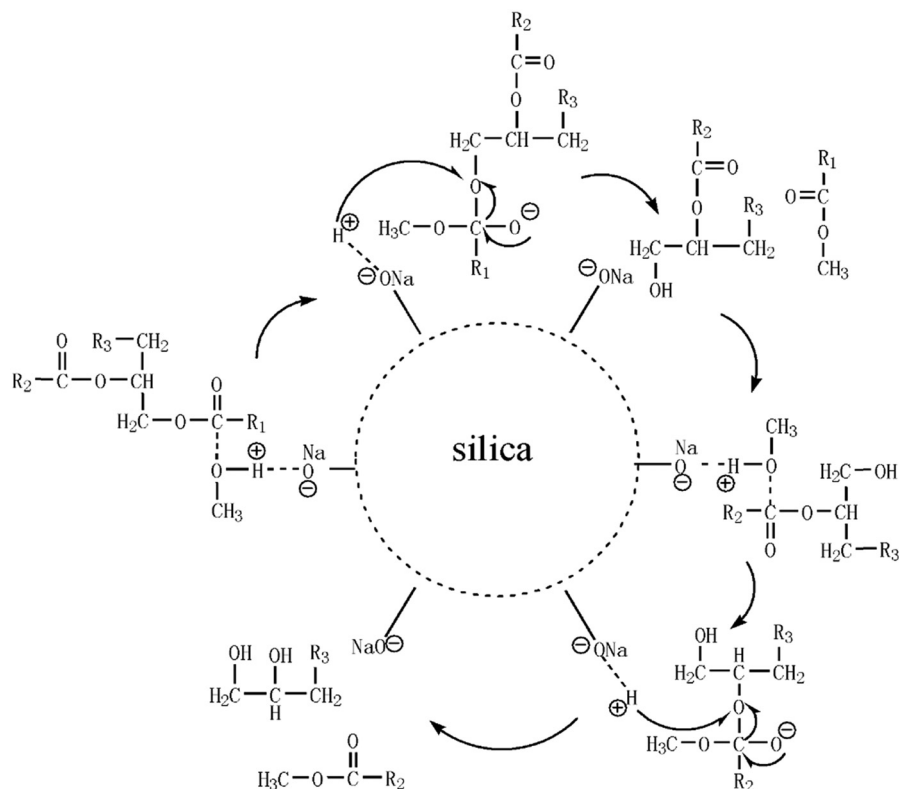
$$C_L = \frac{k_1 C_P C_M}{k_1' C_E} \quad (4)$$

During the entire reaction process, methanol is greatly excessive, so the reverse reaction can be ignored. The formation rate of GPC can be expressed as:

$$\frac{dC_G}{dt} = k_2 C_L C_M \quad (5)$$

Expressing the concentration of each substance by the conversion rate of PC, x_p , so the formula 5 can be changed to:

$$\frac{dx_p}{dt} = \frac{k_1 k_2 (1 - x_p)(C_{M0} - 2C_{P0}x_p)^2}{k_1' C_{P0} 2x_p} \quad (6)$$



Scheme 1: Mechanism of transesterification catalyzed by the supported sodium methoxide.

Defined $C_{M0}/C_{P0} = M$, $K' = k_1k_2/k_1'$, then

$$\frac{dx_p}{dt} = \frac{K'C_{P0}(1-x_p)(M-2x_p)^2}{2x_p} \quad (7)$$

By integrating the aforementioned formula, we get

$$K'C_{P0}t = Kt = \frac{2}{M-2} \cdot \left[\frac{1}{M-2} \ln \left(\frac{M-2x_p}{1-x_p} \right) - \frac{M}{2(M-2x_p)} \right] \quad (8)$$

The experimental data under different catalyst amounts were substituted into the right part of formula 8 and plotted against the reaction time. It was found that the data fit the equation model well (Figure 5).

Similarly, the experimental data at different reaction temperatures were substituted into the right part of formula 8 and plotted against the reaction time (Figure 6). The linear correlation coefficient R^2 of each fitted line is above 0.97, which indicates that the kinetic equation model is

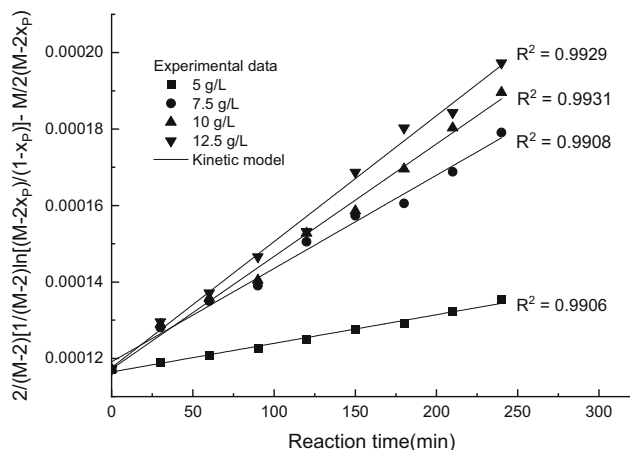


Figure 5: Fitting of reaction kinetics at different catalyst amounts.

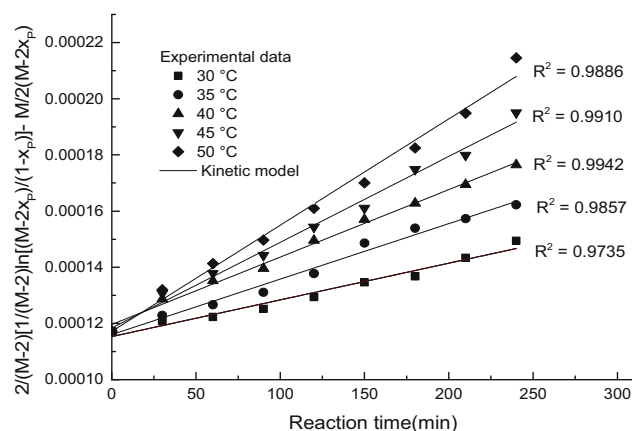


Figure 6: Fitting of reaction kinetics at different reaction temperatures.

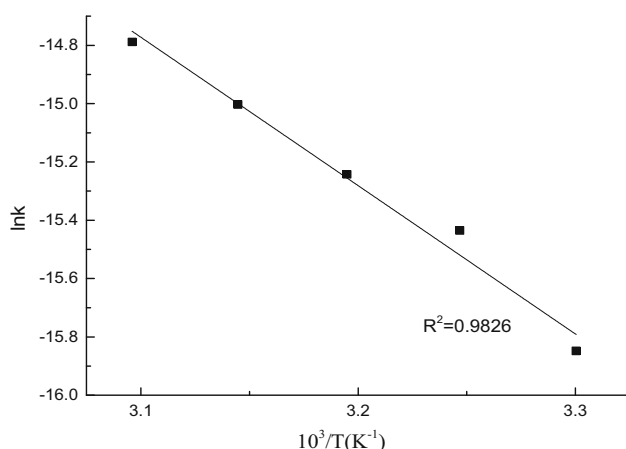


Figure 7: Arrhenius plot of $\ln K$ vs $10^3/T$.

equally applicable for the reaction systems at different temperatures.

According to the Arrhenius equation, the logarithms of the slope k for the dynamic fit curves at different temperatures were plotted against $1/T$ (Figure 7). From the slope of the straight line, the activation energy E_a is $41.6 \text{ kJ}\cdot\text{mol}^{-1}$, indicating that the catalyst has good catalytic performance in their action system.

4 Conclusions

The supported sodium methoxide catalyst has achieved significant results in the preparation of GPC by transesterification. Under the optimum reaction conditions, the amount of catalyst is $7.5 \text{ g}\cdot\text{L}^{-1}$, the reaction temperature is 45°C , stirring rate is 600 rpm, and reaction time is 240 min, and the conversion rate of PC is 98.9%. The reaction kinetic model was established, and it was found that the experimental data fitted the model well. The activation energy of the reaction was $41.6 \text{ kJ}\cdot\text{mol}^{-1}$, and the catalytic performance of the supported sodium methoxide in this reaction system is satisfactory.

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Lele Zhou: resources, data curation, investigation; Zejing Fan: formal analysis, investigation, resources; Biao Yan: validation, formal analysis, data curation; Xiaoli Zhang: visualization, investigation, formal analysis.

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